

Silica removal from natural waters on a New Organic-Inorganic Hybrid Ion Exchanger

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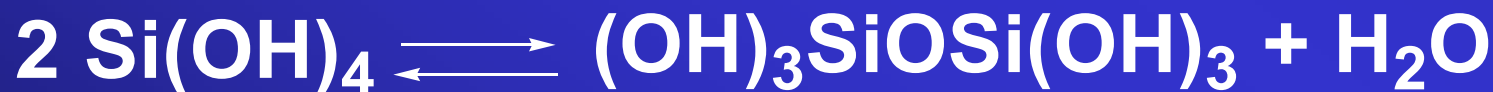
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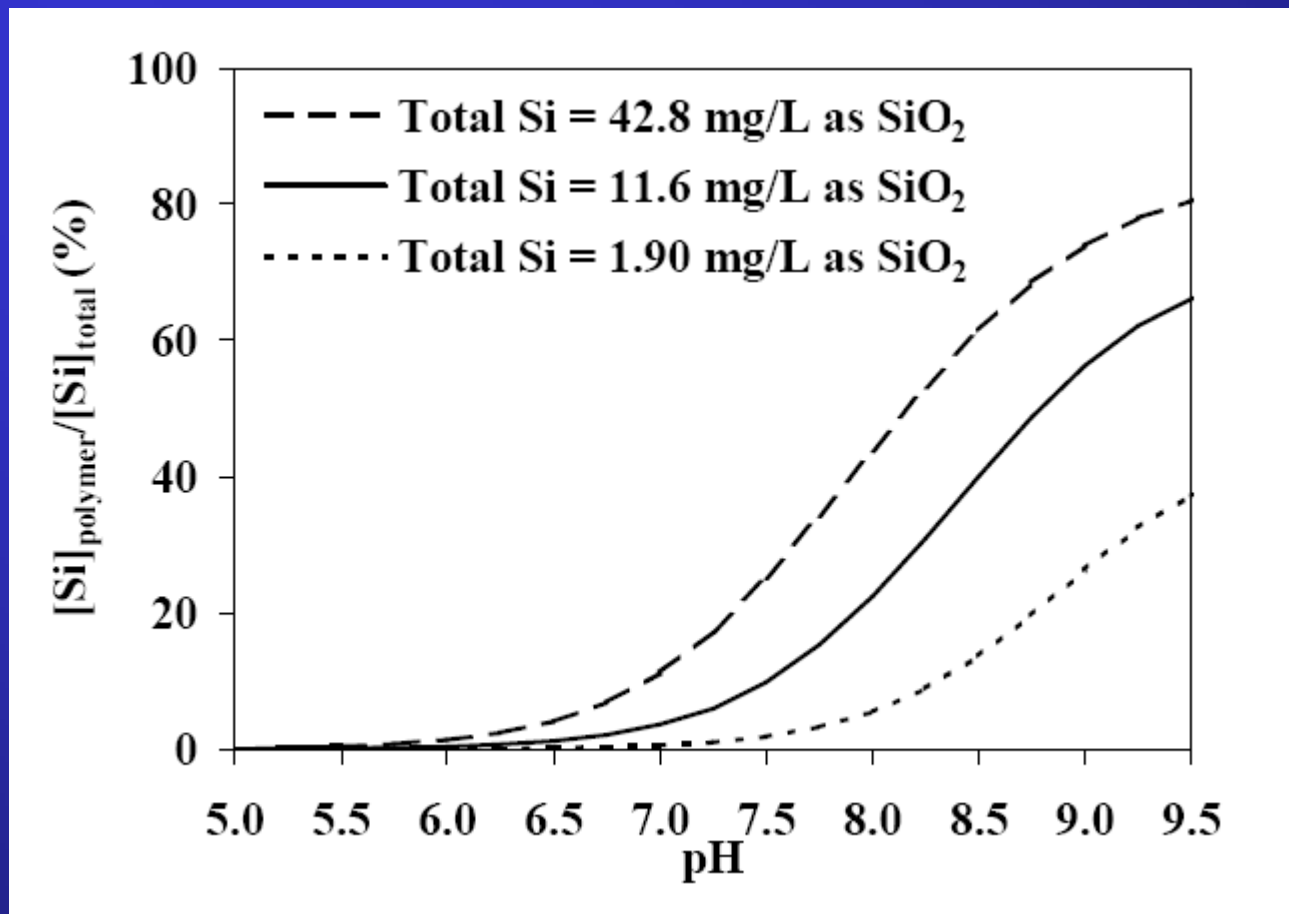
Silica in natural waters

