


# *Process Research Over 25 Years*

*A Personal  
Perspective*

***Steven V. Ley***

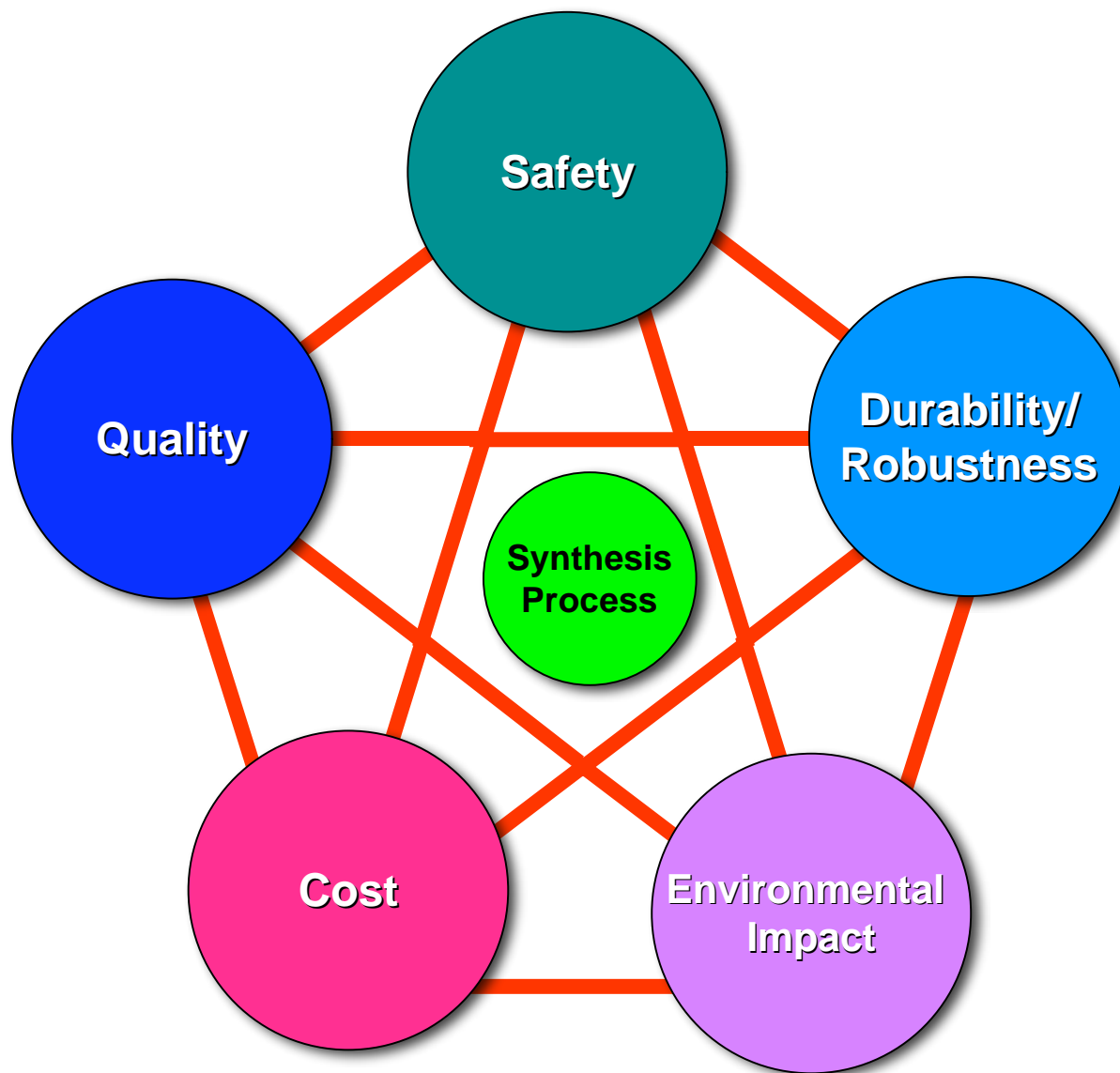
*Department of Chemistry  
University of Cambridge  
<http://leygroup.ch.cam.ac.uk>*



*“It does, for example, no good to offer an elegant, difficult and expensive process to an industrial manufacturing chemist, whose ideal is something to be carried out in a disused bathtub by a one-handed man who cannot read, the product being collected continuously through the drain hole in 100% purity and yield.”*

Sir John Cornforth, *Chem. Brit.* 1975, 342.

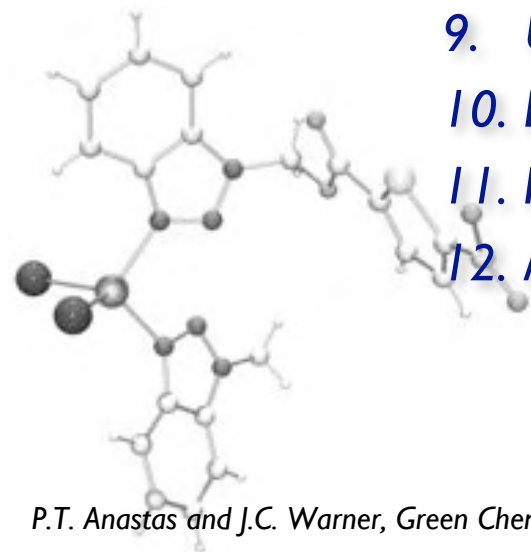
## Major Route Design Factors and Their Interactions



## Twelve Principles of Green Chemistry



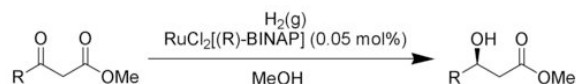
1. Prevent waste rather than treat/clean it up later
2. Invoke atom economy
3. Design safer chemicals
4. Use & generate less toxic substances
5. Massively reduce quantities of solvents used
6. Design syntheses for energy efficiency
7. Renewable feedstock for large scale processes
8. Minimize steps in synthesis
9. Use of highly-selective catalytic reagents
10. Design materials that innocuously degrade
11. Real-time monitoring for pollution prevention
12. Minimise potential for accidents



# Landmark Papers – A Personal Selection Strategically Important Processes

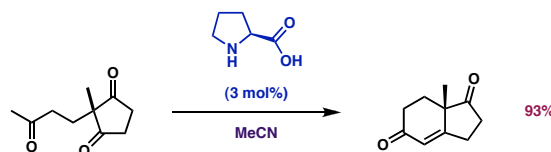
## Noyori asymmetric hydrogenation (reduction of $\beta$ -keto-esters)

R. Noyori, T. Okhuma, M. Kitamura, H. Takaya, N. Sayo,  
H. Kumobayashi, S. Akuragawa,  
*J. Am. Chem. Soc.* **1987**, 109, 5856-5858



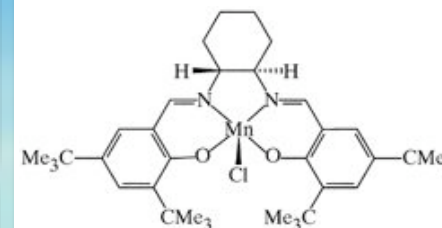
## Hajos-Parrish (orgcat)

Z. G. Hajos and D. R. Parrish  
*J. Org. Chem.* **1974**, 39, 1615



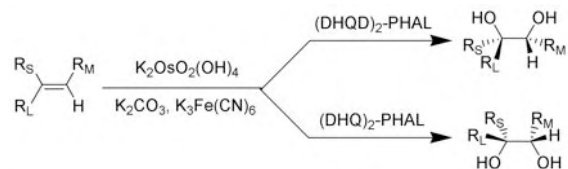
## Jacobsen's Catalyst

E.N. Jacobsen, J.F. Larrow, Y. Gao,  
Y. Hong, X. Nie, C.M. Zepp  
*J. Org. Chem.*, 1994, **59**, 1939.



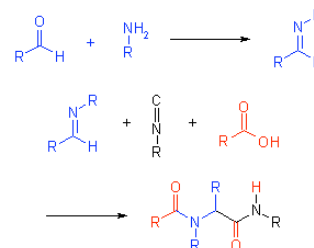
## Sharpless asymmetric dihydroxylation

E.N. Jacobsen, I. Marko, W.S. Mungall, G. Schroeder,  
K.B. Sharpless  
*J. Am. Chem. Soc.* **1988**, 110, 1968



## Ugi multi-component coupling

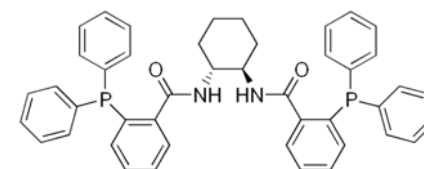
I. Ugi, R. Meyr, U. Fetzer, C. Steinbrucker.  
*Angew. Chem.* **1959**, 71, 386.



## Trost's Ligand

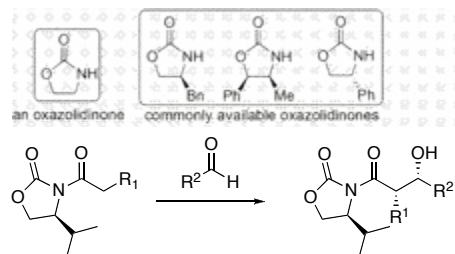
(Asymm. Allylic Alkylation)

B.M. Trost, D.L. Van Vranken, C. Bingel  
*J. Am. Chem. Soc.*, 1992, **114**, 9327.



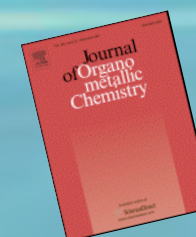
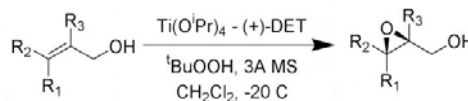
## Evans chiral auxiliary

D.A. Evans, *Aldrich. Acta*, **1982**, 15, 23

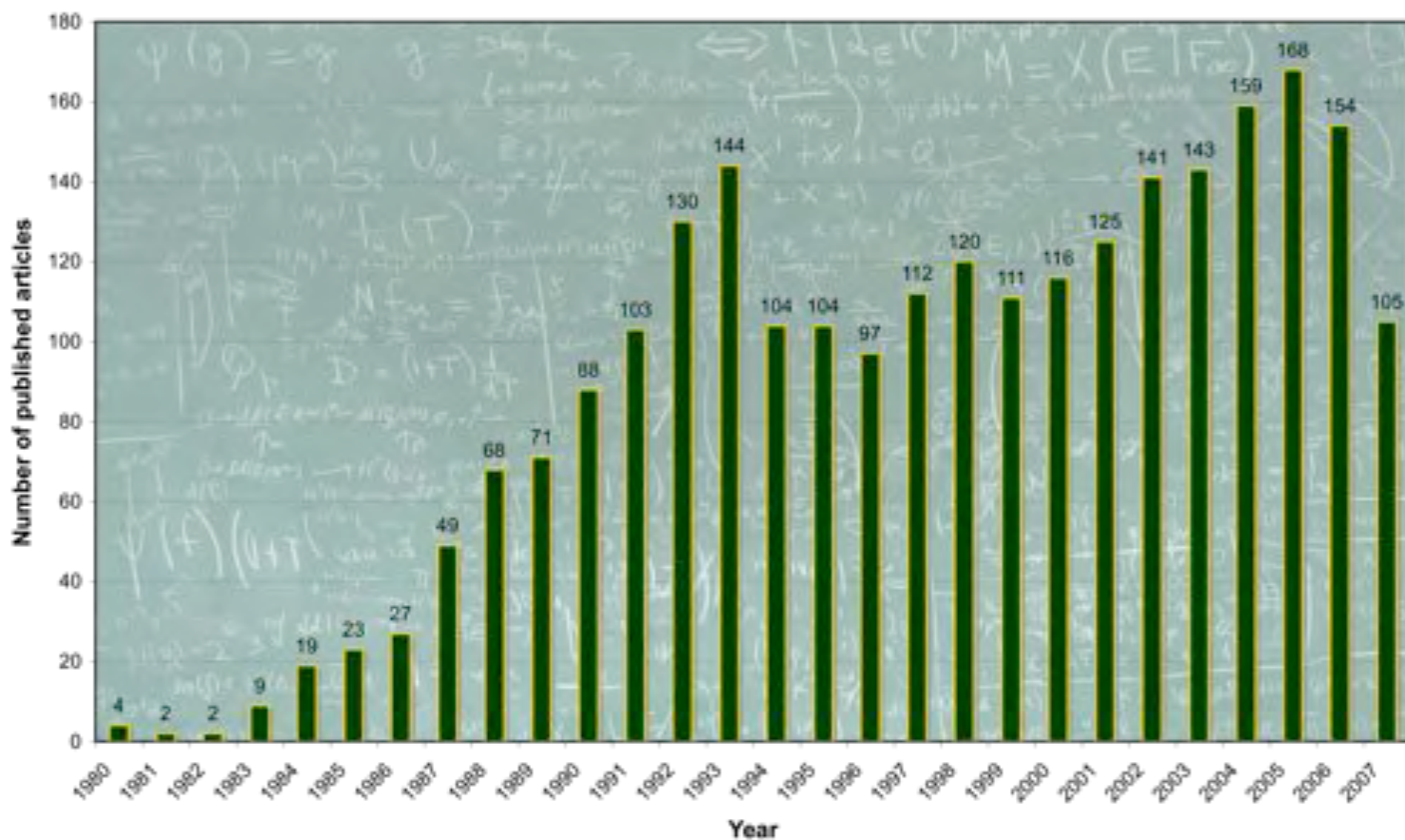
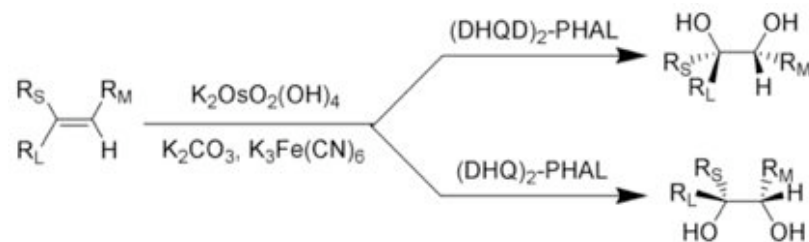
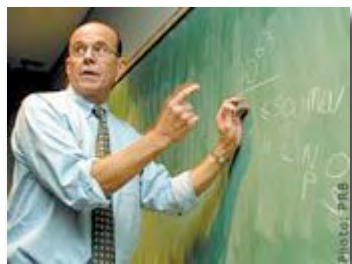


## Sharpless epoxidation

T. Katsuki and K.B. Sharpless  
*J. Am. Chem. Soc.* **1980**, 102, 5974



# Sharpless Asymmetric Dihydroxylation Reaction



# Landmark Papers – A Personal Selection Strategically Important Processes

## Suzuki reaction

N. Miyaura and A. Suzuki  
*J. Chem. Soc., Chem. Commun*, **1979**, 3427

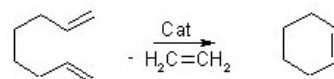


BASF plant in Guaratingueta, Sao Paulo, Brazil, where the fungicide boscalid is manufactured.

## Metathesis reactions

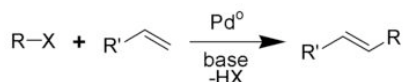
Cross; Ring-closing; Enyne; Ring-opening; ROMP, Acyclic dienes; Alkyne; Alkane.

e.g. R.R. Schrock *et al.*, *J. Am. Chem. Soc.*, 1990, *112*, 3875.  
R.H. Grubbs *et al.*, *J. Am. Chem. Soc.*, 1993, *115*, 9858.  
R.H. Grubbs *et al.*, *Angew. Chem., Int. Ed. Engl.*, 1995, *34*, 2039.



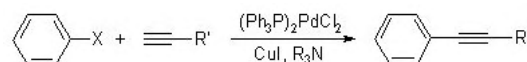
## Heck reaction

R.F. Heck, J.P.J. Nolley,  
*J. Org. Chem.* **1972**, *37*, 2320.



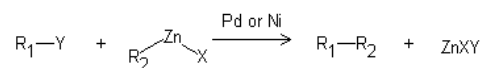
## Sonogashira cross-coupling

K. Sonogashira, Y. Tohda, N. Hagihara  
*Tetrahedron Lett.*, 1975-4467.



## Negishi cross-coupling

E. Negishi *et al.*, *J. Org. Chem.* **1977**, *42*, 1821.



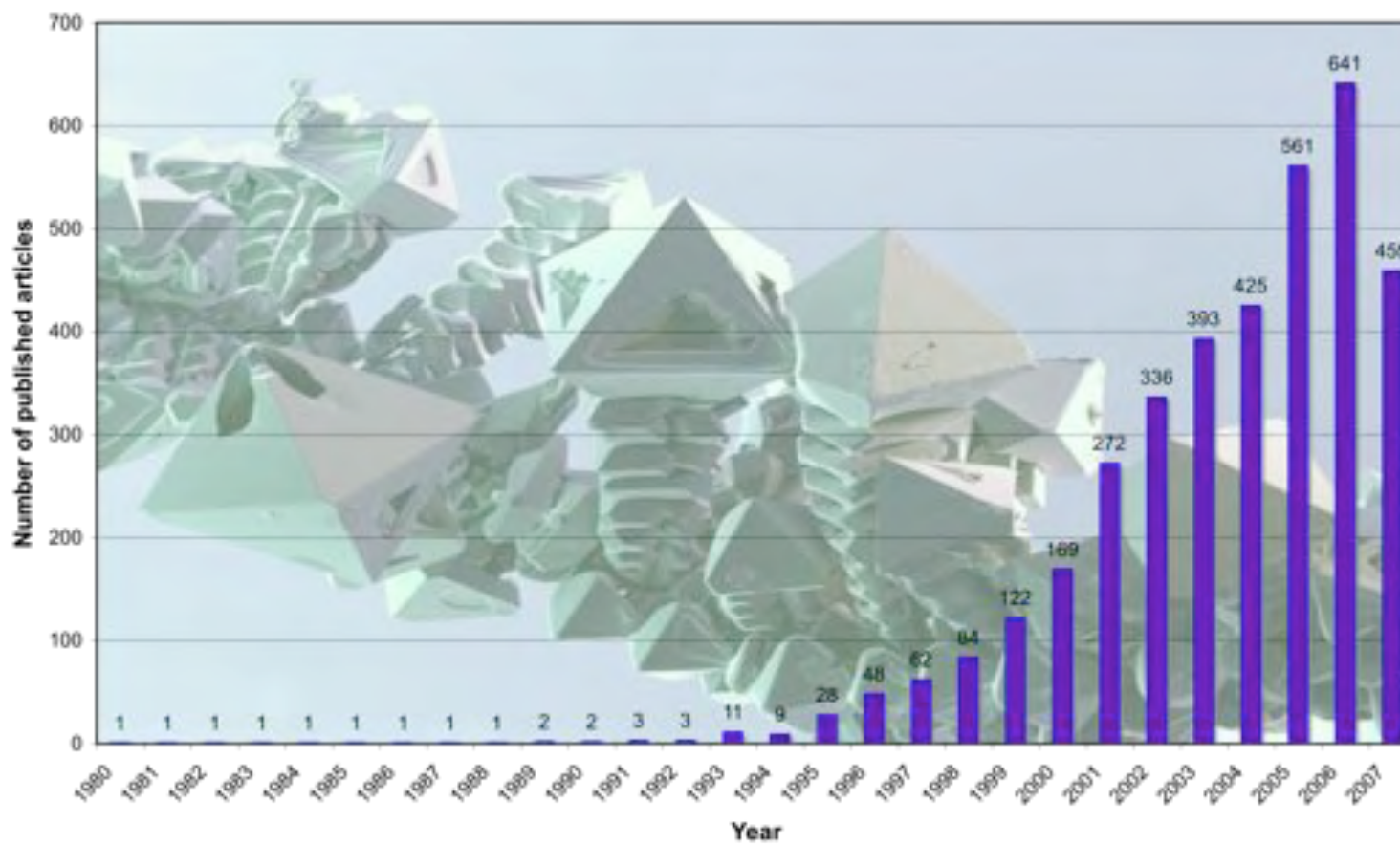
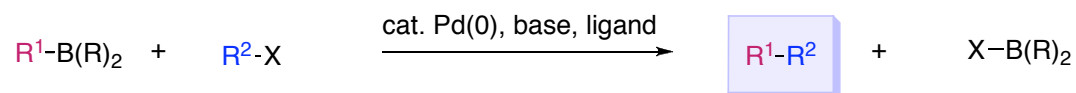
X, Y = halogen

