

# Monitoring Flow Streams in Multi-step Transformations

**Reaction optimisation conference**

**Flow Chemistry Lecture**

**24<sup>th</sup> of April 2013**

**Department of Chemistry,  
University of Durham  
University South Road, Durham.  
DH1 3LE, UK  
e-mail: [i.r.baxendale@durham.ac.uk](mailto:i.r.baxendale@durham.ac.uk)**



**Ian R. Baxendale**

***'For 60% of today's chemical reactions  
the easiest approach is a batch based synthesis.'***

French chemist Antoine Lavoisier (the "father of modern chemistry") started the chemical revolution in **1773**.

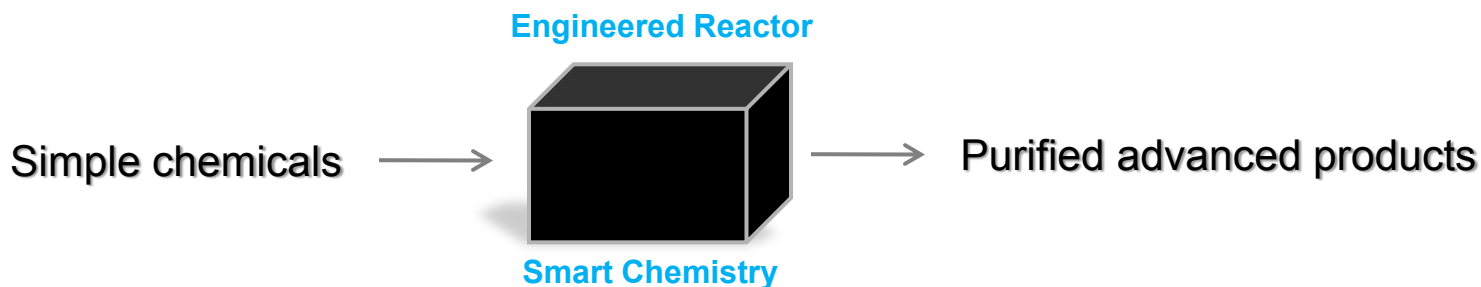
We have now had over **240** years to perfect batch based approaches.

### ***So why adopt flow chemistry as an additional tool?***

***To overcome some of the current limitations in working practice.***

***A few examples:***

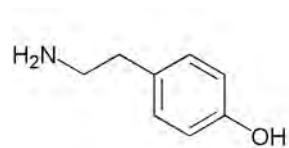
- **Solvent boiling point as upper temperature limit (avoid DMSO/DMF)**
  - the problem of 'reflux restriction' (Microwave chemistry/scale-up)
- **Use of large dilution, e.g. to control heat releases or to simply create a working volume.**
- **The direct scale up of a reaction is not always a linear progression or multiplication of substrates/solvents and parameters.**
- **Achieve controlled reactivity rather than relying upon aggressive or labile reagents**
  - quick and dirty chemistry reliant on chromatography.
- **In-line monitoring means problems can be rectified early - not all your eggs are in one basket.**



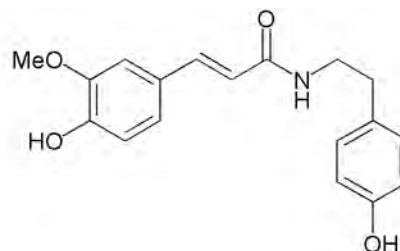
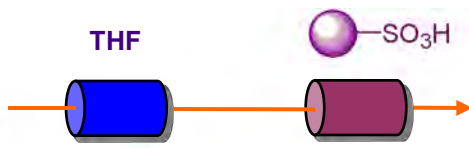
**100% efficient, 100% yielding and 100% reproducible!**

We still have a 'little' bit of work to do.