- **Concentration:** 1 - 20 mg/L as SiO₂ in surface waters
0.8 - 63 mg/L as SiO₂ in ground waters
- **Speciation:**



Silica in natural waters

$(\text{HO})_3\text{SiOSi}(\text{OH})_2\text{O}^-$ 99% of the polymeric silicon



Implications for environmental systems

A high silica content in water would be a major problem for:

- **Coagulation-Filtration Technologies**
 - Interactions with Aluminum
 - Interactions with Iron
 - **Membrane Separation Technologies (RO)**
 - **Ion Exchange Technologies**
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Silica removal from natural waters

- ❖ **Ion exchange – SBA exchange resins**
 - Silica removal is suppressed by the competition of other present anions (SO_4^{2-})
- ❖ **Adsorption – Iron hydroxide media**
 - It was found that sorption increases as the silica concentration and pH increase with a maximum adsorption at \sim pH 9 (L. Sigg and W. Stumm, *Colloids Surf.*, **1981**, 2, 101-117)
- ❖ **Adsorption on hybrid sorbents**
 - The polymeric ion exchangers were used as host skeleton for nanoparticles of hydrous ferric oxide for oxyanions removal (L. Cumbal, A.K. SenGupta, *Environ. Sci. Technol.*, **2005**, 39, 6508-6515)
 - Potential media for silica removal.

The purpose of the present work

- To evaluate the performance of a new organic/inorganic hybrid ion exchanger, containing nanoparticles of hydrous ferric oxide inside the matrix of a macroporous strong base anion (SBA) resin, for silica removal from natural waters.

Experimental

- Sorption isotherms on the hybrid sorbent and the parent ion exchanger were measured at 1-5 mmol/L Si in NSF-53 solution and DM water at pHs of 6.5, 7.5 and 8.5 at 298°K using AAS.
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New Organic / Inorganic Hybrid Ion Exchanger "D-9908"

Strong Base Anion (SBA)



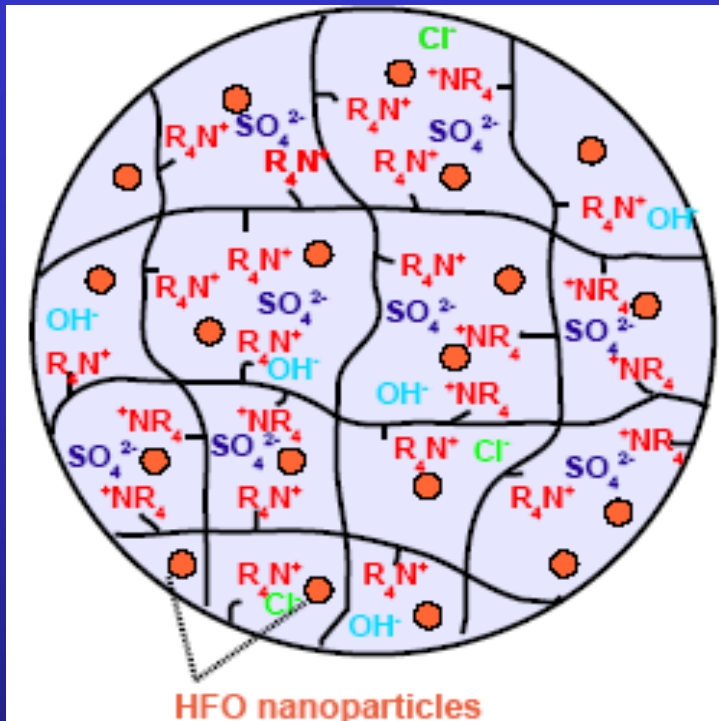
- Macroporous matrix
- Quaternary ammonium functional groups (R_4N^+)
- SO_4^{2-} form

D-9908



- Hydrous ferric oxide irreversible encapsulated throughout the SBA beads
- 250 mg Fe / g dry resin