R<sub>1</sub> = alkenyl, aryl, allylic, benzylic

R<sub>2</sub> = alkenyl, aryl, alkynyl, alkyl, allylic, benzylic

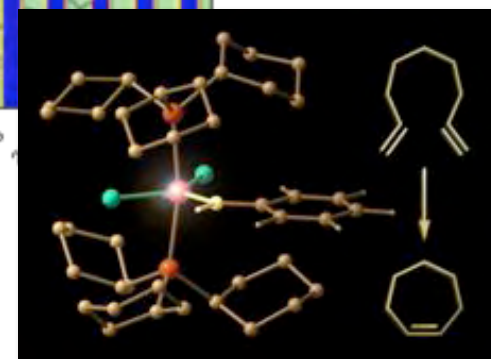
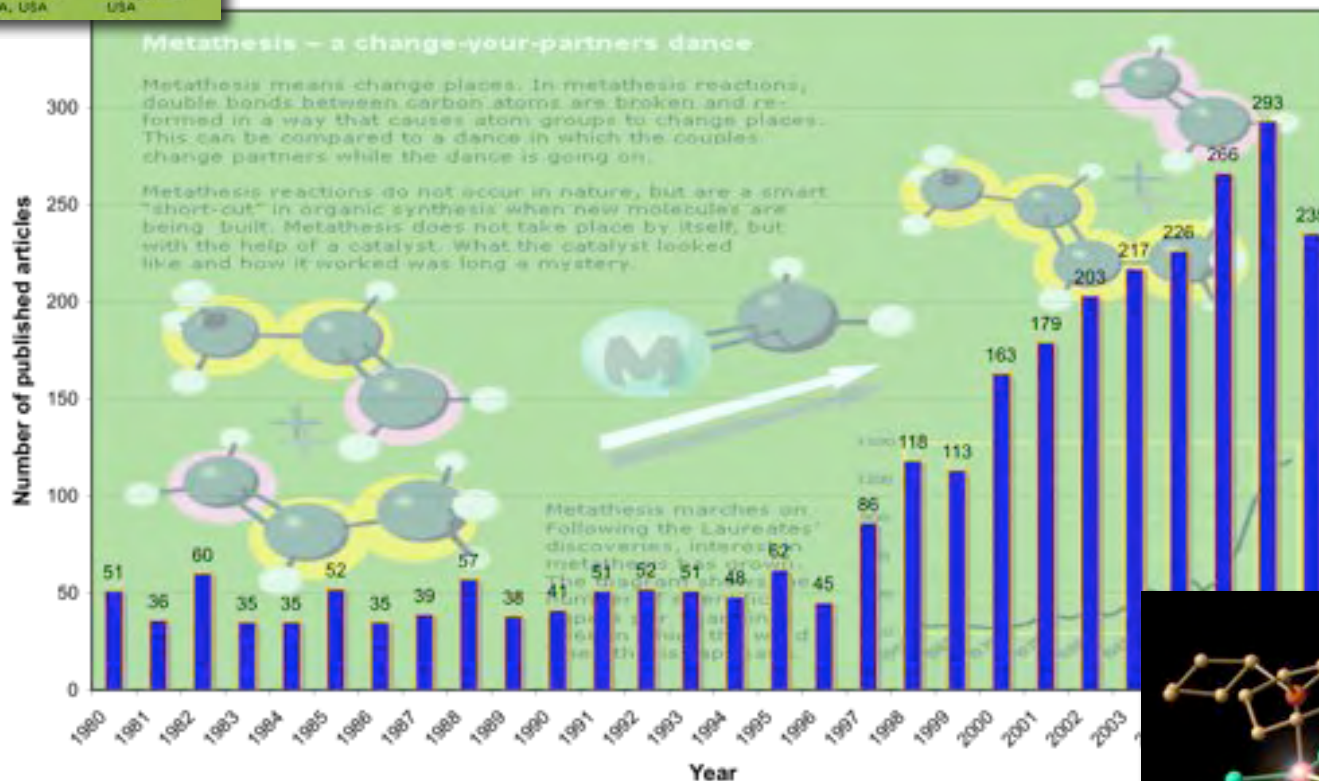


# The Suzuki Reaction – a Key Organic Process









# Alkene Metathesis



# Analysis of Reactions Used for Drug Candidate Synthesis

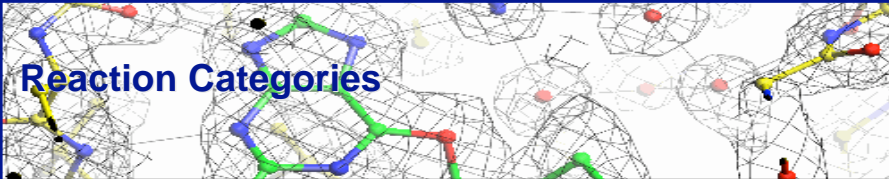





In carrying out this survey, the syntheses of **128 drug candidate molecules** were analysed, these were divided between the three companies and covered all therapeutic and geographic areas that the companies have R&D interests.

 <b>Headline Data</b>	AstraZeneca 	GlaxoSmithKline 	Pfizer 	Total
Number of syntheses	45	39	44	128
Total number of chemical transformations	371	310	358	1039
Average number of chemical transformations per synthesis	8.2	7.9	8.1	8.1
Number of chiral compounds	25	23	21	69
Number of chiral centres	46	52	37	135
Number of chiral centres generated	22	19	20	61
Number of substituted aromatic starting materials	64	79	63	206
New aromatic heterocycles formed	14	11	29	54

Analysis of the reactions used for the preparation of drug candidate molecules  
 J.S. Carey, D. Laffan, C. Thomson and M.T. Williams, *Org. Biomol. Chem.*, 2006, 4, 2337-2347.

## Summary of Reaction Categories

	AstraZeneca 	GlaxoSmith Kline 	Pfizer 	Total /% of total reactions
Heteroatom alkylation and arylation	87	57	52	196 (19%)
Acylation	41	37	50	128 (12%)
C-C bond forming reaction	31	41	44	116 (11%)
Aromatic heterocycle formation	16	10	26	52 (5%)
Deprotection	54	56	49	159 (15%)
Protection	18	16	27	61 (6%)
Reduction	27	24	43	94 (9%)
Oxidation	17	7	16	40 (4%)
Functional group interconversion	43	34	27	104 (10%)
Functional group addition	13	8	12	33 (3%)
Resolution	14	8	8	30 (3%)
Miscellaneous	10	12	4	26 (3%)
<b>Totals</b>	<b>371</b>	<b>310</b>	<b>358</b>	<b>1039</b>

Analysis of the reactions used for the preparation of drug candidate molecules  
 J.S. Carey, D. Laffan, C. Thomson and M.T. Williams, *Org. Biomol. Chem.*, 2006, 4, 2337-2347.

## New Reactions – Trends, Drivers & Changes



- Metal-catalyzed aryl and olefin amination
- C-H activation methods
- Organogold chemistry
- Metathesis
- New metal-based catalysts (recycle/containment)
- Asymmetric organocatalysis
- Control of radical reactions
- Alternative solvents (scCO<sub>2</sub>, H<sub>2</sub>O, ionic liquids)
- Greener chemistries
- Biotransformations, directed evolution techniques
- Effects of outsourcing

## Emerging Technologies for Chemical Process R&D

- *High throughput screening and analysis methods*
- *DoE and principal component analysis methods*
- *Calorimetry measurement methods*
- *Real-time analysis and kinetics evaluation*
- *Polymorph and salt selection protocols*
- *Impurity profiling methods*
- *Reaction modeling and workflow analysis*
- *Route evaluation methods*
- *Continuous processing procedures*
- *Micro and meso flow reactors, spinning disc reactors, shear mixers*
- *Immobilization, particularly scavenging methodology*
- *Plug and segmental flow techniques*
- *Microwave/superheated flow tubes*

## Emerging Technologies for Chemical Process R&D

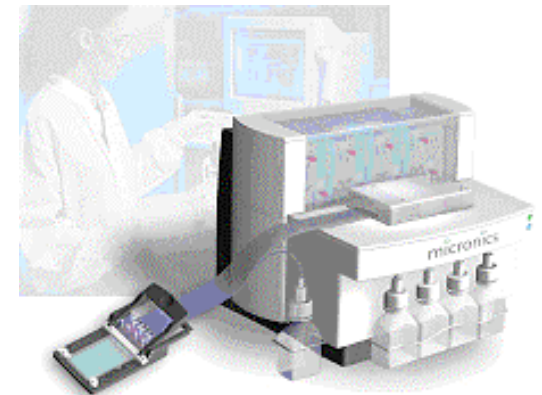
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- *DoE and principal component analysis methods*
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## Disadvantages and Barriers to Continuous Flow Processing

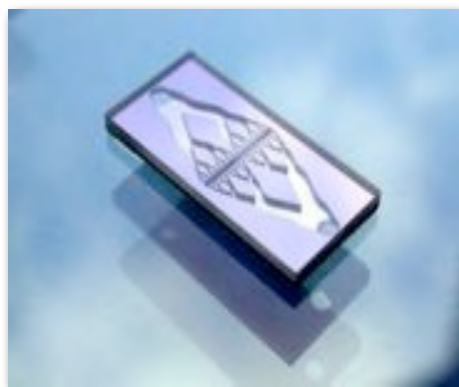


### *Change in Technology but a Massive Change in Philosophy*

- Cost of the equipment in an ever changing environment and time needed for effective assessment of the relevant competitive technologies
- Lack of relevant experience and knowledge of flow chemistry;
  - there is a need for training
  - future development of the relevant skill base (and management)
- The problem of solids / slurries (oscillation methods, high temperatures / pressures, protecting group strategies, disk reactors, etc.)
- The cost of investment in existing plant and infrastructure leads to a level of inflexibility
- Regulatory issues batch to flow yet to be properly addressed
- Enforced conservatism as opposed to the bold solution



## Some Early Decisions



- Single vs. Multi-step
- Reaction understanding needs to be high
- Use of immobilized systems – reagents, scavengers, catch and release tagging and phase switch techniques
- Versatility of the equipment – rapidly reconfigured modular devices or designed for specific operations
- Plug flow and segmentation vs. steady-state continuous processing
- Scale  $10^{17}$  range in quantity requirements – nano - full scale production
- Need for effective cross disciplinary interactions



# New Tools for Molecule Makers

## NEW CHEMISTRY DEVICES

Microarrays, Calorimetry, Flow reactors  
Nanoscience/ technology  
Mini reactor wells, Microfluidic reactors  
Diagnostic reporter devices  
Novel solvents: *ionic liquids*,  $CO_2$ ,  $H_2O$ ,  
*fluorous phase*  
Wireless devices

## AUTOMATION TOOLS

Multi-channel mass spectroscopy  
Robotic equipment: *polymorph  
hunting devices*, *salt selectors*  
Preparative autoseparation devices  
DoE, PCA & ReactArray methods  
Flow and MAS NMR techniques  
HT X-ray crystallography  
Databases & informatics



## BIOCHEMISTRY TOOLS

Gene shuffling  
Phage display techniques  
Multi-enzymes in synthesis  
Directed evolution techniques

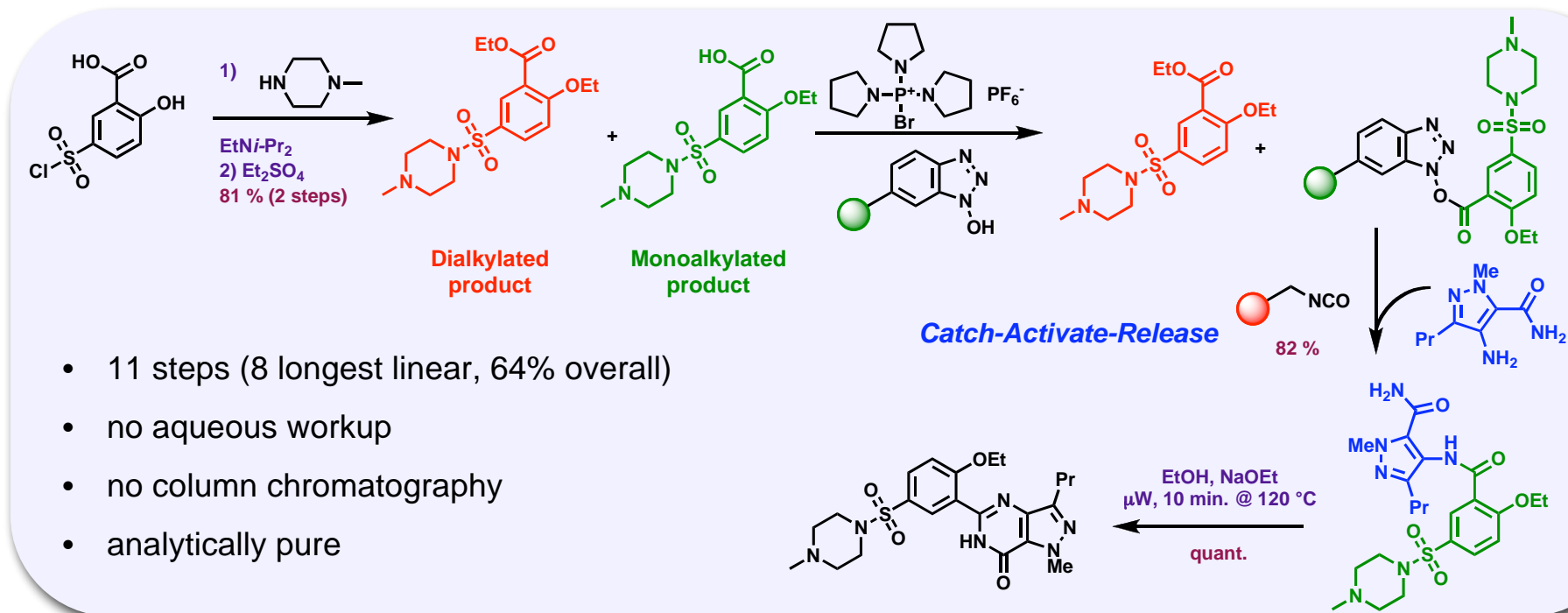
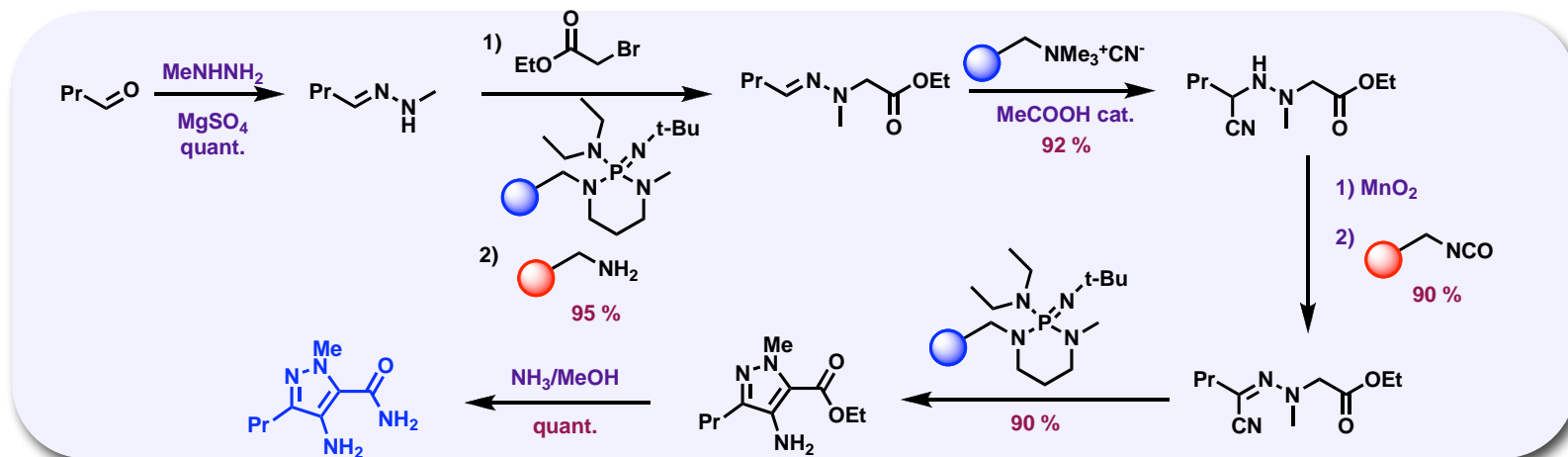
## CHEMISTRY TOOLS

Polymer-supported reagents  
Scavenger resins  
Capture & release techniques  
Multi-parallel synthesis  
Fast serial processing  
Microwaves, microfluidics  
Dynamic and Self Assembly  
methods  
Molecular imprinting  
Rapid catalyst discovery  
Structural morphing techniques

## COMPUTATIONAL TOOLS

Conformation, shape & cluster analysis, Compound design, Diversity algorithms

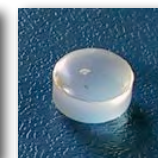
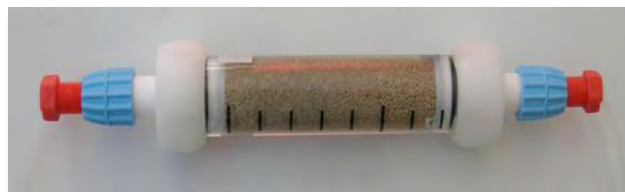
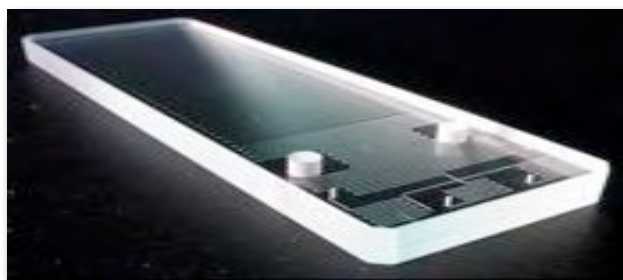
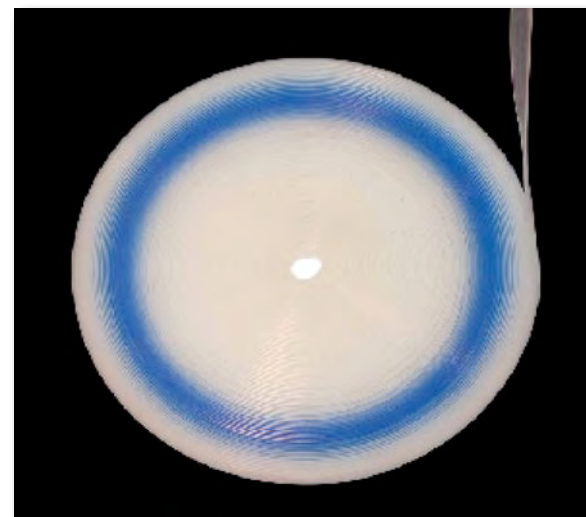
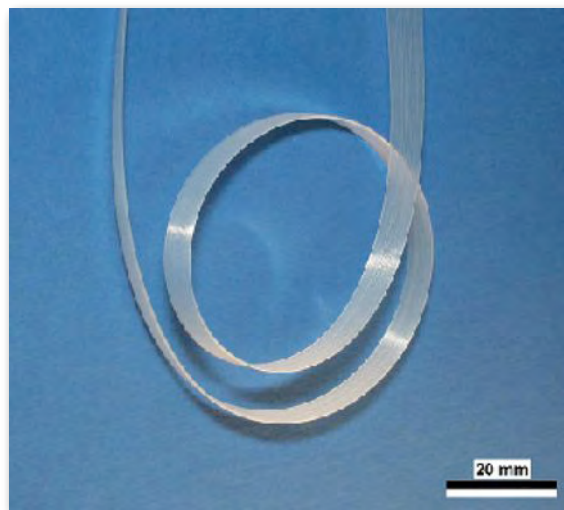
# Synthesis of Sildenafil (Viagra™)