# Synthesis of Grossamide

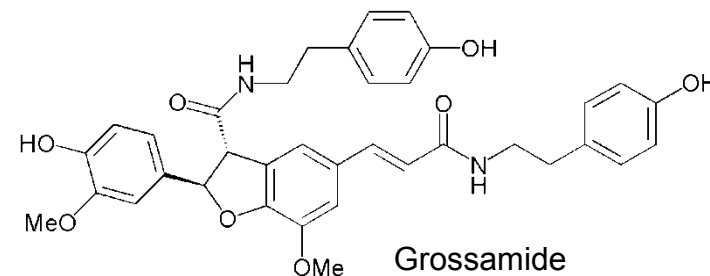
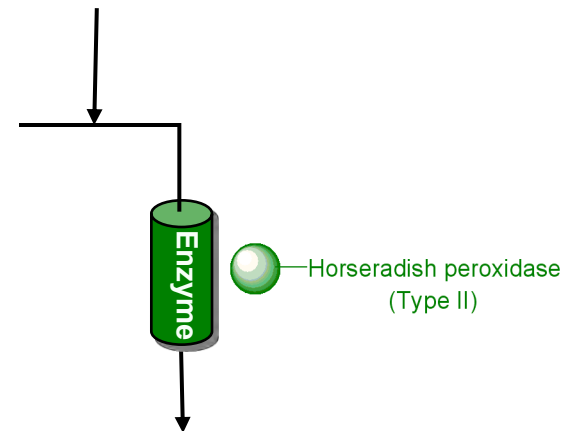


THF



Second input stream

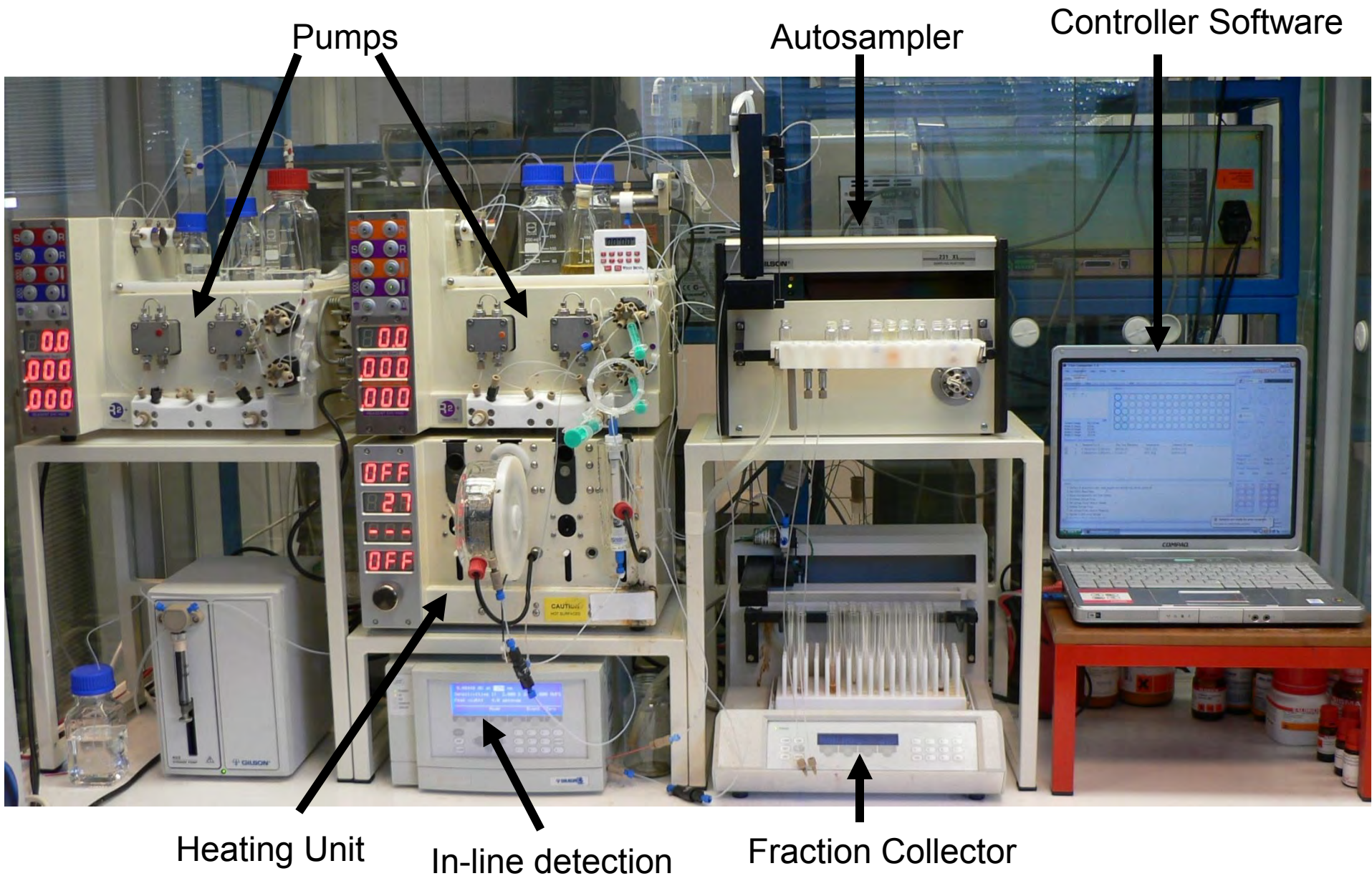
$H_2O_2$ -urea complex  
Acetone /  $H_2O$  (10:1)