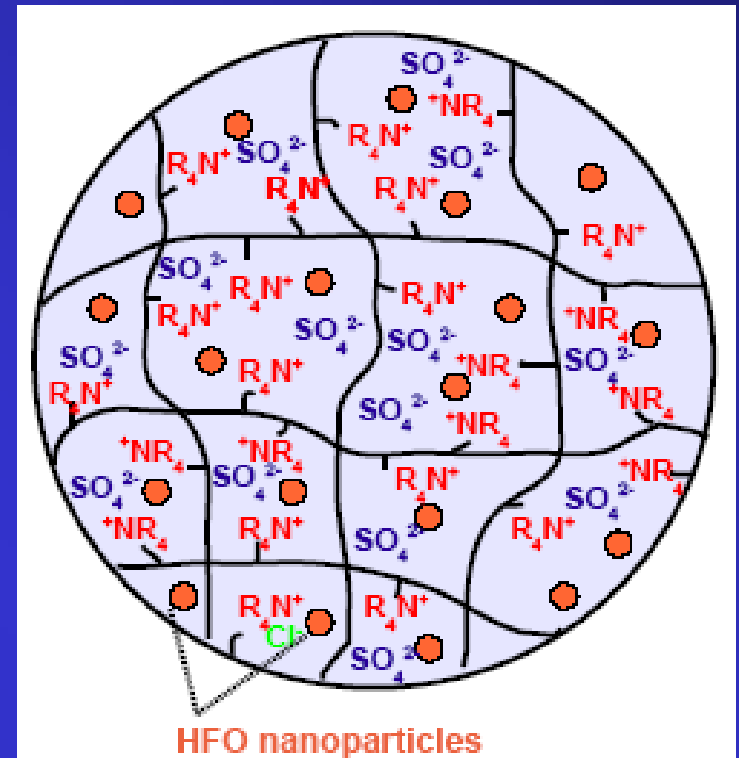
New Organic / Inorganic Hybrid Ion Exchanger "D-9908"



D-9908 "virgin"

75 % SO_4^{2-}
 17 % OH^-
 7 % Cl^-

excess of Na_2SO_4
 1 M solution



D-9908 (SO_4^{2-})

97.2 % SO_4^{2-}
 2.8 % Cl^-

NSF-53 standard test water composition

CATIONS	meq/L	ANIONS	meq/L
Ca^{2+}	2.00	HCO_3^-	2.97
Mg^{2+}	1.04	SO_4^{2-}	1.04
Na^+	3.169	NO_3^-	0.14
		PO_4^{3-}	0.004
		Cl^-	2.00
		F^-	0.052
Total cations:	6.209	Total anions:	6.206

NSF/ANSI-53 Standard for Drinking Water Treatment Units – Health effects, 2003, 43, 51-54.

Measured isotherms at 298° K

Resin	C_{Si}^0 (mmol/L)	Solution matrix	pH _{initial}
D-9908	1	NSF-53	6.5; 7.5; 8.5; 9.5
D-9908	3	NSF-53	7.5
D-9908	5	NSF-53	6.5; 7.5; 8.5
D-9908	1	DMW	6.5; 7.5; 8.5
D-9908 (SO ₄ ²⁻)	1	DMW	6.5; 7.5; 8.5
SBA (SO ₄ ²⁻)	1	NSF-53	6.5; 7.5; 8.5
SBA (SO ₄ ²⁻)	5	NSF-53	6.5; 7.5; 8.5
SBA (SO ₄ ²⁻)	1	DMW	6.5; 7.5; 8.5

Multicomponent ion exchange system

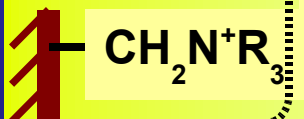
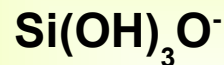
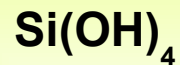
Initial stage