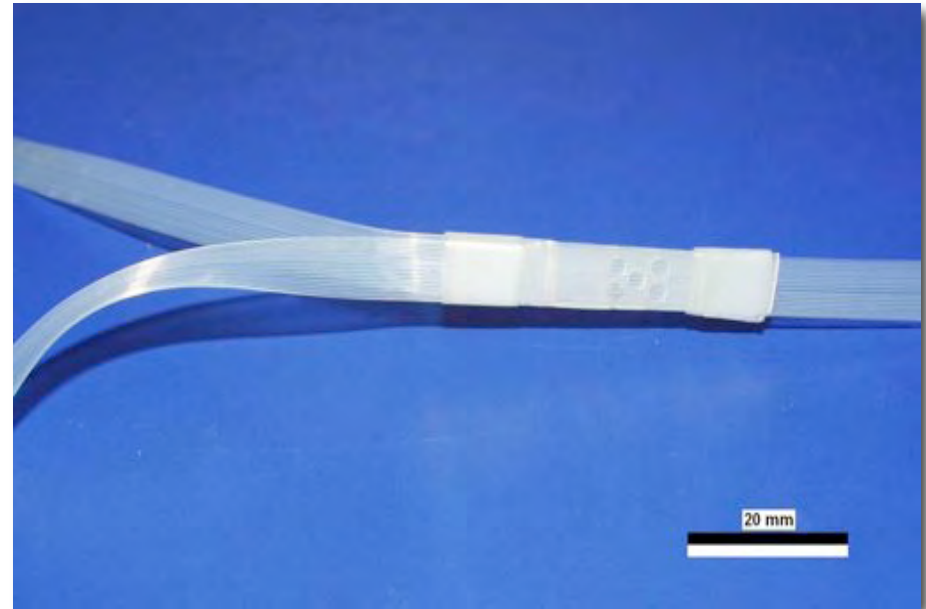
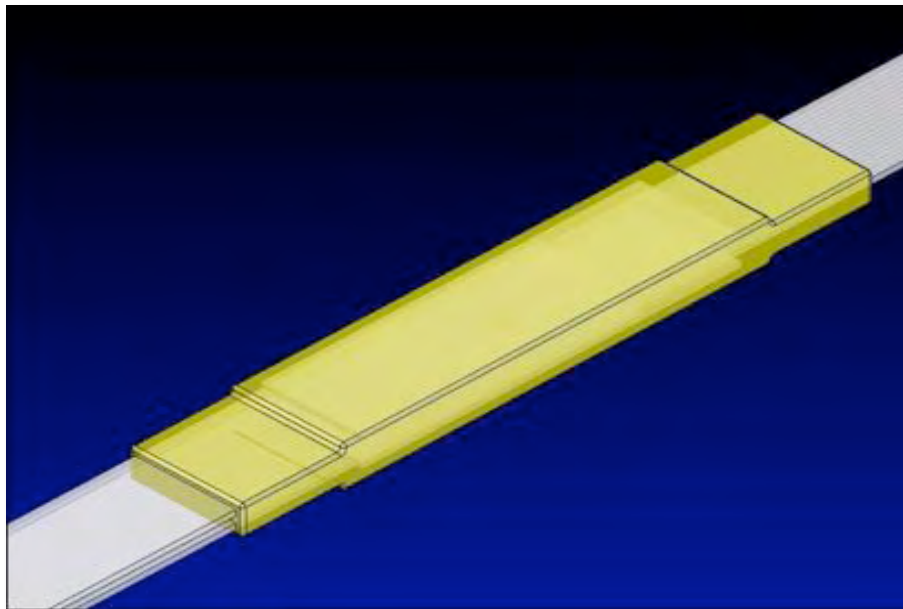
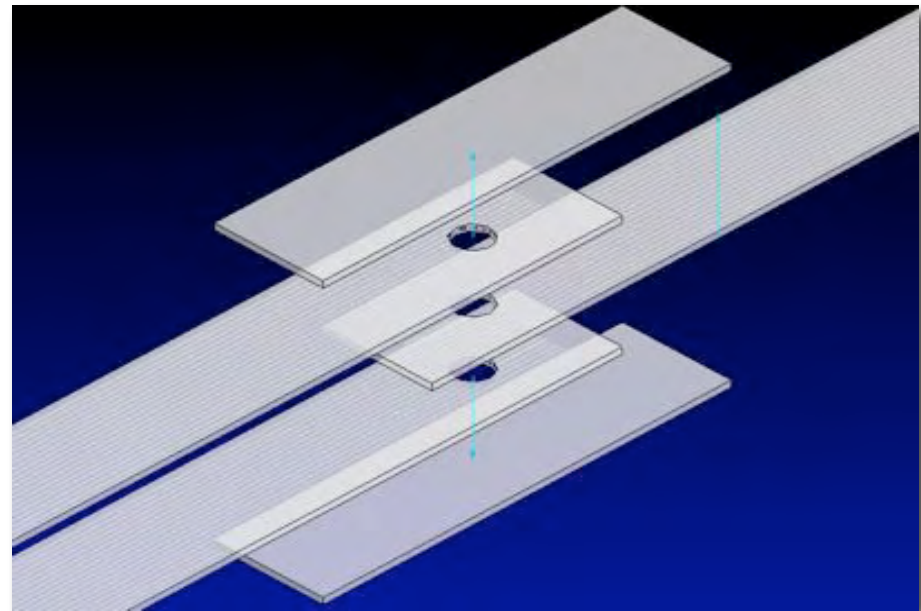
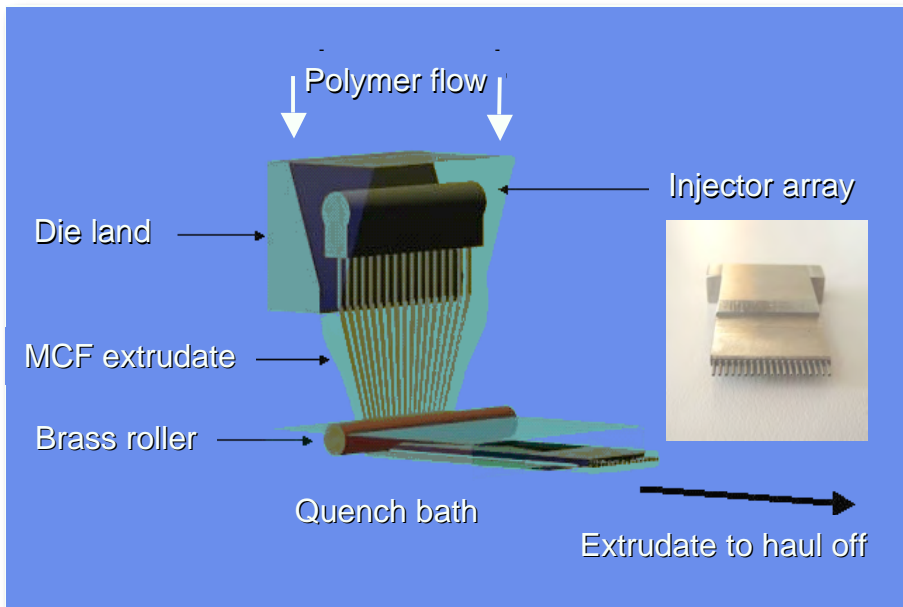
- 11 steps (8 longest linear, 64% overall)
- no aqueous workup
- no column chromatography
- analytically pure

Polymer-Supported Reagents for Multi-Step Organic Synthesis: Application to the Synthesis of Sildenafil  
 I.R. Baxendale and S.V. Ley, *Bioorg. Med. Chem. Lett.*, 2000, 10, 1983-1986.

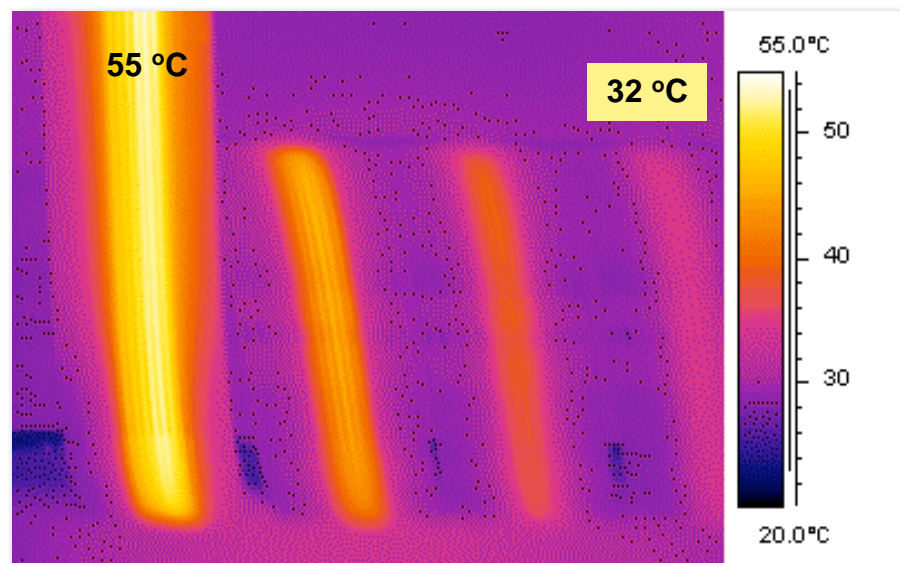
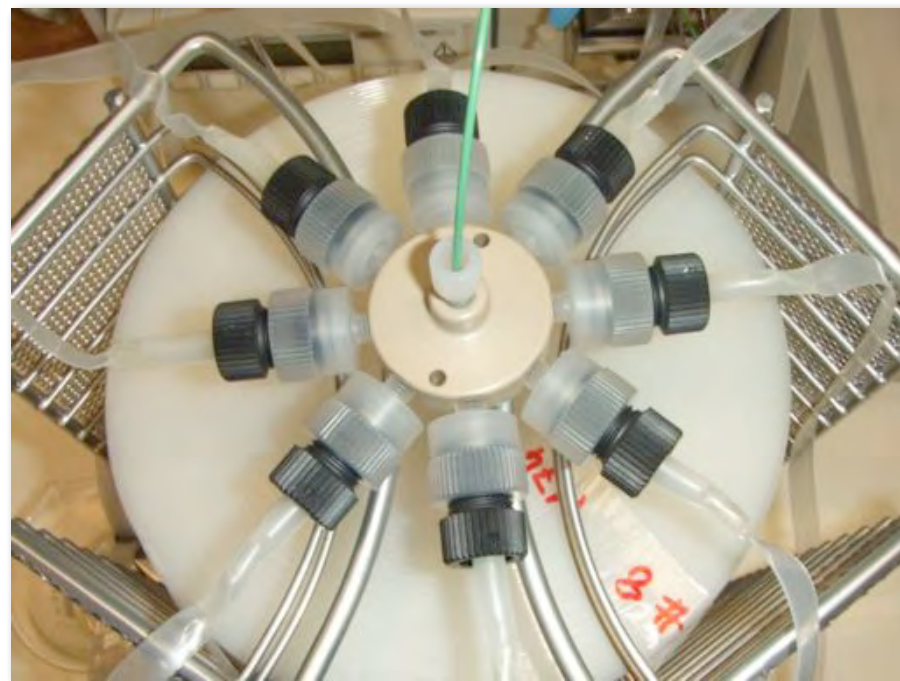
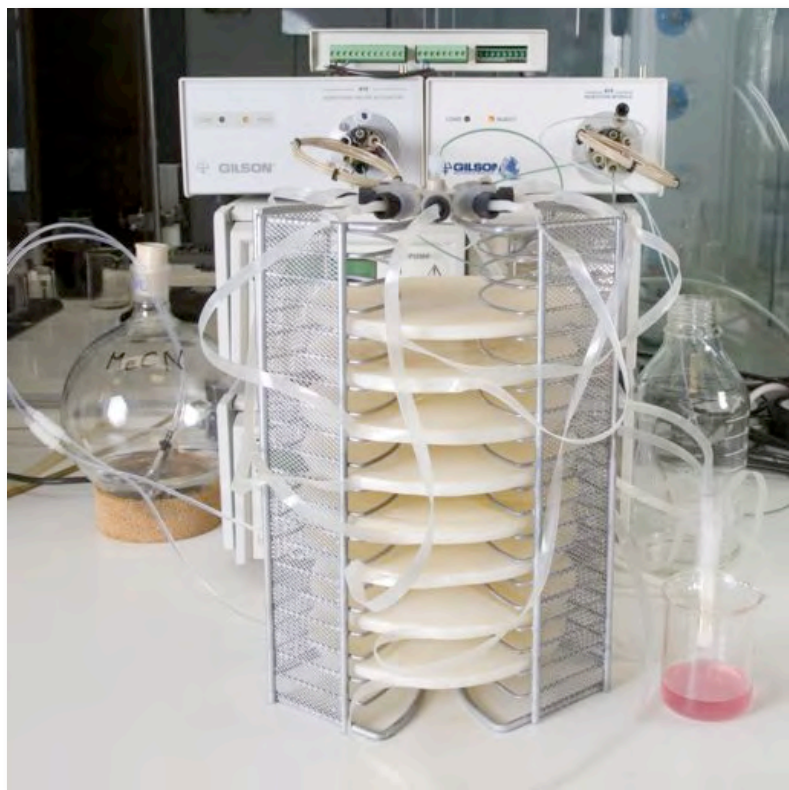
# Different Formats for Supported Reagents



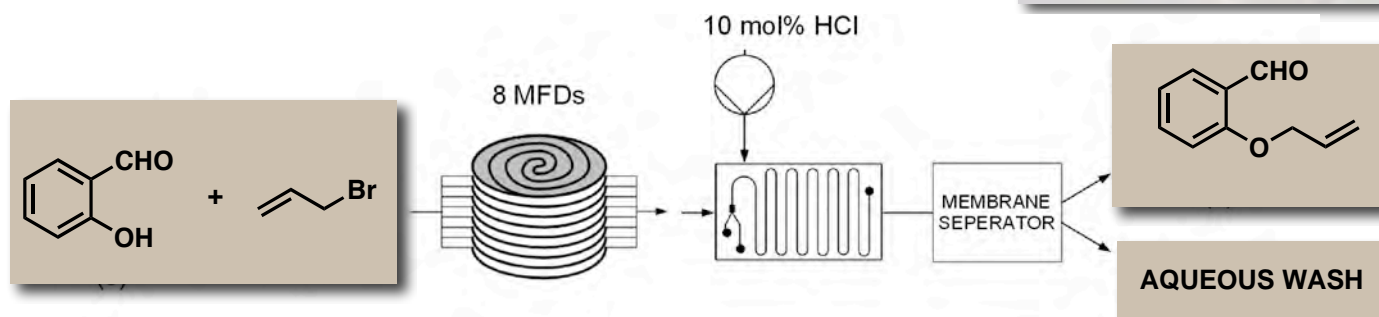
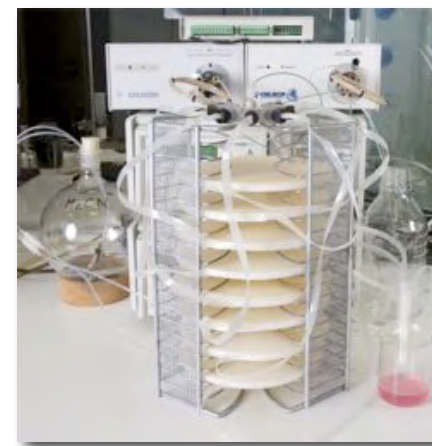
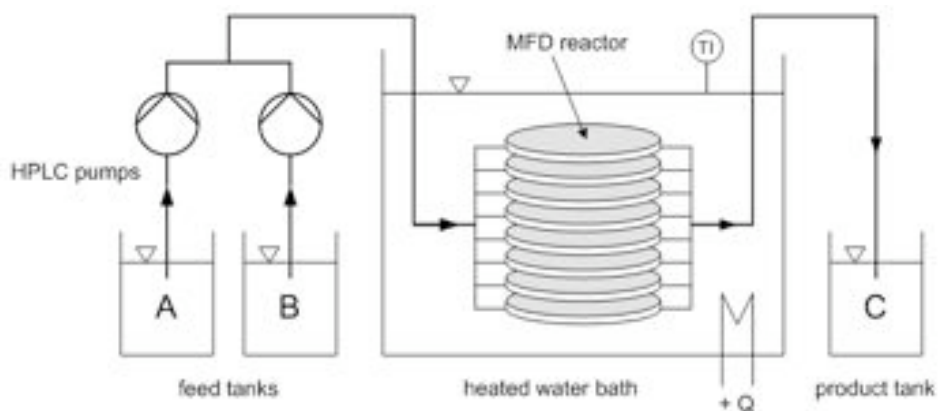
# Microcapillary Reactor & Mixing Device



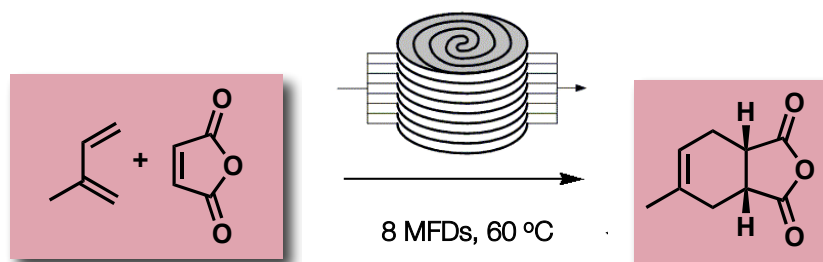
# Microcapillary Reactor



# MFD Reactor



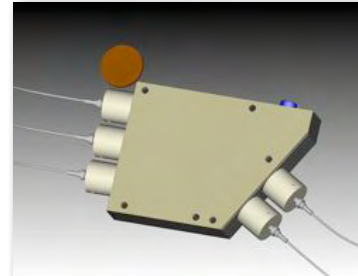
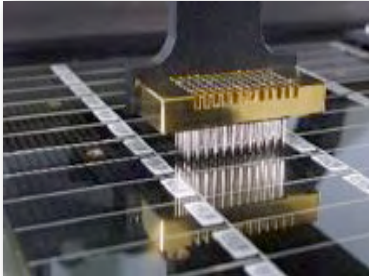
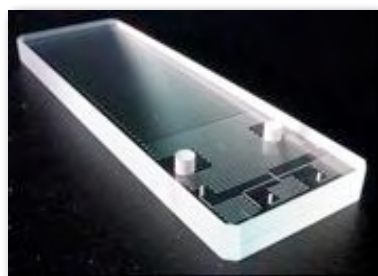
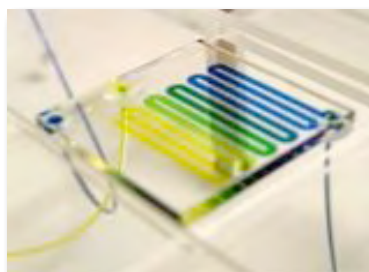
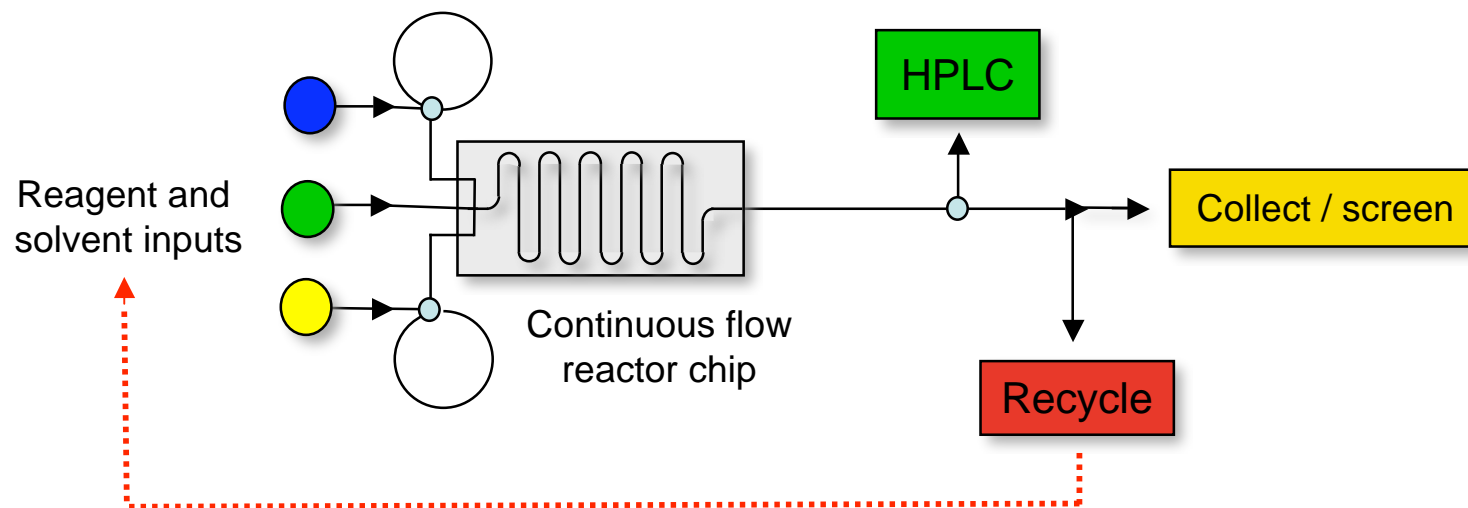
98% isolated yield; 4 ml/min  
output 0.37 g/min or 0.526 kg/day



93 % conversion (98%  
isolated yields) 6 ml/min;  
output of 2.73 g/min or 3.93  
kg/day

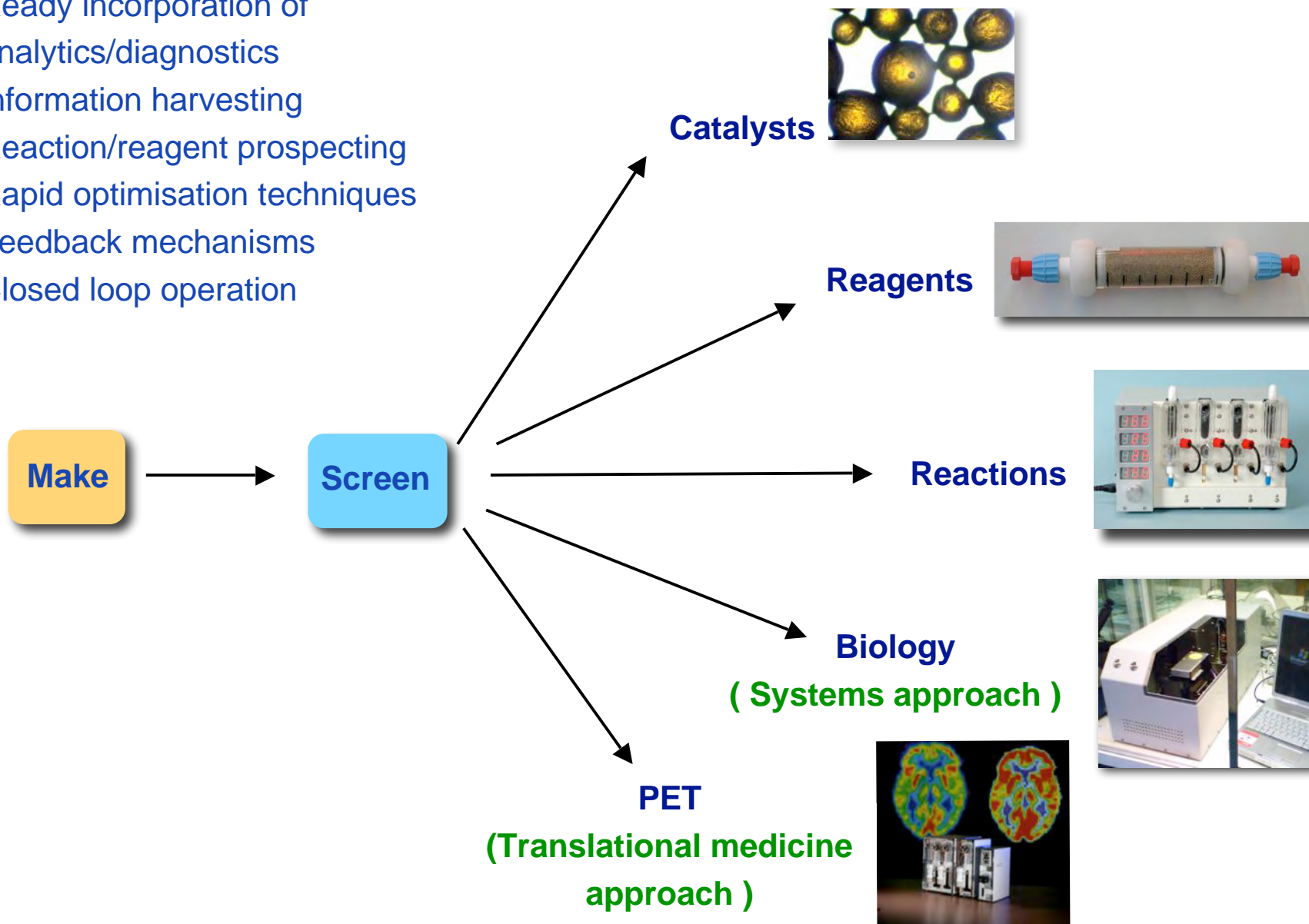
A Novel Microcapillary Flow Disc (MFD) Reactor for Organic Synthesis  
C.H. Hornung, M.R. Mackley, I.R. Baxendale and S.V. Ley and, *Org. Proc. Res. Dev.*, 2007, 11, 399.