Heater/Cooler module a reactor chip -40-150 °C  
Two HPLC pumps 100-10,000  $\mu$ L/min 35 bar system pressure  
2 reagent loading channels from liquid handling unit  
UV/diode array detection  
Split stream real-time MS analysis for optimisation  
In-line reverse phase preparative purification – Mass directed  
Fully software controlled via UNIPOINT + DoE software



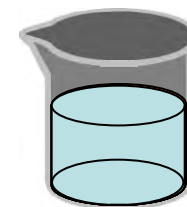
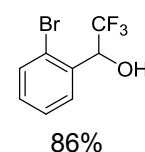
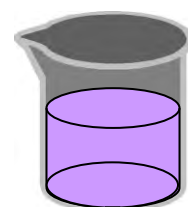
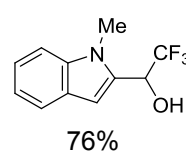
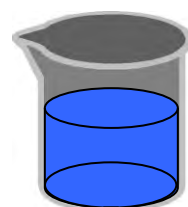
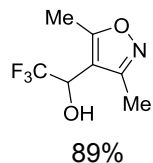
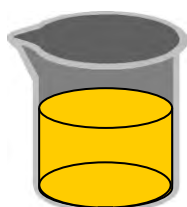
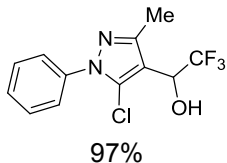
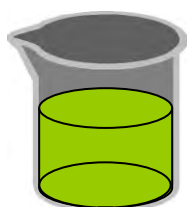
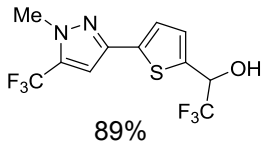
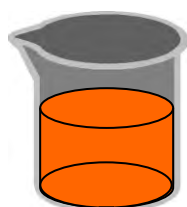
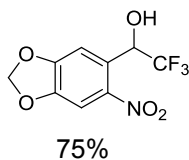
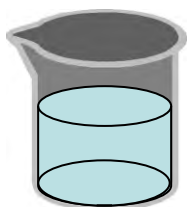
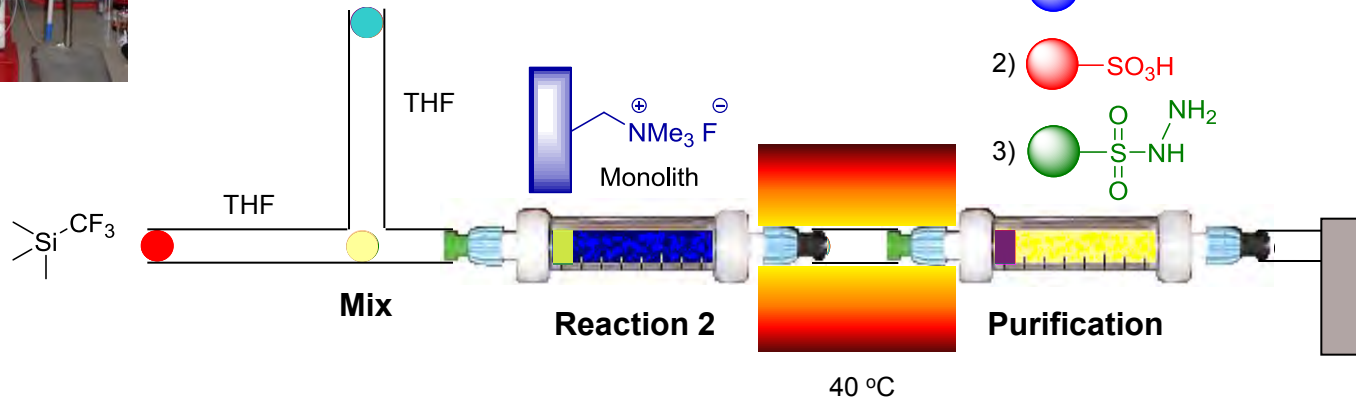
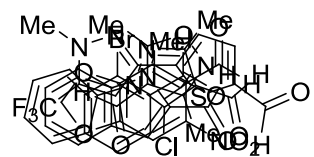
# Integrated Flow Chemistry Platform