Resin phase

Solution phase



$\text{pH}_{\text{initial}} = 6.5 / 7.5 / 8.5 / 9.5$



SO_4^{2-} : 75%



HO^- : 17%



Cl^- : 7%

NSF-53

CO_3^{2-} : 1%

HCO_3^- : 3 meq/L

Cl^- : 2 meq/L

SO_4^{2-} : 1 meq/L

NO_3^- : 0.14 meq/L

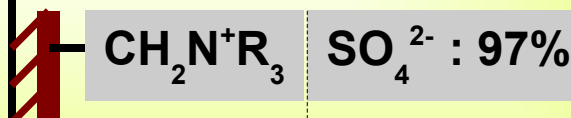
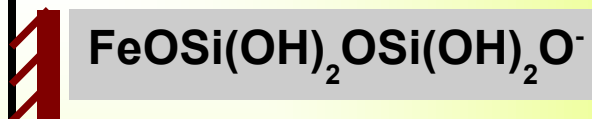
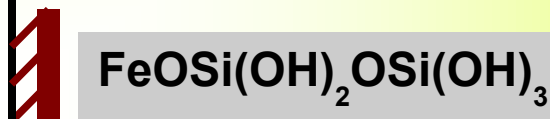
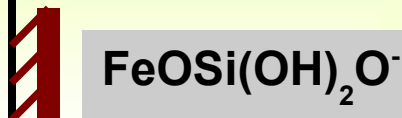
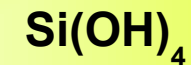
F^- : 0.052 meq/L