# Typical Flow Reactor Configuration



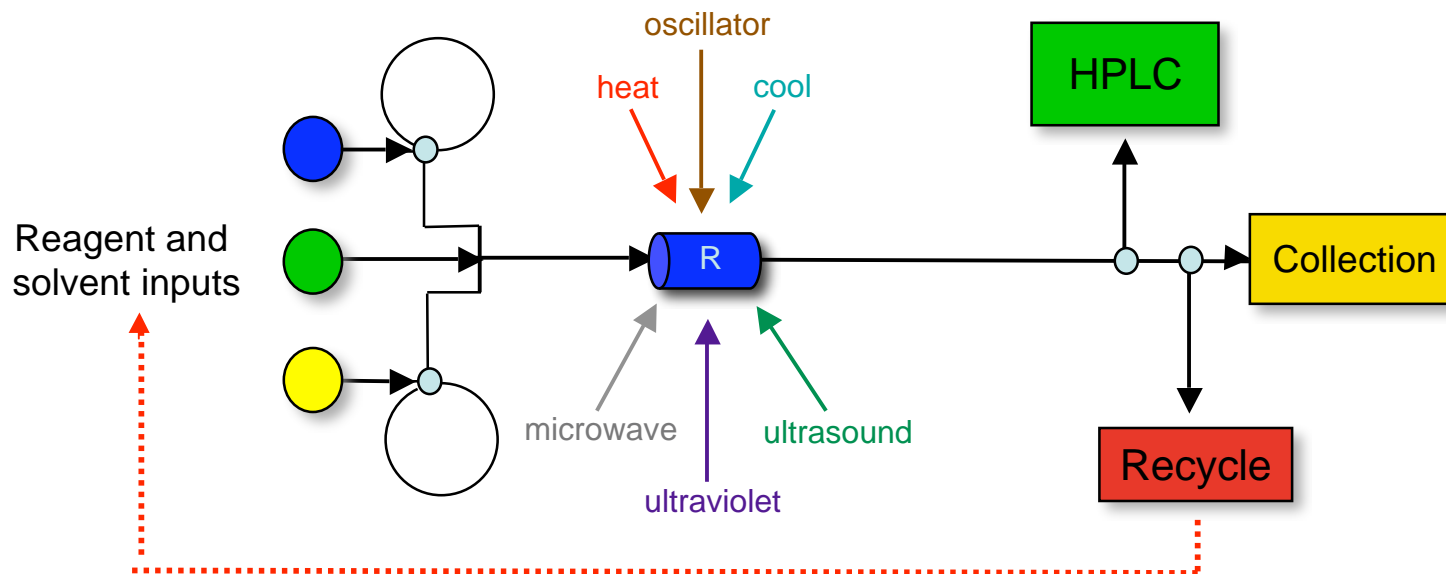
# Make and Screen Opportunities

- Ready incorporation of analytics/diagnostics
- Information harvesting
- Reaction/reagent prospecting
- Rapid optimisation techniques
- Feedback mechanisms
- Closed loop operation

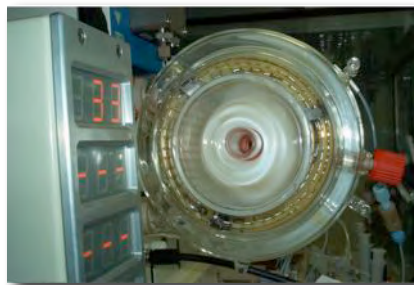
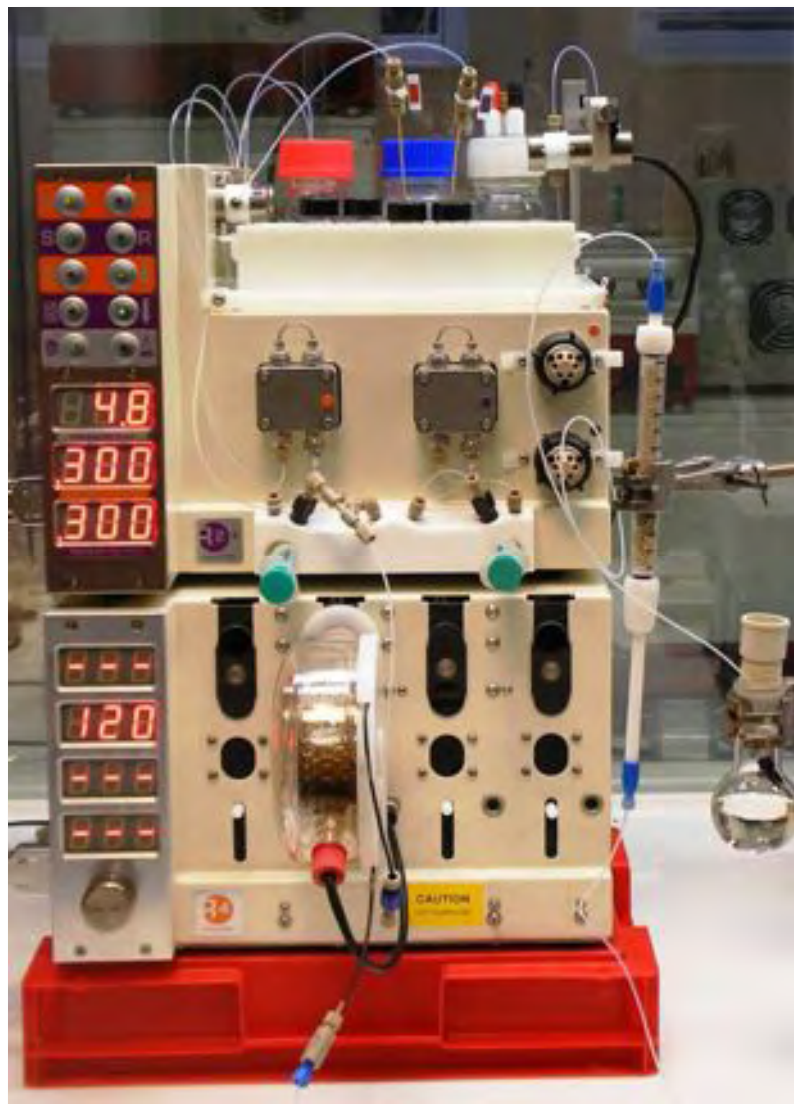




# Typical Flow Reactor Configuration



# The Flow Coil Reactors



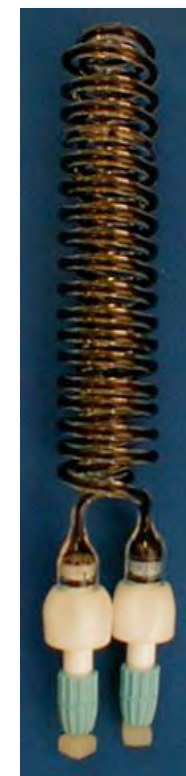
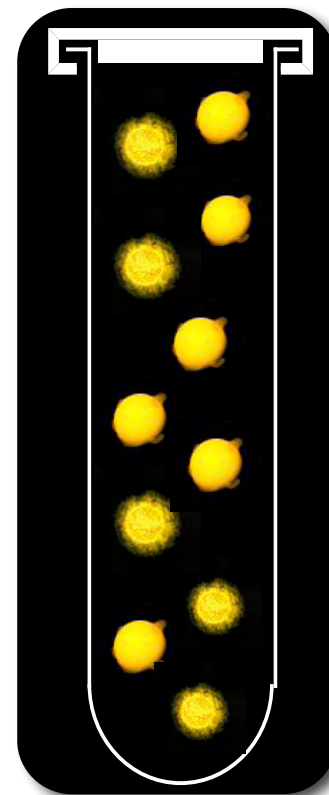
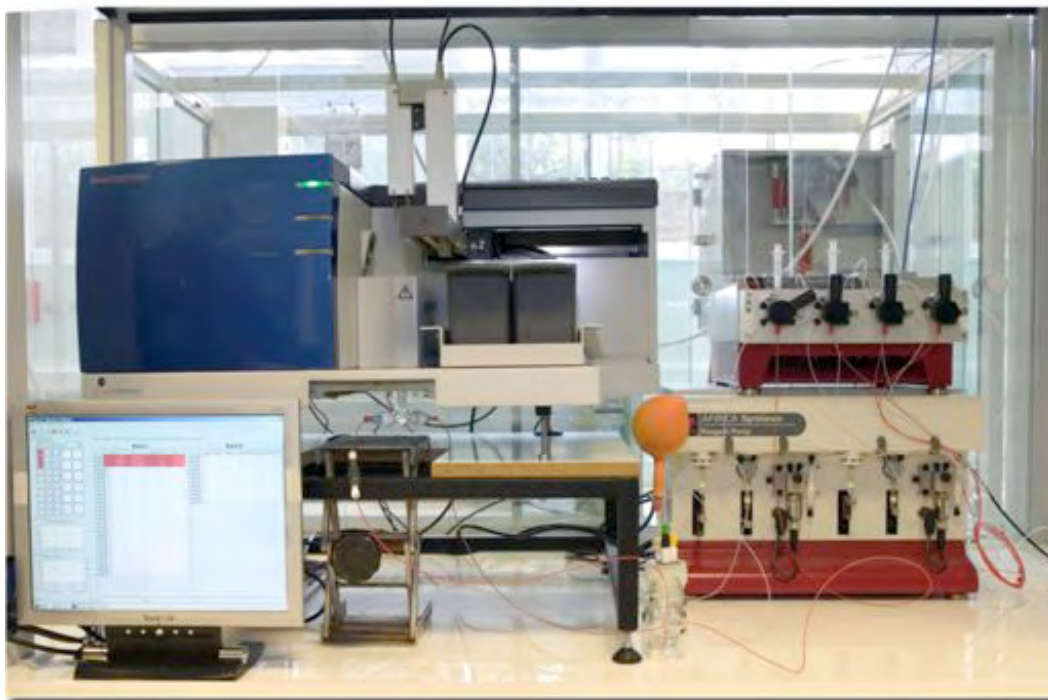
## Flow Synthesis Equipment Configuration



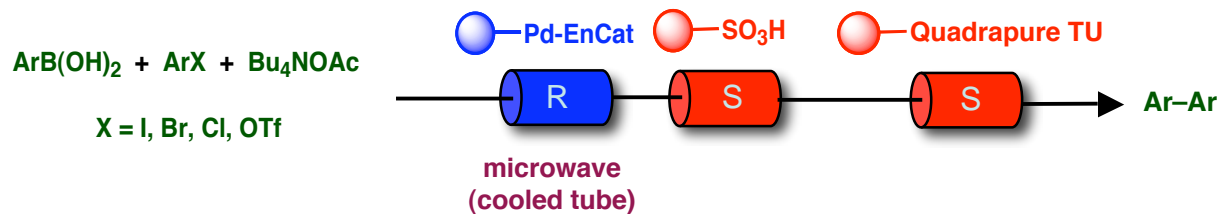
## Flow Synthesis Equipment Configuration



# Reaction Activation – Microwaves



# Suzuki Couplings

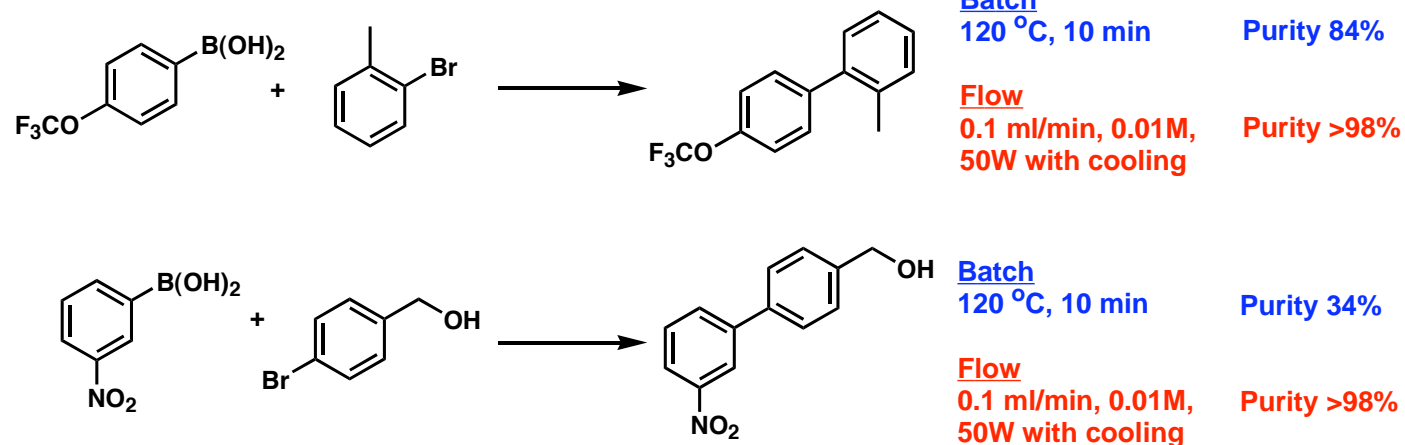


## Batch Run

374 examples from 11 boronic acids and 34 halides. Pyridine, thiophene, quinoline, pyrimidine, pyrazole, benzoxodiazole, benzofuran and biaryl compounds and sensitive functional groups e.g. aldehyde, benzyl bromide, benzyl alcohol.

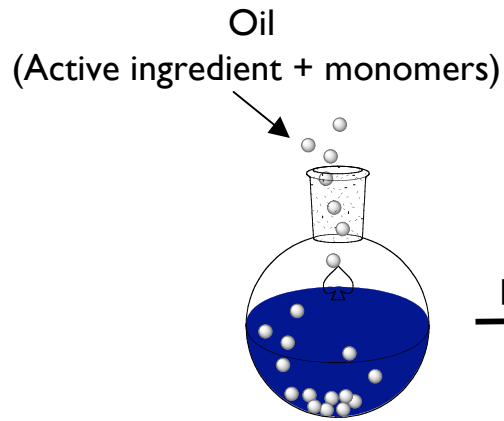
193 >80% yield, >90% purity

## Batch to Flow Comparison

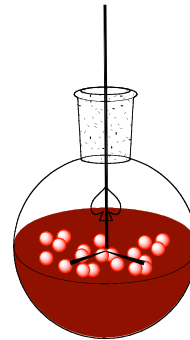


Microwave Assisted Suzuki Coupling Reactions with an Encapsulated Palladium Catalyst for Batch and Continuous Flow Transformations  
 I.R. Baxendale, C.M. Griffiths-Jones, S.V. Ley and G. Tranmer, *Chem. Eur. J.*, 2006, 12, 4407-4416.

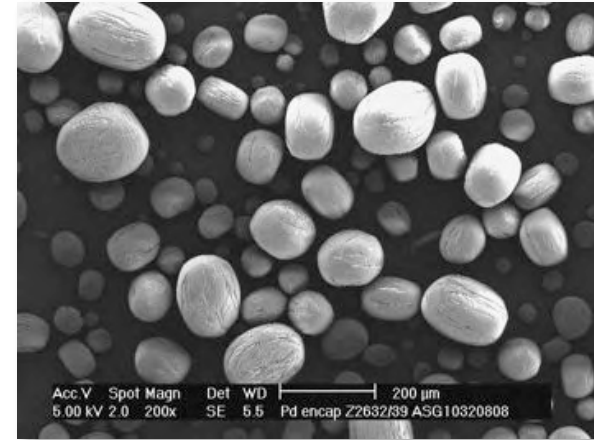
# Microcapsules Manufacturing by Interfacial Polymerisation



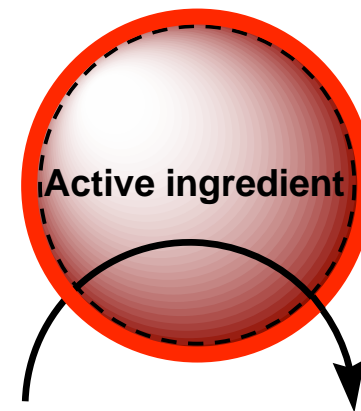
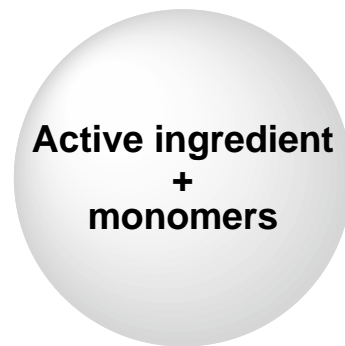
Aqueous: water, colloid stabilisers,  
emulsifiers



Wall formation



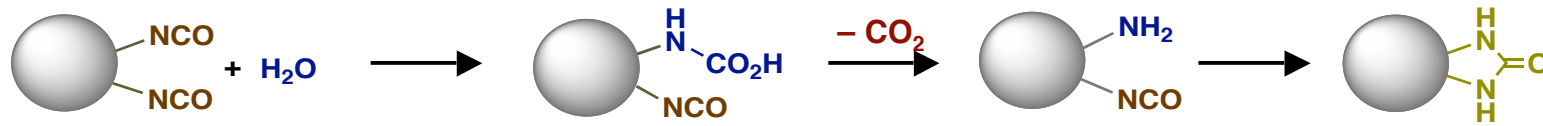
Filtered & dried EnCat™ (50-300 μm)



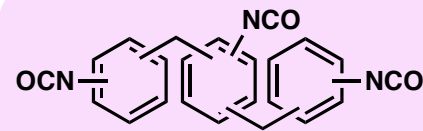
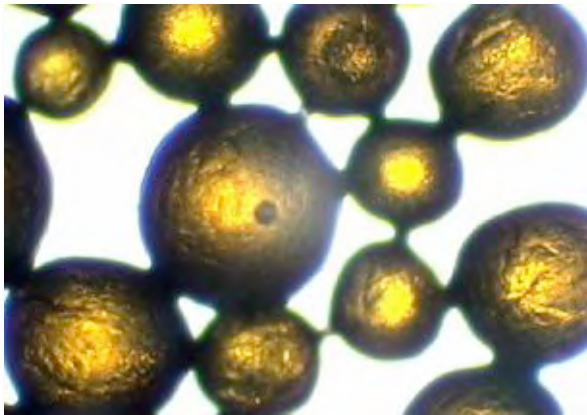
Substrate in

Product out

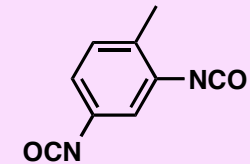
# Polyurea Microcapsules Made by In-situ Interfacial Polymerisation



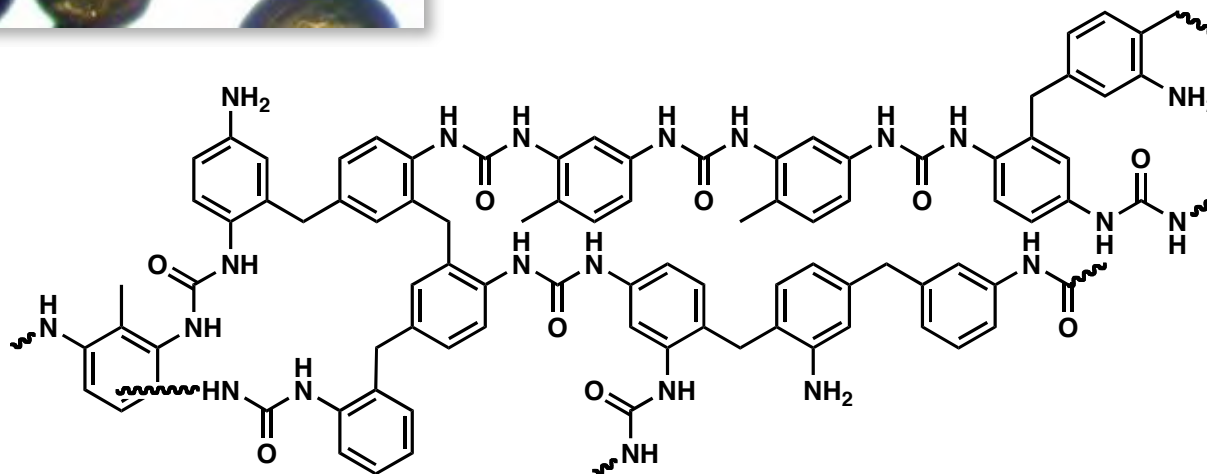
Oil droplet



Polymethylenepolypropylene isocyanate

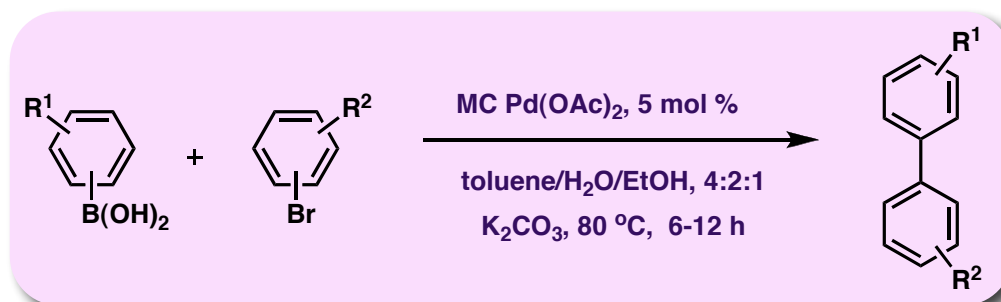


Toluene diisocyanate





# Synthesis of Biaryls Using Pd(OAc)<sub>2</sub> Encapsulated in Polyurea

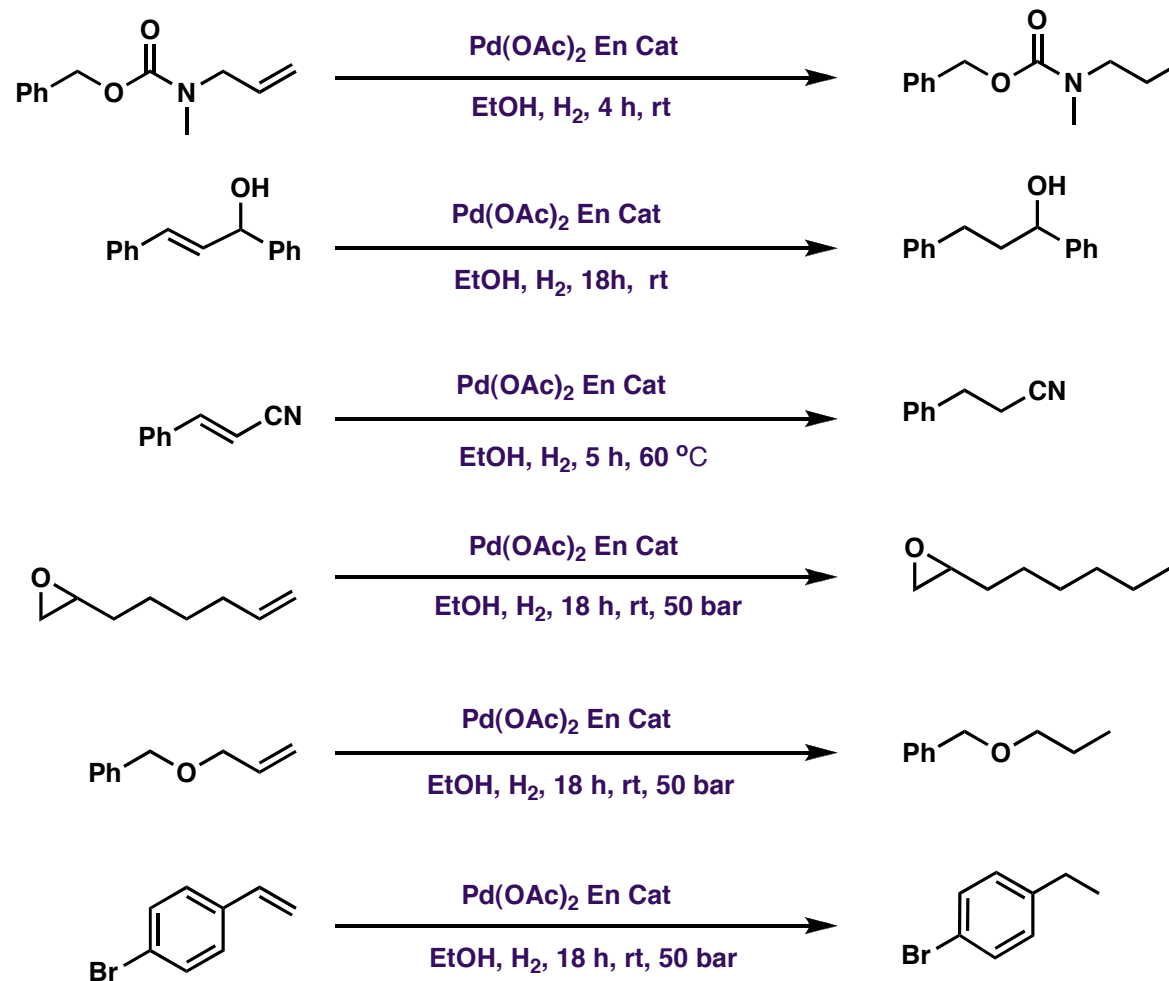


Entry	R <sup>1</sup>	R <sup>2</sup>	Yield/% <sup>†</sup>
1	<i>p</i> -OMe	<i>p</i> -OMe	87
2	<i>p</i> -OMe	<i>p</i> -F	89
3	<i>p</i> -OMe	<i>p</i> -NO <sub>2</sub>	91
4	<i>p</i> -OMe	<i>p</i> -OMe	71
5	<i>p</i> -Ac	<i>p</i> -OMe	84
6	<i>p</i> -Ac	<i>p</i> -F	90
7	<i>p</i> -Ac	<i>p</i> -NO <sub>2</sub>	97
8	H	<i>p</i> -OMe	94
9	H	<i>p</i> -F	93
10	H	<i>p</i> -NO <sub>2</sub>	97

<sup>†</sup> (%) based on isolated products. ICP Pd analysis typically 0.5-5 ppm

300 examples  
 Works in scCO<sub>2</sub>  
 Can entrap various phosphorous ligands  
 Flow reactor version

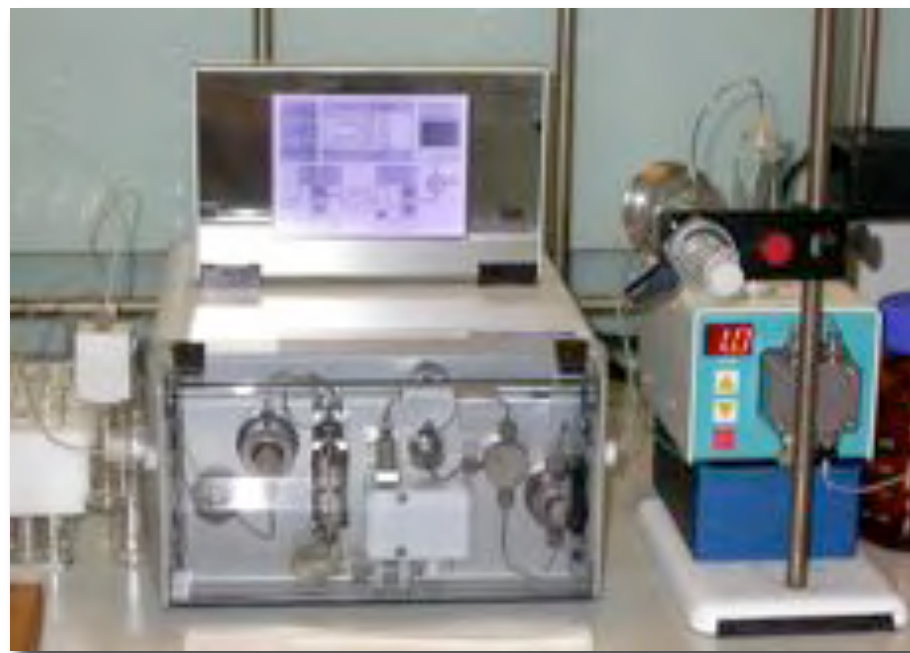
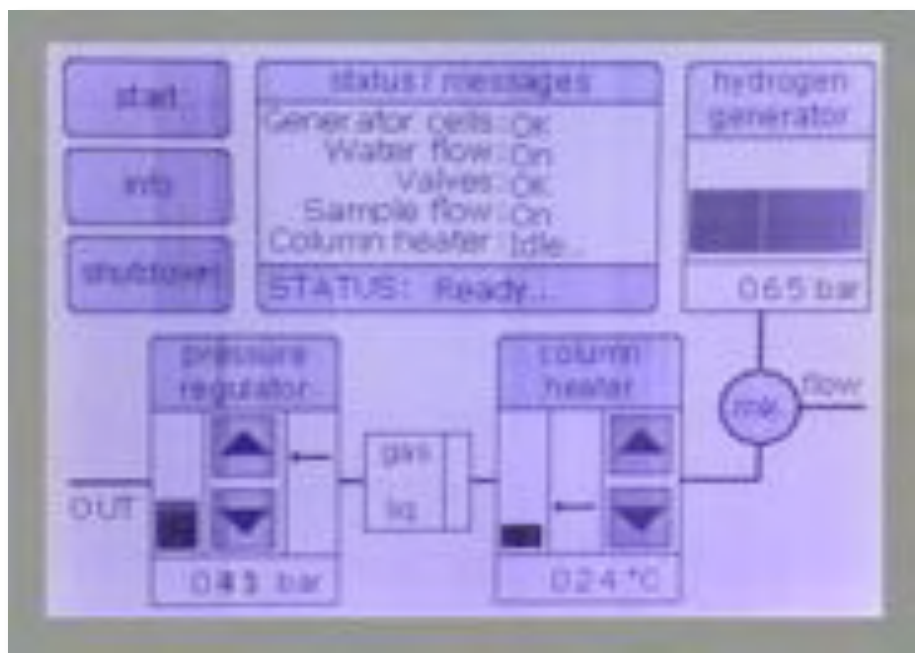
## $Pd(OAc)_2$ EnCats in Hydrogenation



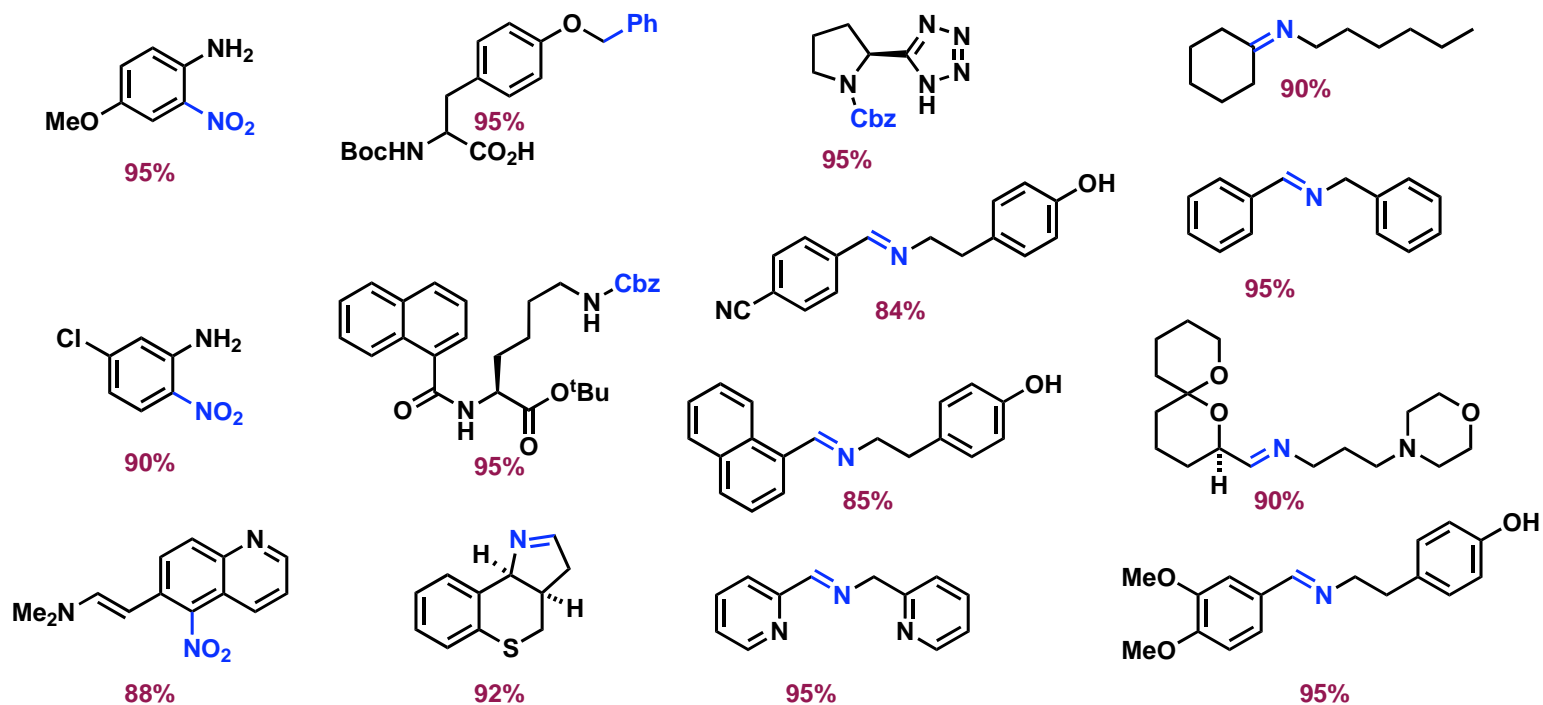
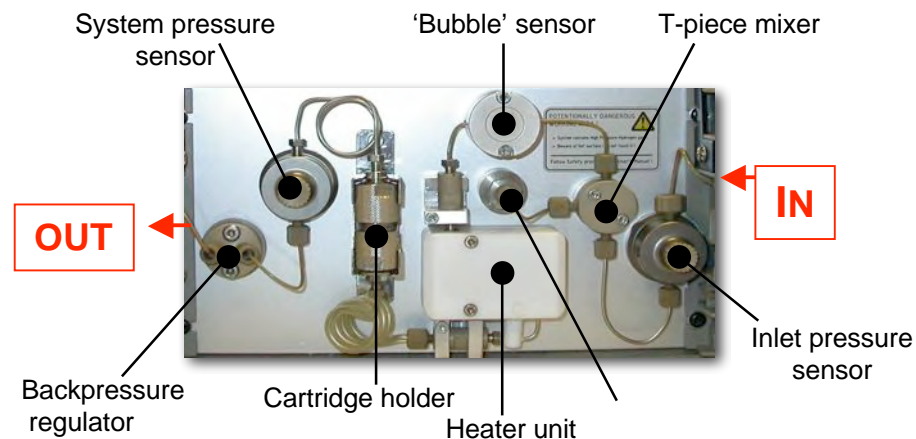
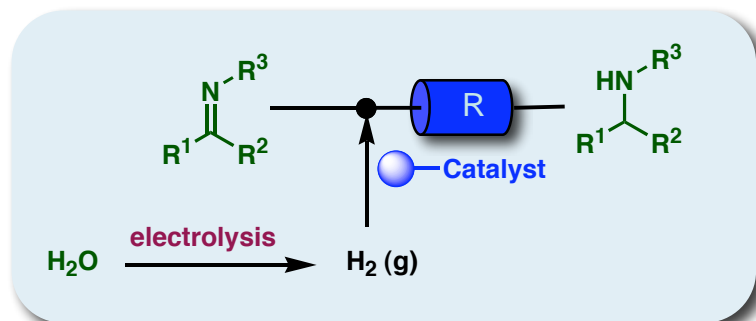
Quantitative yield up to 30x recycle

## H-Cube Flow Hydrogenator

- H-Cube generates H<sub>2</sub> gas *in situ* from the electrolysis of water (< 8 cm<sup>3</sup>).
- H<sub>2</sub> gas and a flowing solution of the substrate are mixed at a T-piece to form a mixture of gas and liquid ('bubbles').
- Mixture flows through an interchangeable metal cartridge containing a hydrogenation catalyst.
- Product mixture then flows through a backpressure regulator to a collection vial.
- **System pressure** controllable up to 100 bar
- **System temperature** is variable up 90 °C



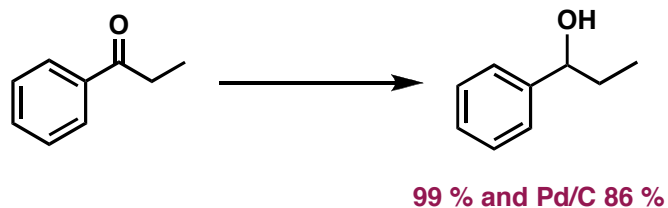
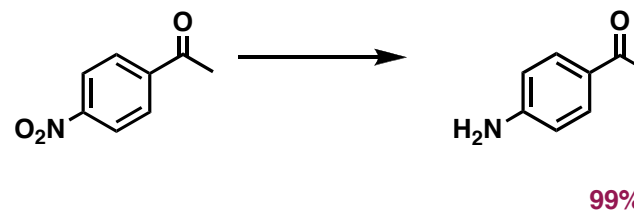
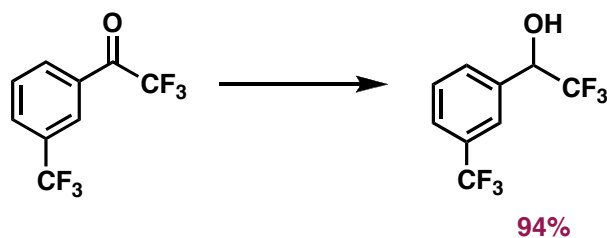
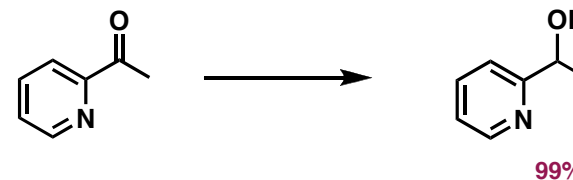
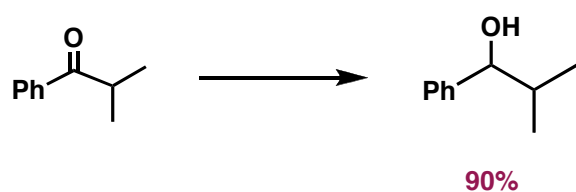
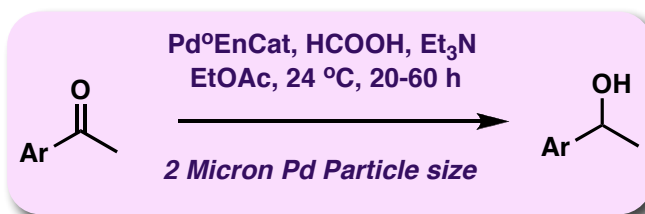
# Flow Hydrogenation in Action



The use of a Continuous Flow-Reactor Employing a Mixed Hydrogen-Liquid Flow Stream for the Efficient Reduction of Imines to Amines  
 S. Saaby, K.R. Knudsen, M. Ladlow and S.V. Ley, *J. Chem. Soc., Chem. Commun.*, **2005**, 2909-2911.