PO_4^{3-} : 0.04 meq/L

At equilibrium

Resin phase

Solution phase



NSF-53

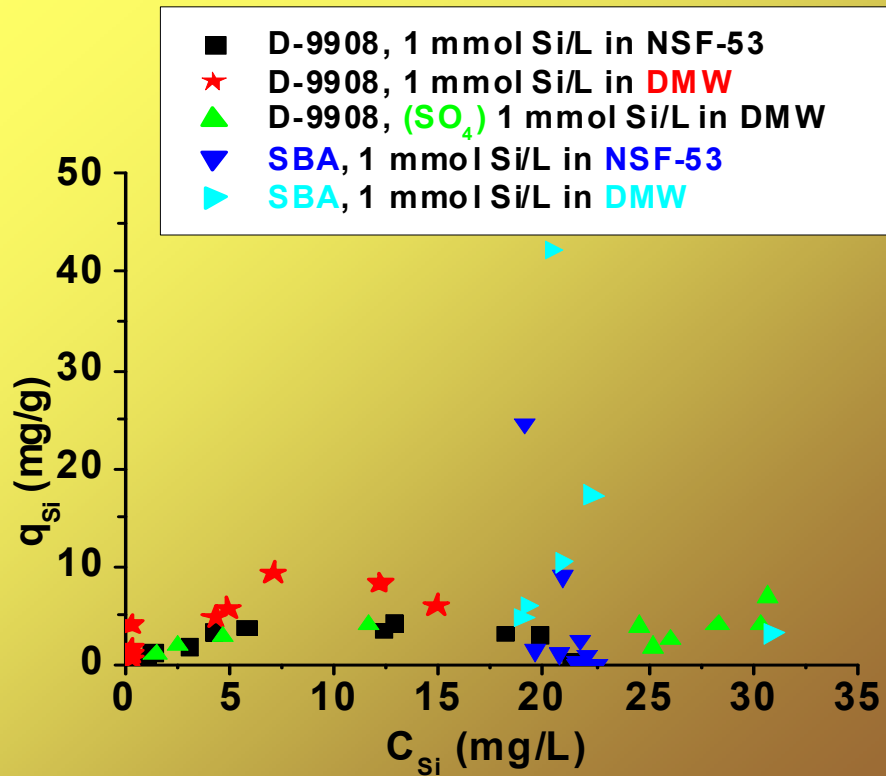
HCO_3^- ; Cl^- ; NO_3^-

F^- ; OH^- ; CO_3^{2-}

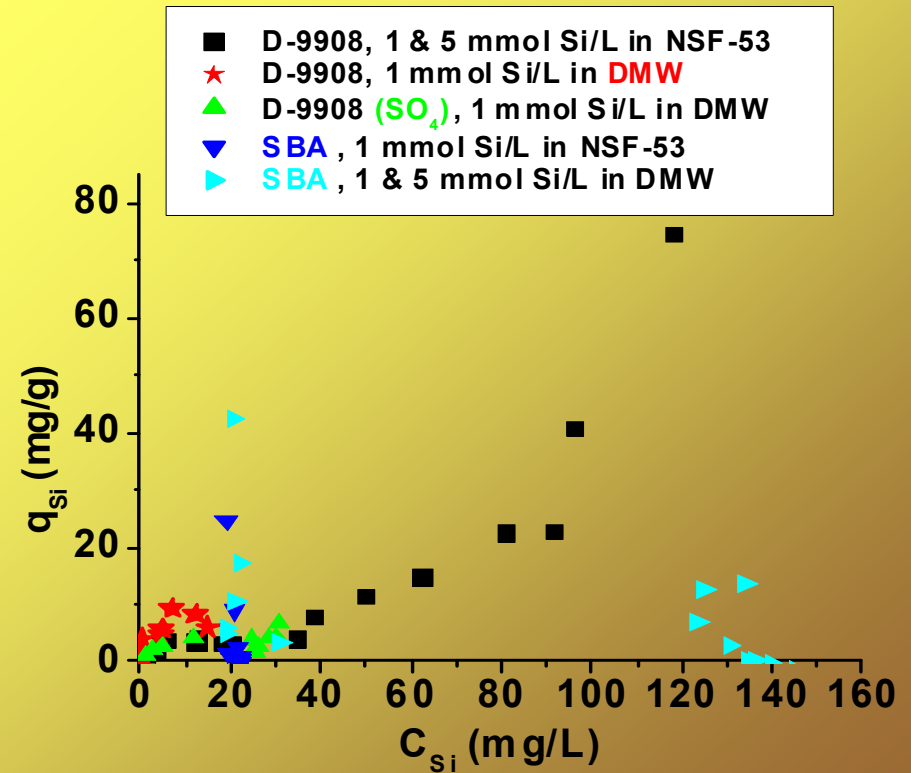
SO_4^{2-} ; PO_4^{3-}

Sorption isotherms of silica on D-9908 and SBA from NSF-53 and DMW solutions at $pH_{in} = 6.5$