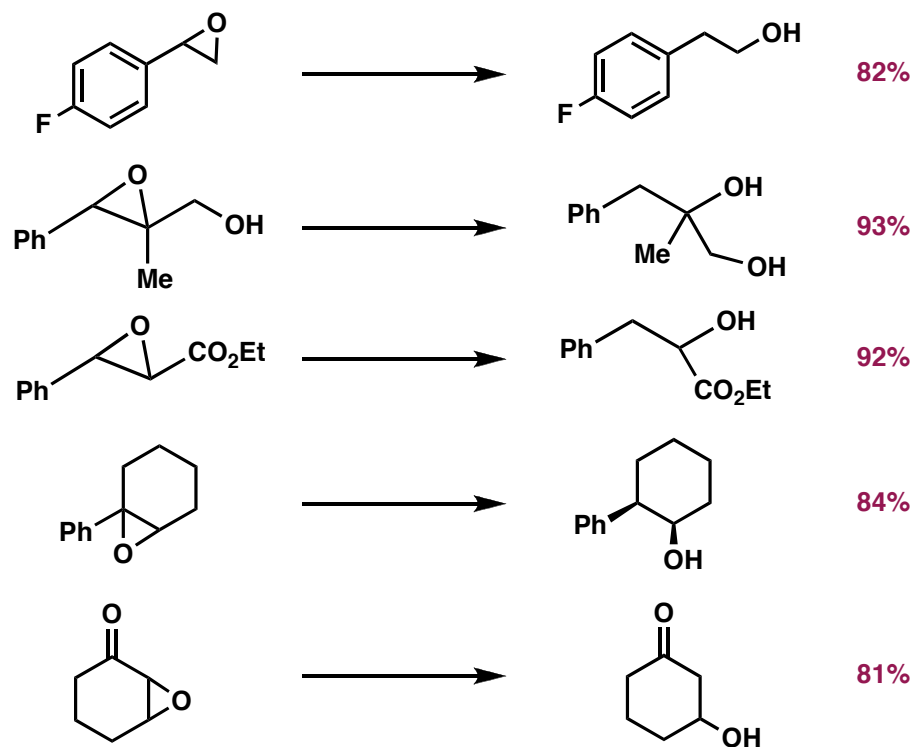
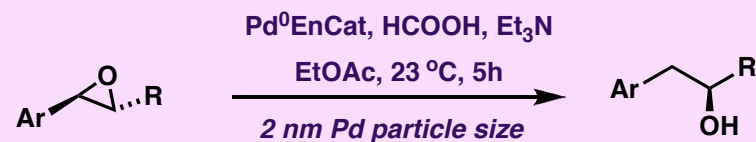
Optimisation of Conditions for *O*-Benzyl and *N*-Benzyloxycarbonyl Protecting Group Removal using an Automated Flow Hydrogenator  
 K.R. Knudsen, J. Holden, S.V. Ley and M. Ladlow, *Adv. Syn. Cat.*, **2007**, 349, 535-538

# EnCat Pd(0) in Polyurea – For Hydrogen Transfer Reduction of Aryl Ketones



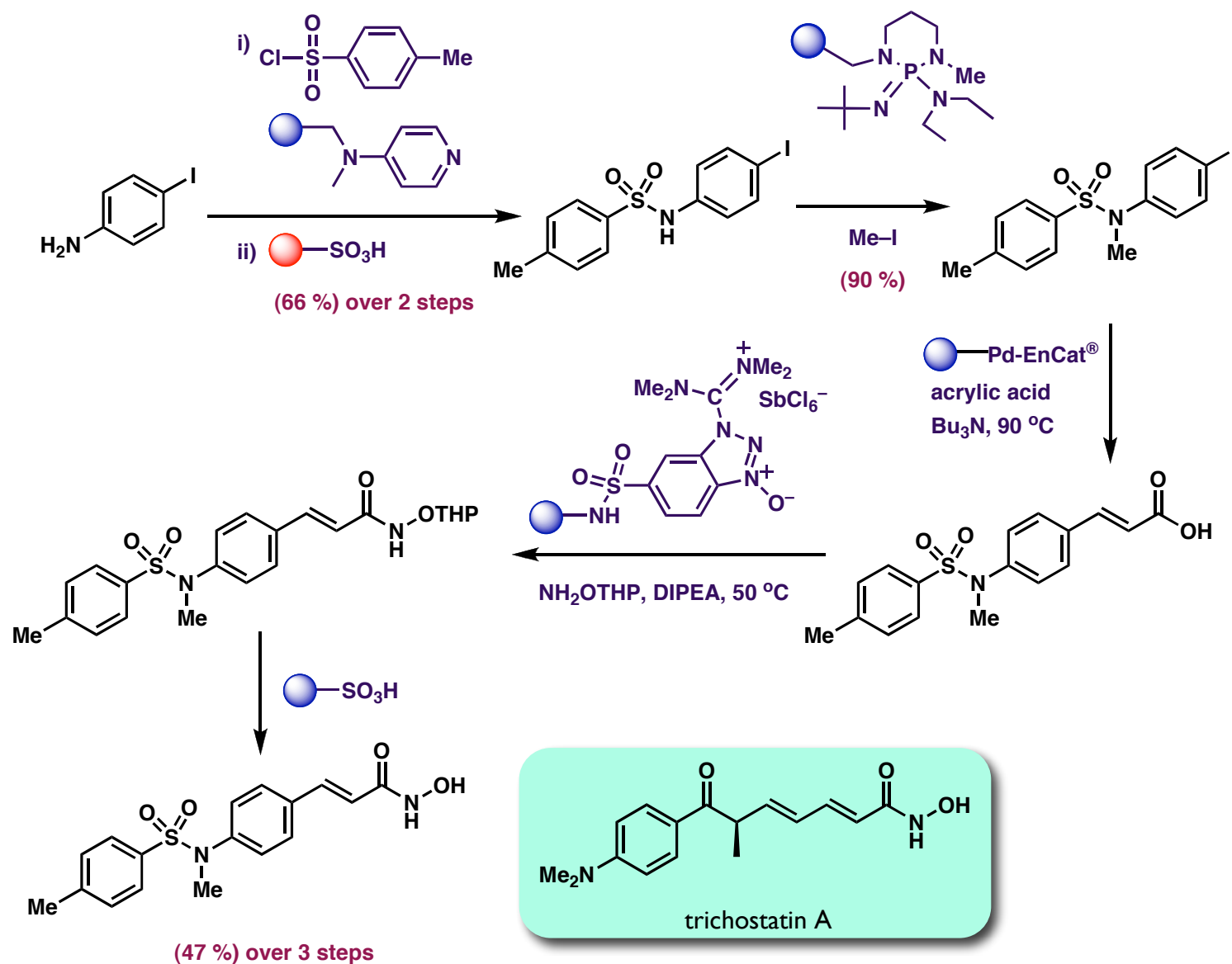
Recycle up to 10+ times

# EnCat Pd(0) in Polyurea – For Hydrogenolysis of Epoxides

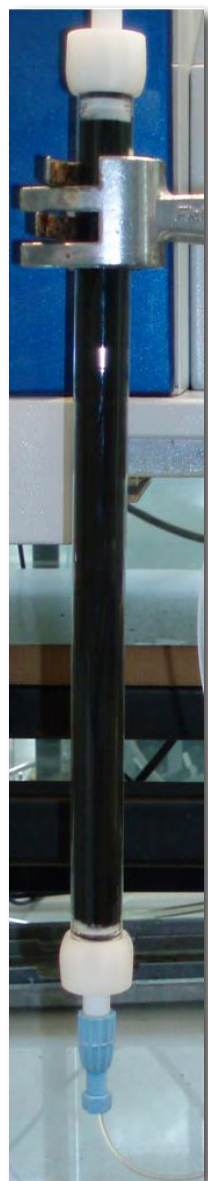


Recycle up to 10+ times

# Synthesis of Histone Deacetylase Inhibitors

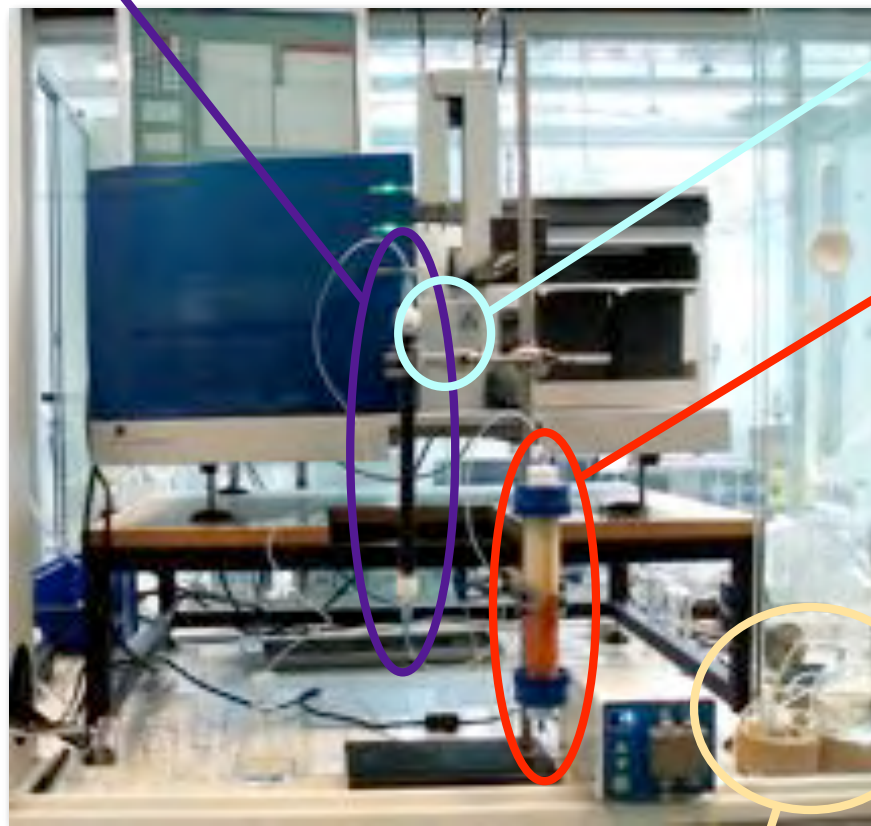
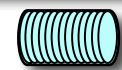


# Synthesis of Pyrazole Dimers

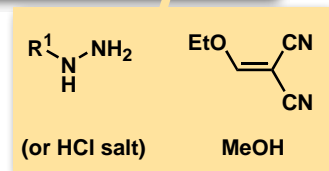
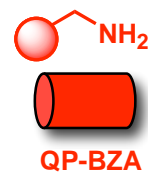


Activated carbon

MW 100 °C  
10 min

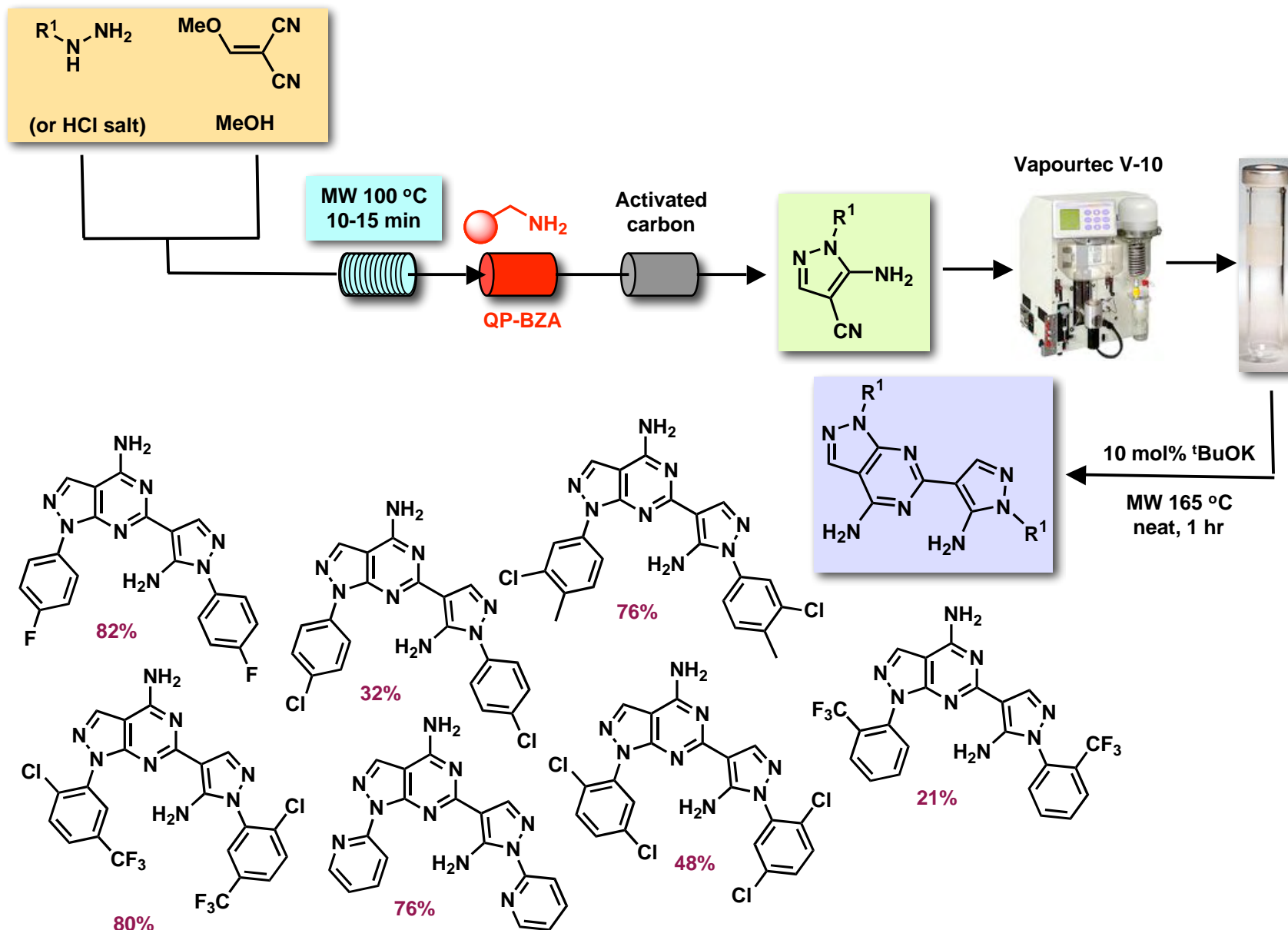


Amine scavenger





# Synthesis of Pyrazole Dimers

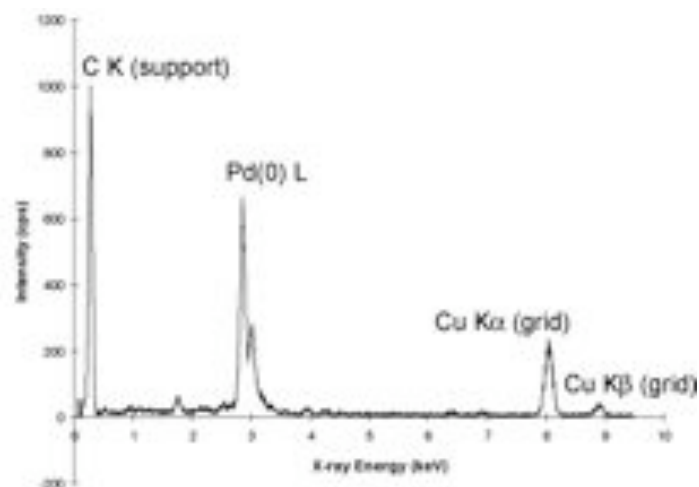
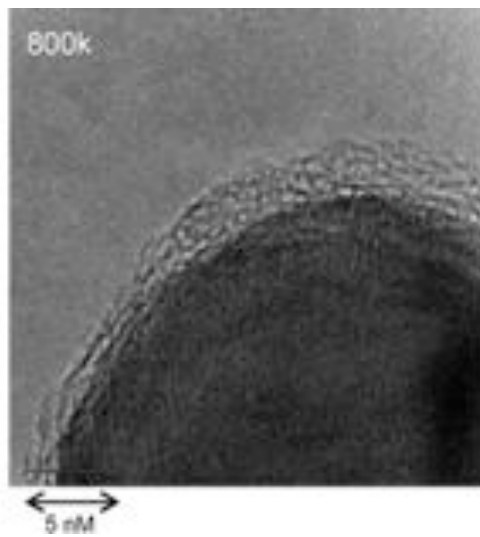
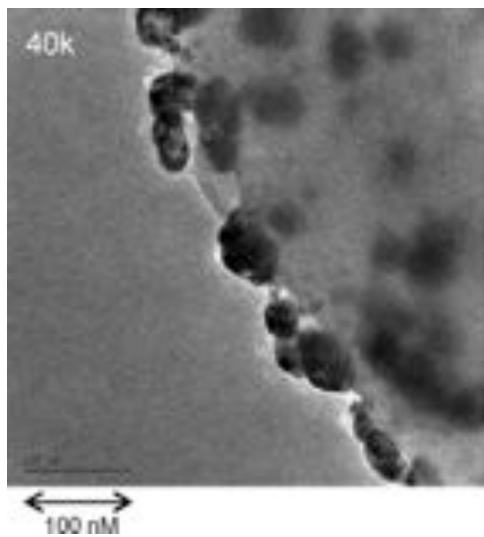
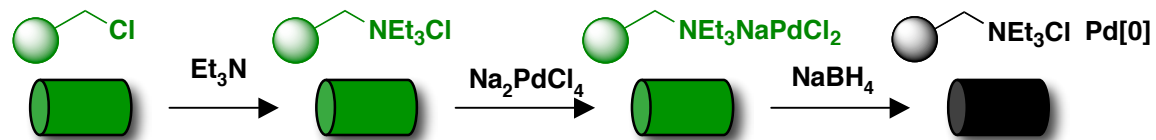
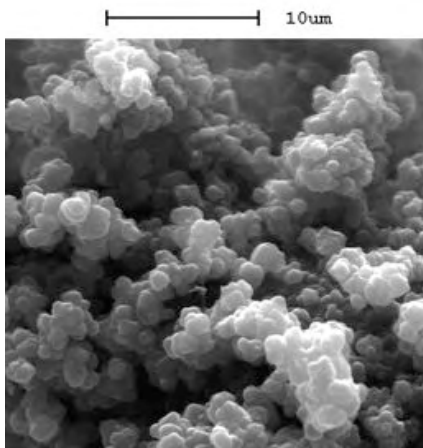


## *Monolith Preparation*

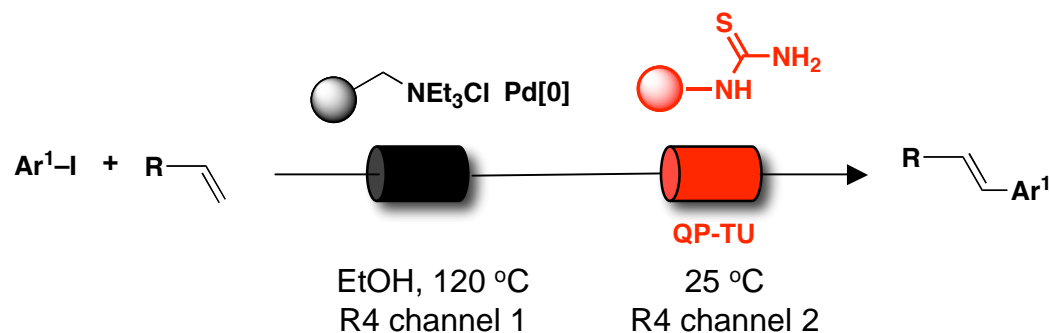


*High loading capacity  
Macroporous polymer  
Inexpensive  
Easy to prepare  
Available in a variety of materials*

# Nanoparticulate Monolith Pd



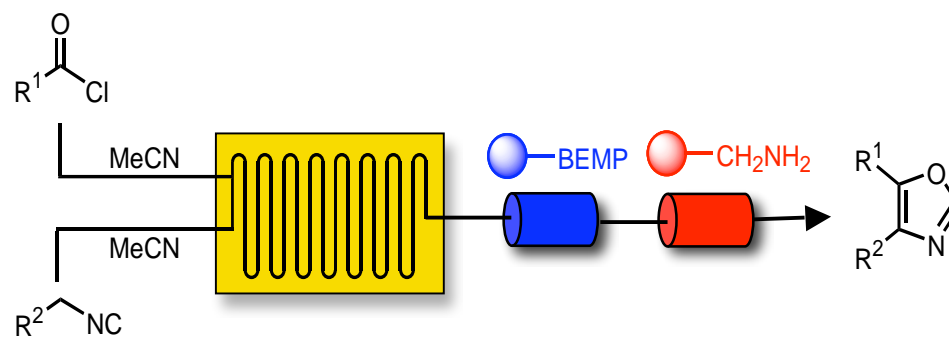
# Nanoparticulate Monolith Pd in Heck Reactions



Flow rate 0.05 mL/min  
 ICP analysis <5 ppm Pd  
 Column reused 50 times  
 Lithograph surface area 5 m<sup>2</sup>/g

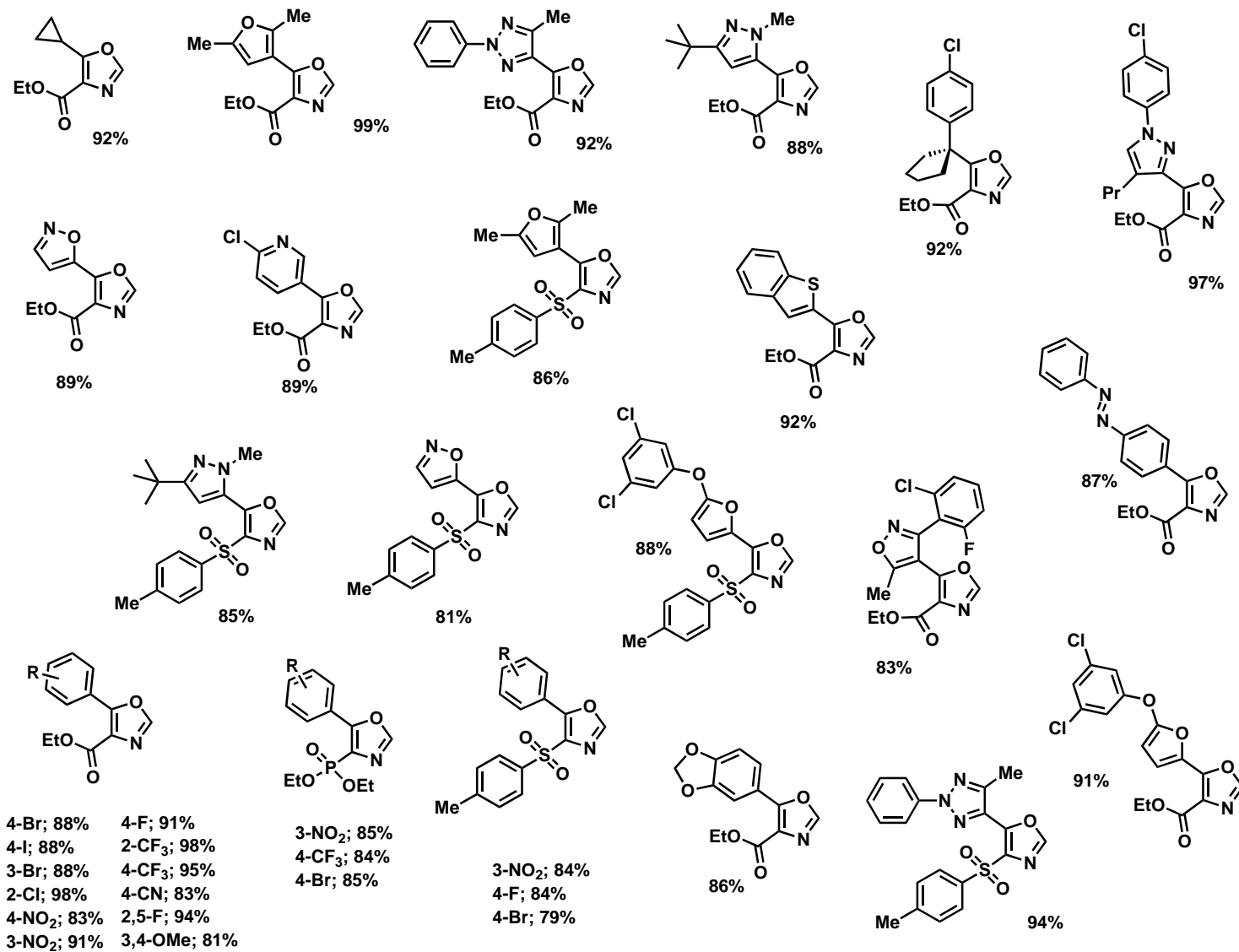
Aryl Halide	Alkene	Product	Conversion (%)	Purity	Yield (%)
			100	>99	86
			100	>95	87
			100	>95	88
			100	>95	87
			100	>95	88
			100	>99	79
			100	>99	85
			100	>99	78
			100	>99	73

# Synthesis of Oxazoles in Flow



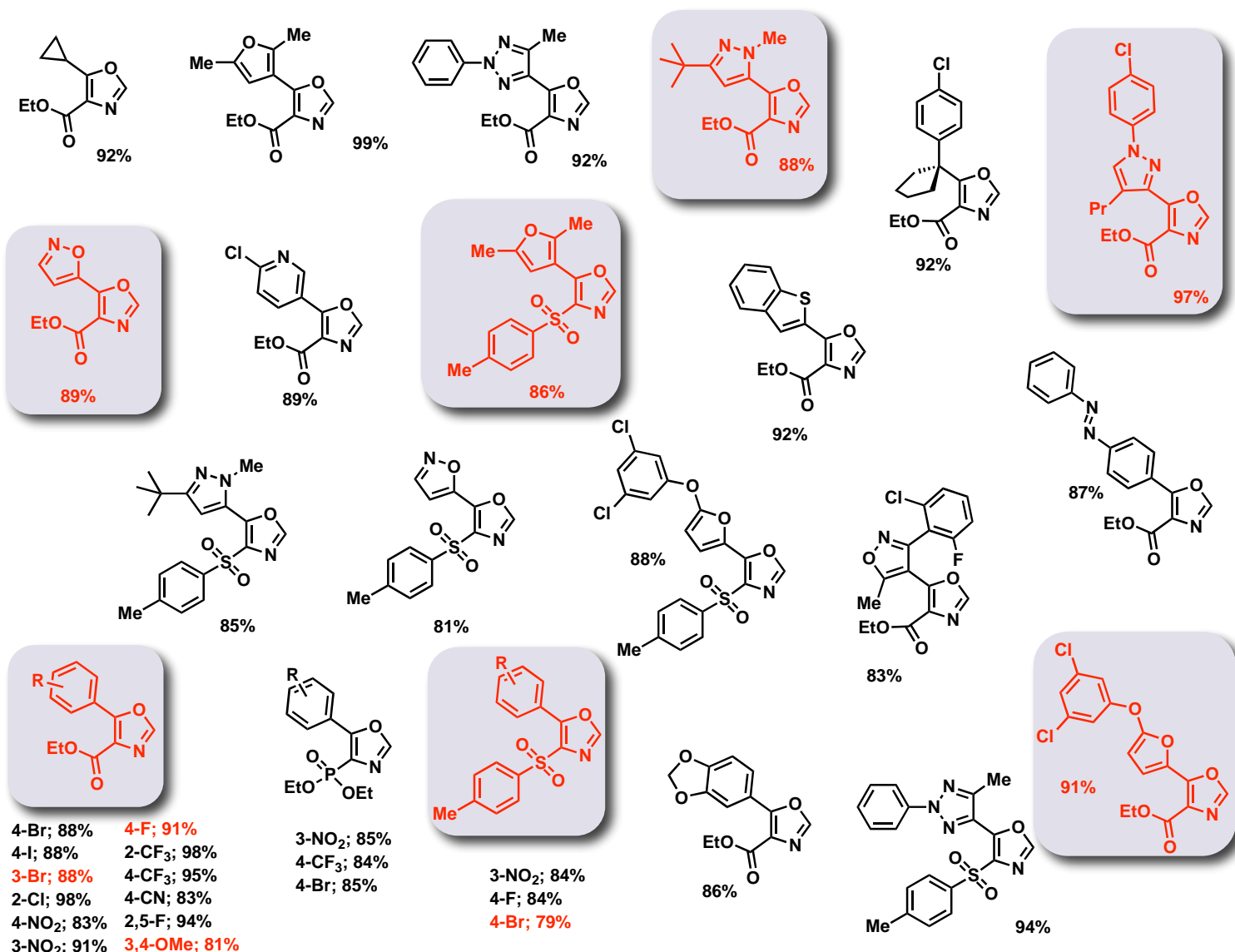
A Fully Automated Continuous Flow Synthesis of 4,5-Disubstituted Oxazoles,  
M. Baumann, I.R. Baxendale, S.V. Ley, C.D. Smith and G.K. Tranmer, *Org. Lett.*, 2006, 8, 5231-5234.

# Synthesis of Oxazoles in Flow



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# Synthesis of Oxazoles in Flow

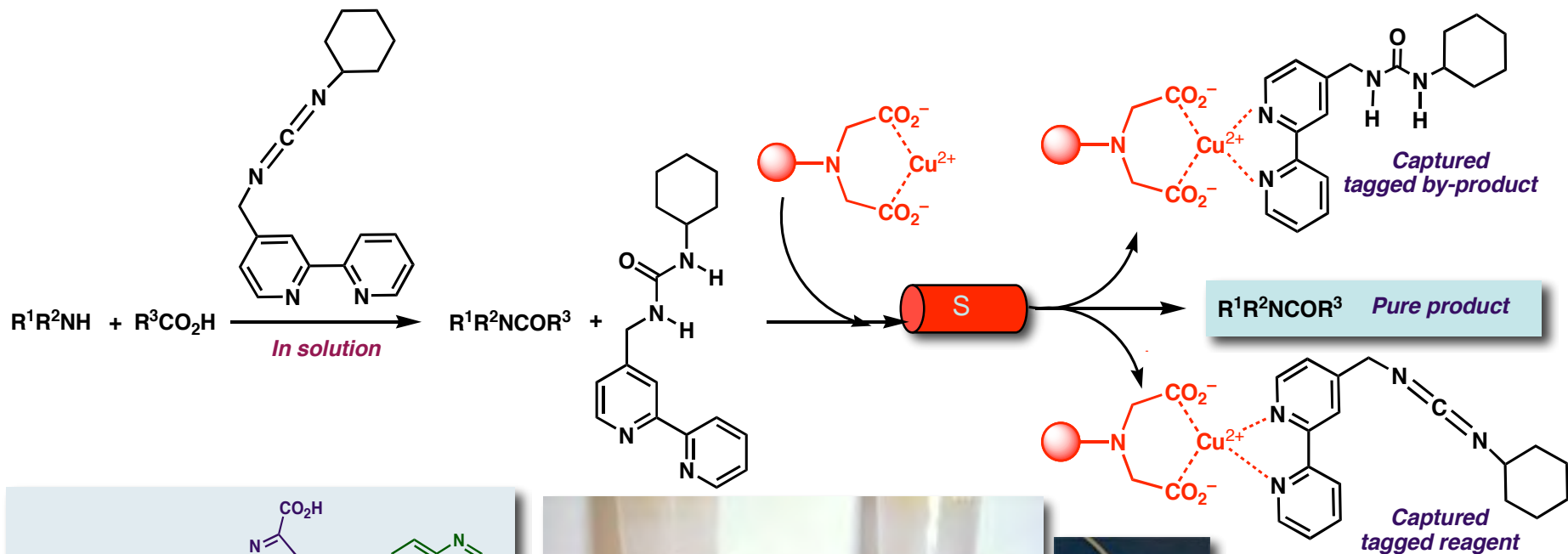


- 4-Br; 88%
- 4-I; 88%
- 3-Br; 88%
- 2-Cl; 98%
- 4-NO<sub>2</sub>; 83%
- 3-NO<sub>2</sub>; 91%
- 4-F; 91%
- 2-CF<sub>3</sub>; 98%
- 4-CF<sub>3</sub>; 95%
- 4-CN; 83%
- 2,5-F; 94%
- 3,4-OMe; 81%

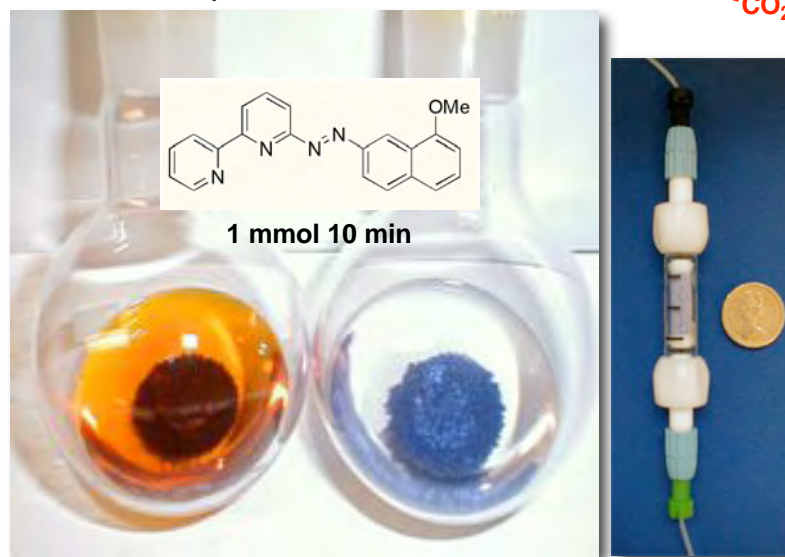
oxazole preparations scaled to >10g

A Fully Automated Continuous Flow Synthesis of 4,5-Disubstituted Oxazoles,  
 M. Baumann, I.R. Baxendale, S.V. Ley, C.D. Smith and G.K. Tranmer, *Org. Lett.*, 2006, 8, 5231-5234.

# Reagent Phase Switch Tagging Techniques



Amine	Yield (%)	Yield (%)
	87%	83%
	91%	89%
	90%	85%

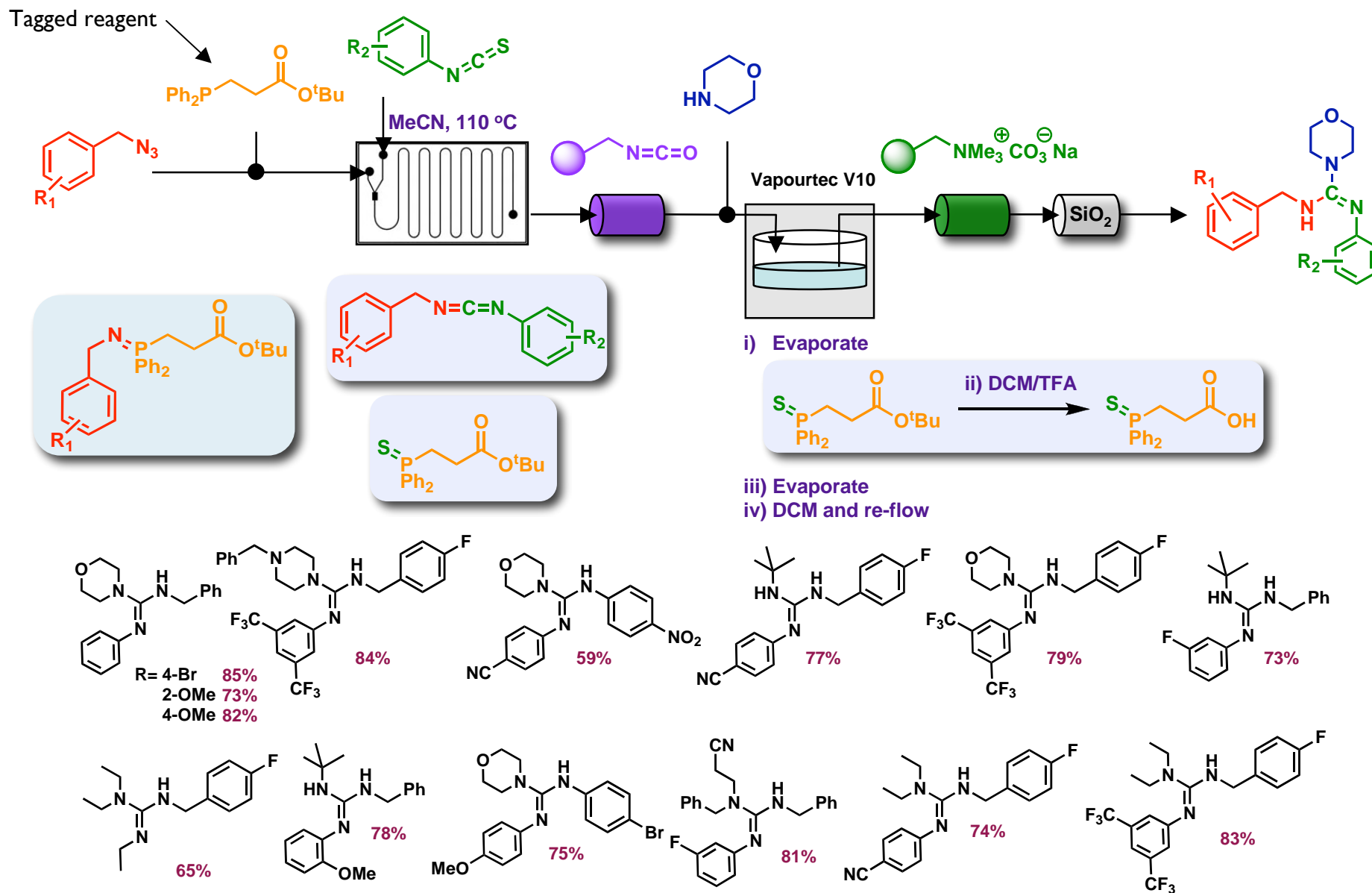


A Phase-Switch Purification Approach for the Expedient Removal of Tagged Reagents and Scavengers Following their Application in Organic Synthesis

J. Siu, I.R. Baxendale, R.A. Lewthwaite and S.V. Ley, *Org. Biomol. Chem.*, 2005, 3, 3140-3160.

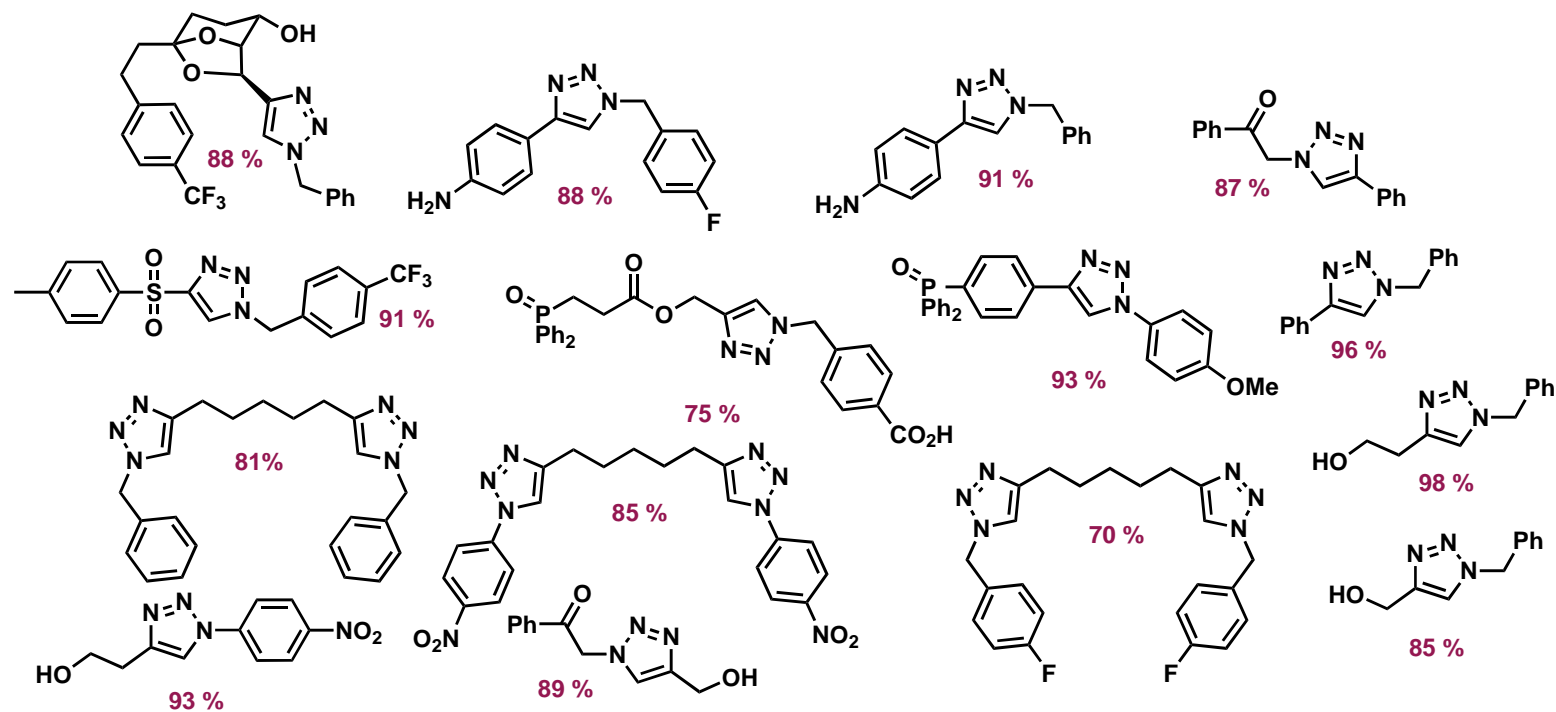
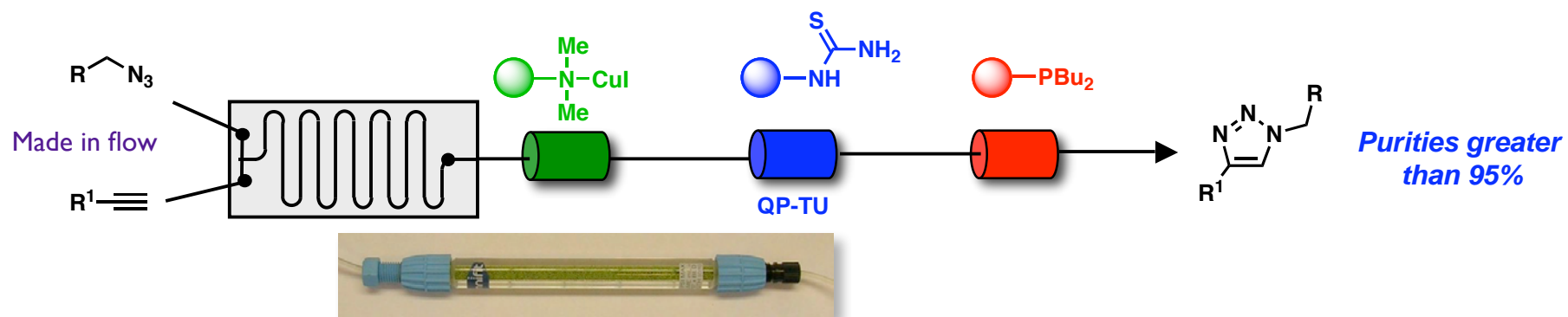