a) 1 mmol / L

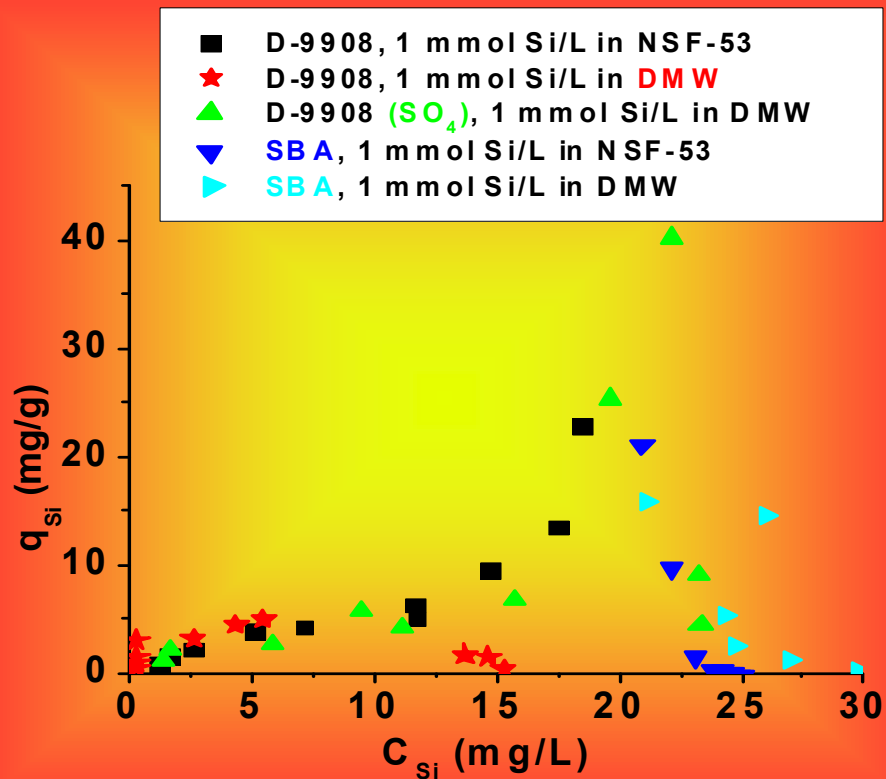


b) 1 & 5 mmol / L

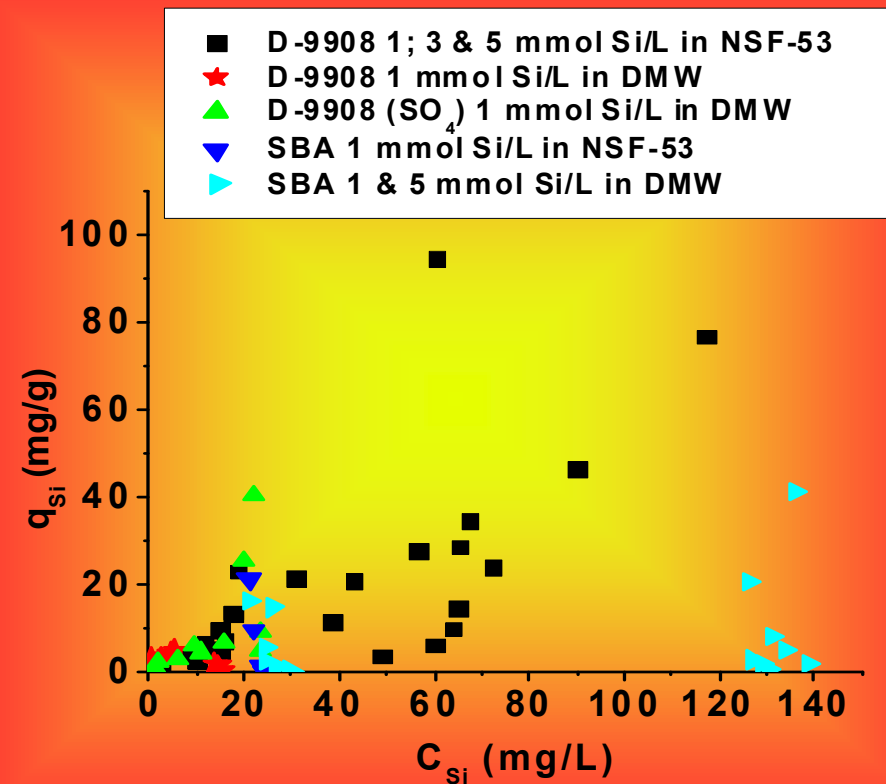


Sorption isotherms of silica on D-9908 and SBA from NSF-53 and DMW solutions at $pH_{in} = 7.5$

a) 1 mmol / L

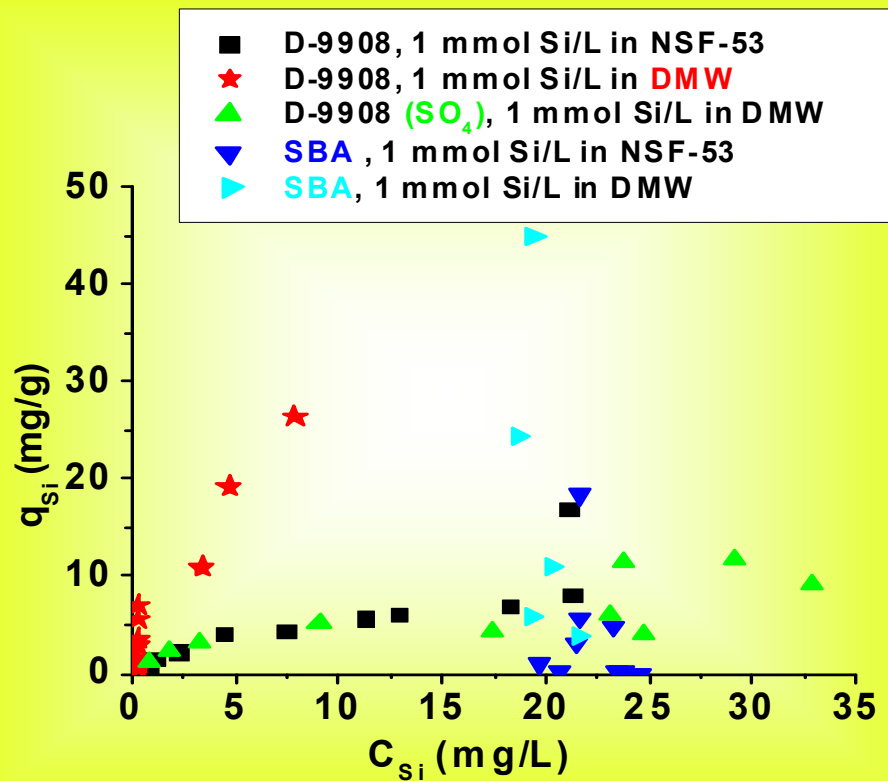


b) 1 & 5 mmol / L

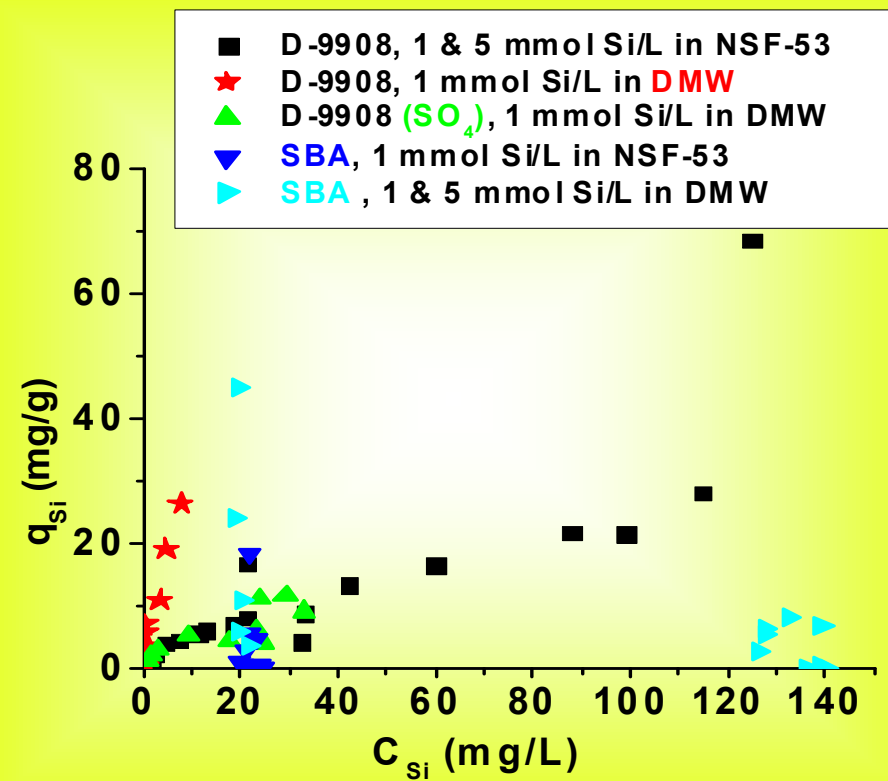


Sorption isotherms of silica on D-9908 and SBA from NSF-53 and DMW solutions at $pH_{in} = 8.5$