# Tagged Reagents in Flow – Synthesis of Guanidines



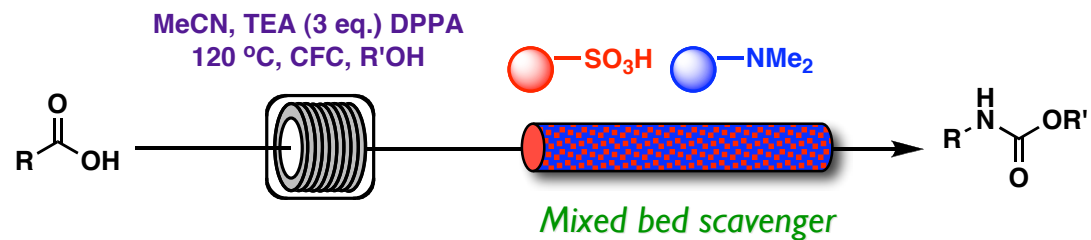
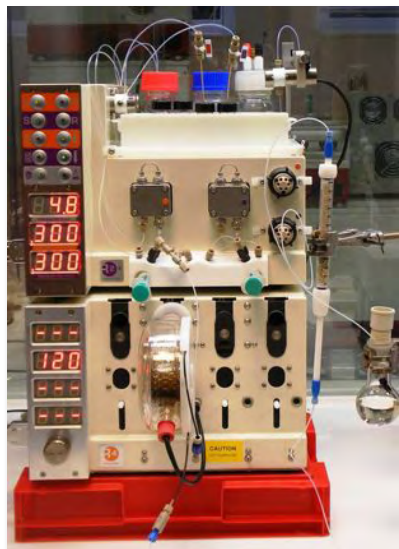
Tagged Phosphine Reagents to Assist Reaction Work-up by Phase-Switched Scavenging Using a Modular Flow Reactor Process. C.D. Smith, I.R. Baxendale, G.K. Tranmer, M. Baumann, S.C. Smith, R.A. Lewthwaite and S.V. Ley, *Org. Biomol. Chem.*, 2007, 5, 1562-1568

# Azide Couplings in Flow

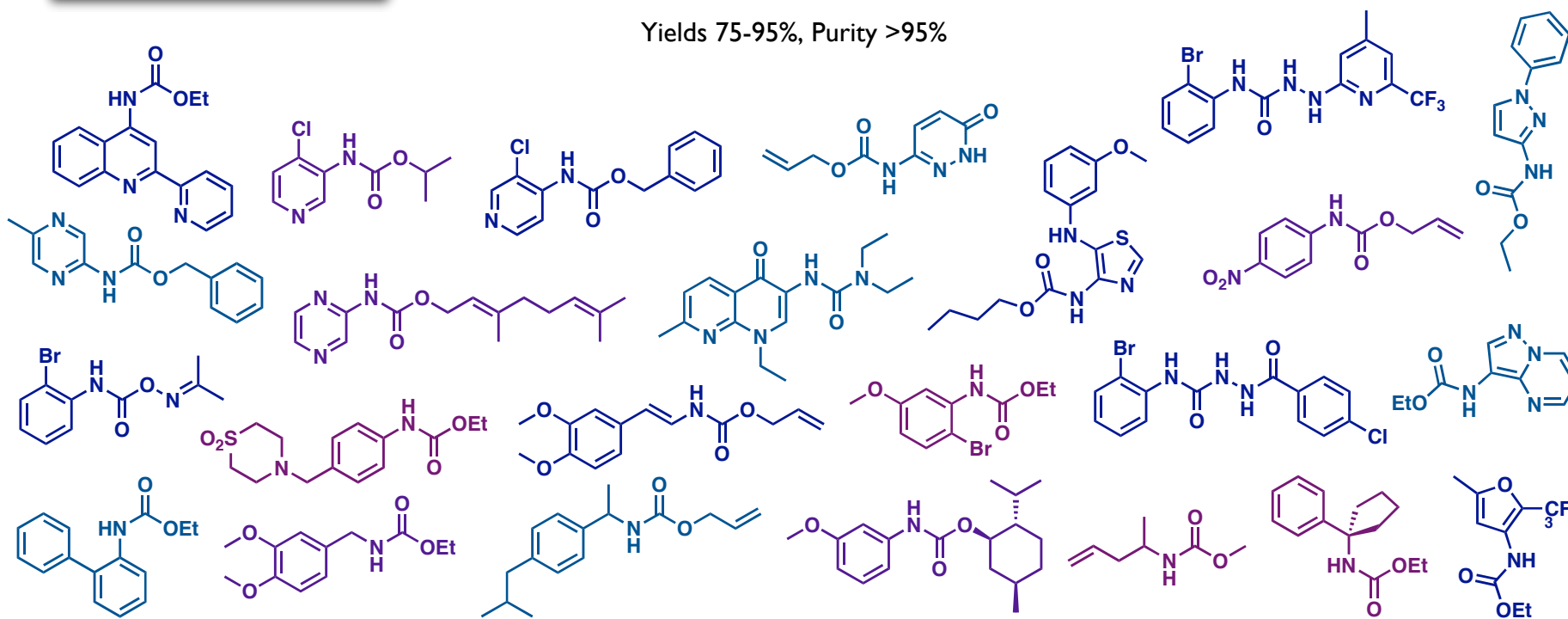


[3 + 2] Cycloaddition of Acetylenes with Azides to give 1,4-Disubstituted 1,2,3- Triazoles in a Modular Flow Reactor  
 C.D. Smith, I.R. Baxendale, S. Lanners, J.J. Hayward, S.C. Smith and S.V. Ley, *Org. Biomol. Chem.*, 2007, 5, 1559-1561.

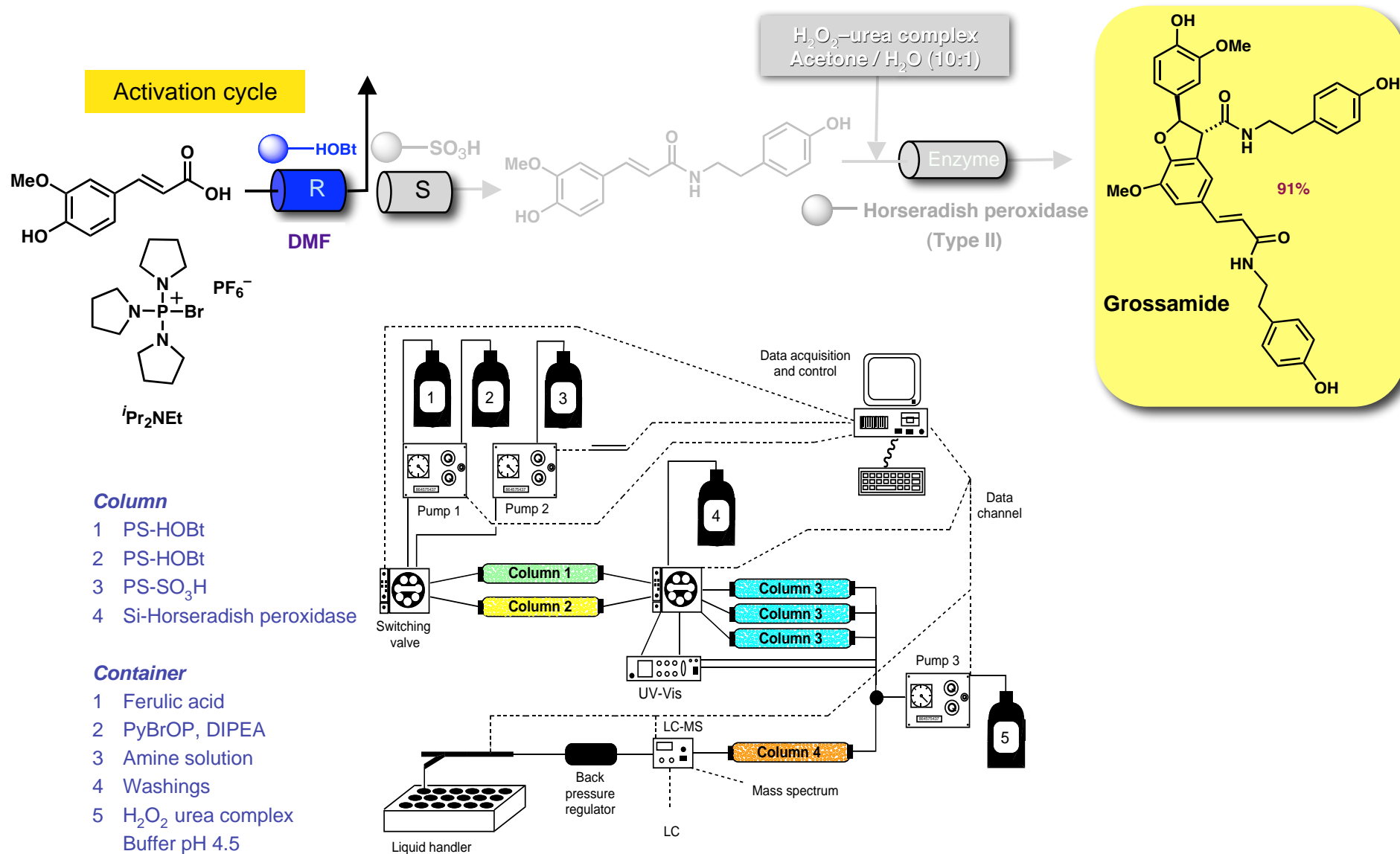
# Curtius Rearrangements in Flow



Yields 75-95%, Purity >95%

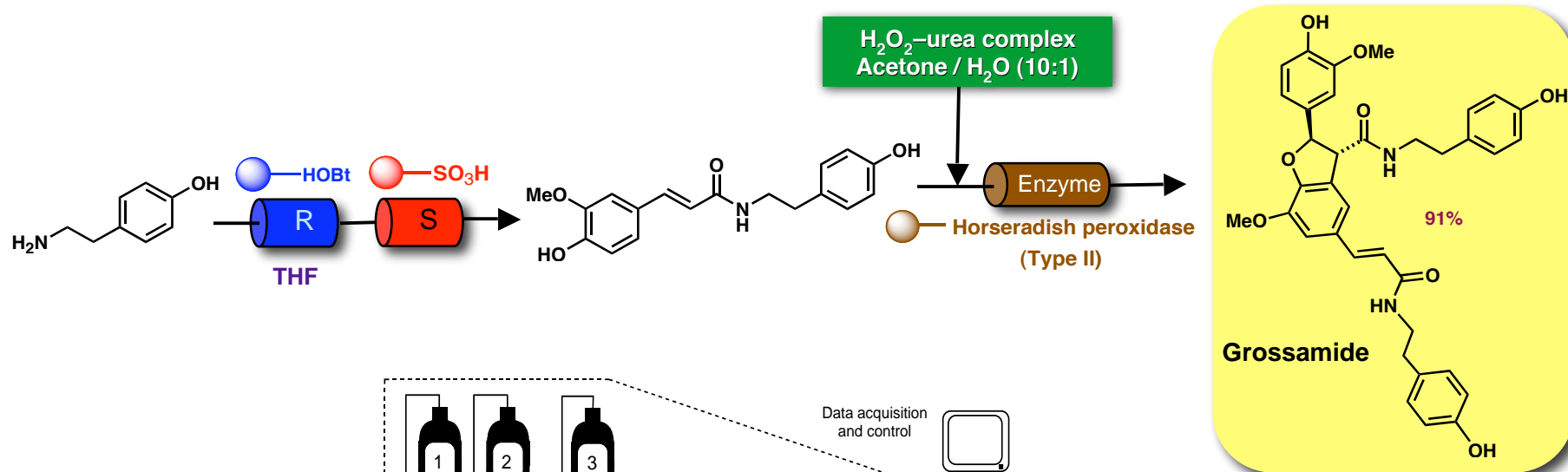


# Flow Synthesis of Grossamide using Immobilized Enzymes



Preparation of the Neolignan Natural Product Grossamide by a Continuous Flow Process  
I.R. Baxendale, C.M. Griffiths-Jones, S.V. Ley and G.K. Tranmer, *Synlett*, 2006, 427-430

# Flow Synthesis of Grossamide using Immobilized Enzymes

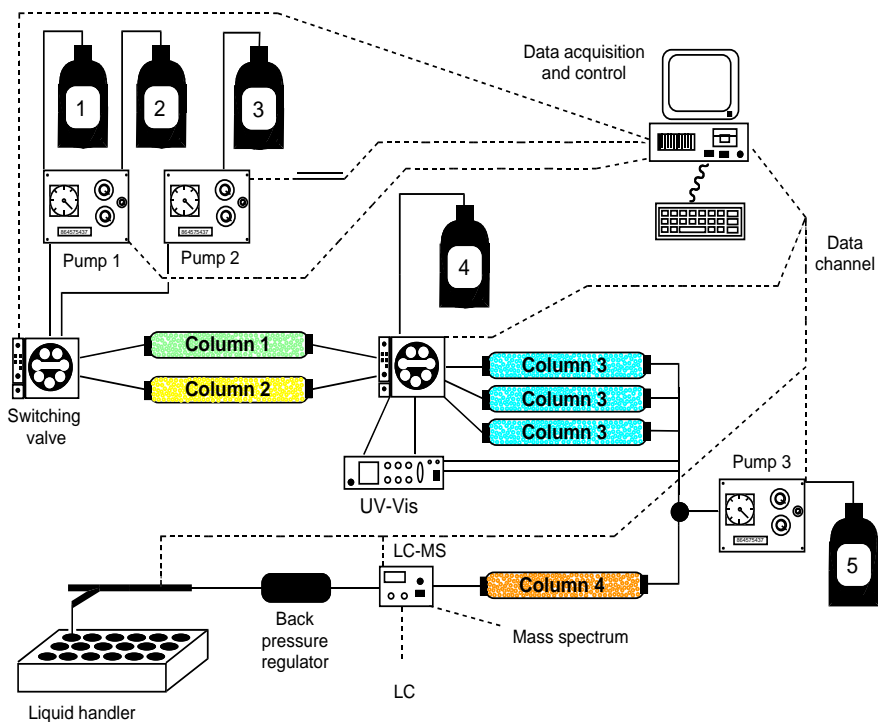


## Column

- 1 PS-HOBt
- 2 PS-HOBt
- 3 PS-SO<sub>3</sub>H
- 4 Si-Horseradish peroxidase

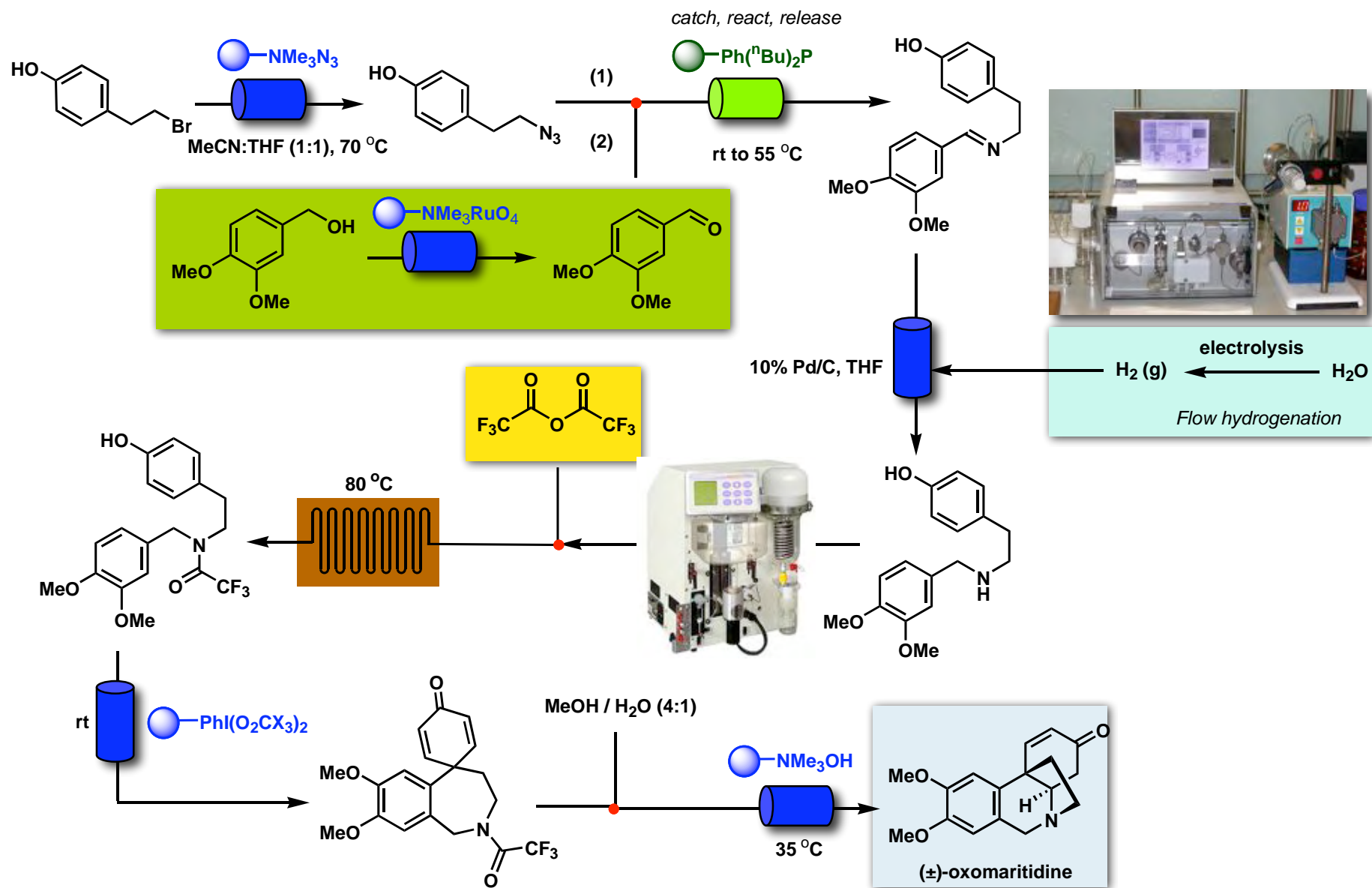
## Container

- 1 Ferulic acid
- 2 PyBrOP, DIPEA
- 3 Amine solution
- 4 Washings
- 5 H<sub>2</sub>O<sub>2</sub> urea complex  
Buffer pH 4.5

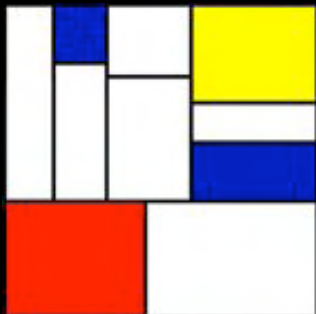


Preparation of the Neolignan Natural Product Grossamide by a Continuous Flow Process  
I.R. Baxendale, C.M. Griffiths-Jones, S.V. Ley and G.K. Tranmer, *Synlett*, 2006, 427-430

# Convergent Flow Synthesis of Oxomaritidine



A Flow Process for the Multi-Step Synthesis of the Alkaloid Natural Product Oxomaritidine: A New Paradigm for Molecular Assembly  
I.R.Baxendale, J.Deeley, C.M.Griffiths-Jones, S.V. Ley, S.Saaby, G.K.Tranmer, *J. Chem. Soc., Chem. Commun.* 2007, 2566-2568.



I.R. Baxendale

C.H. Hornung  
C.M. Griffiths-Jones  
G.K. Tranmer  
N. Bremeyer  
C. Ramarao  
C.J. Smith  
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M. Ladlow, J. Tierney, B.H. Warrington (GSK)  
R.A. Lewthwaite and C. Selway (Pfizer)  
I.M. Shirley and S.C. Smith (Syngenta)  
D. Pears (Reaxa)

EPSRC, Merck, Pfizer, GSK, AstraZeneca, Novartis