a) 1 mmol / L

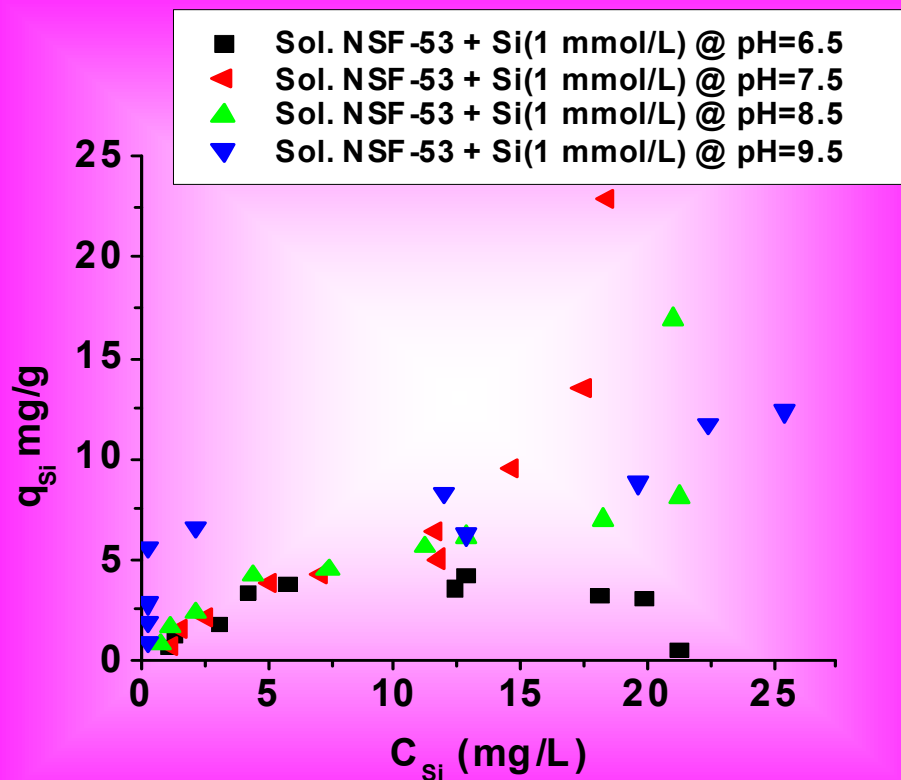


b) 1 & 5 mmol / L

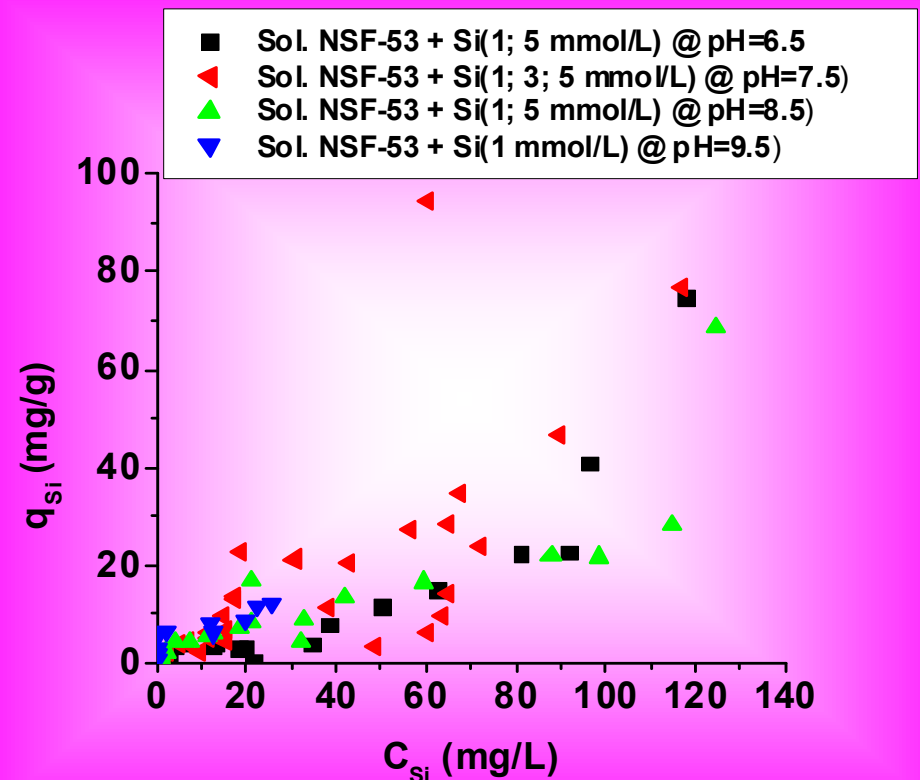


Silica sorption isotherms on the hybrid ion exchanger D-9908 at different pHs

a) 1 mmol/L Si



b) 1 & 3 & 5 mmol/L Si



The series of variation of the loading with silicon of D-9908 at equilibrium at different pHs

$C_{Si} / \text{mg/L}$	loading variation with pH
$0 < C_{Si} < 12$	$9.5 \gg 6.5 \approx 7.5 \approx 8.5$
$12 < C_{Si} < 25$	$7.5 > 9.5 > 8.5 > 6.5$
$25 < C_{Si} < 70$	$7.5 > 8.5 \approx 6.5$
$70 < C_{Si} < 120$	$7.5 > 6.5 > 8.5$

Concluding Remarks

- **The performance of a new organic-inorganic hybrid ion exchanger for silica removal from natural waters was evaluated measuring the sorption isotherms at 298 K. The sorbent contains nanoparticles of hydrous ferric oxide encapsulated in a macroporous matrix of a strongly basic anion exchanger. NSF-53 standard test water was used to simulate the composition of the natural water. The total silica concentration was 1, 3 and 5 mmol/L. The initial pH was 6.5, 7.5, 8.5, and 9.5**
 - **The isotherms depict solid-liquid multicomponent systems at equilibrium**
 - **The results show that the new material is a good sorbent for removing silica from natural waters at all investigated pHs and has better properties than the host anion exchanger**
 - **The experiments support the retention of silica on the hydrous ferric oxide nanoparticles of the hybrid material at all investigated pHs**
 - **The presence of other anions in the natural water suppressed the silica removal on the hybrid material; at pH 7.5 the effect is negligible**
 - **The up-take on the hybrid sorbent depends strongly on the initial pH and silica concentration in the natural water, due to silica speciation**
 - **The sorption of silica on the new hybrid ion exchanger seems to be the maximum at pH 7.5.**
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Thank you for your attention!!!