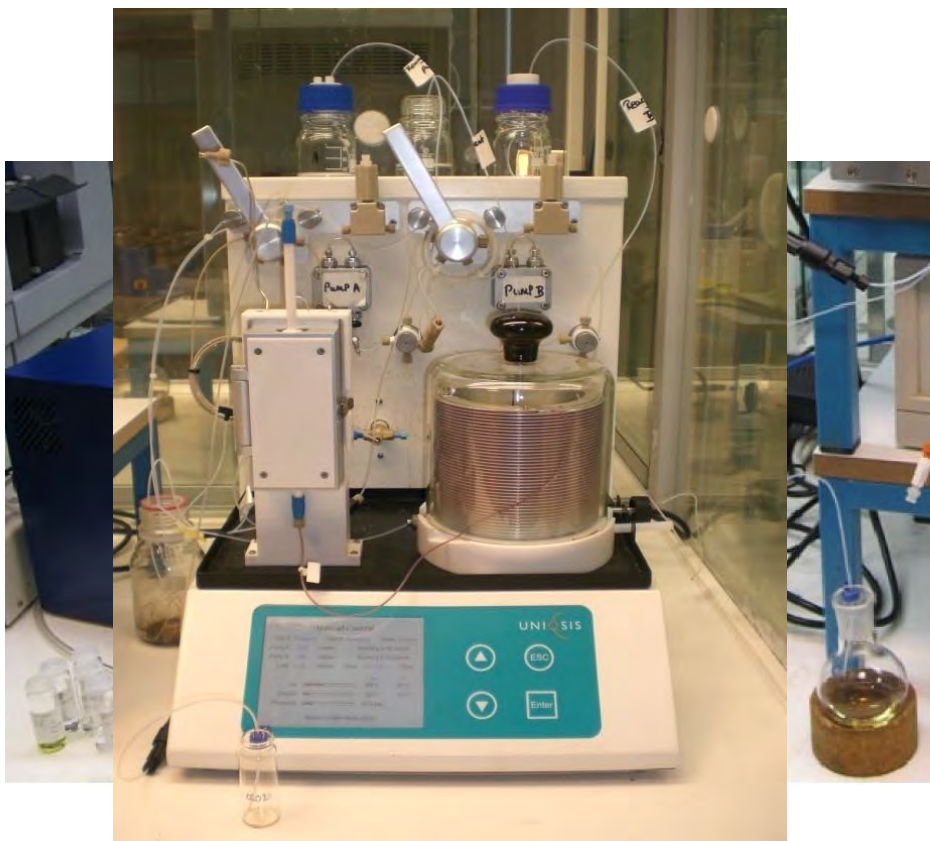
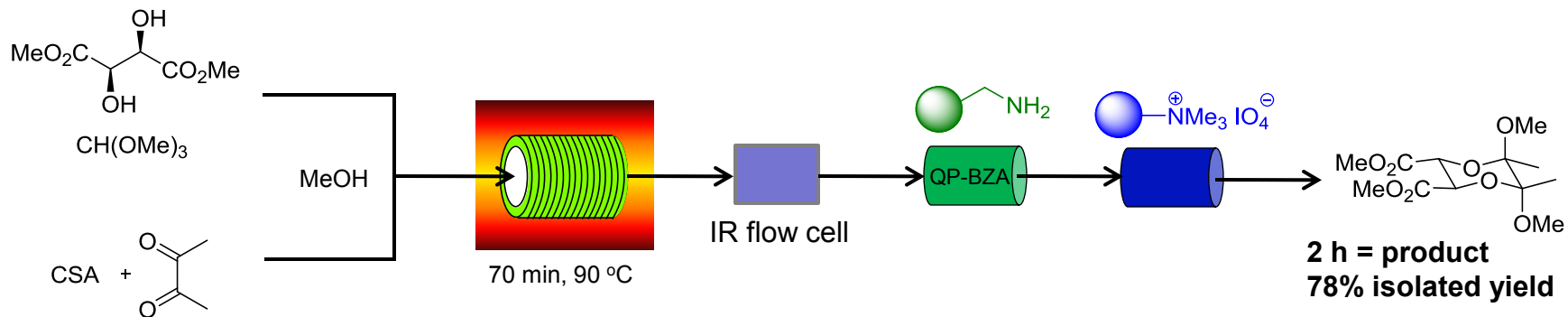
# Automated Sequential Reactions



## Trifluoromethylation with Ruppert's Reagent

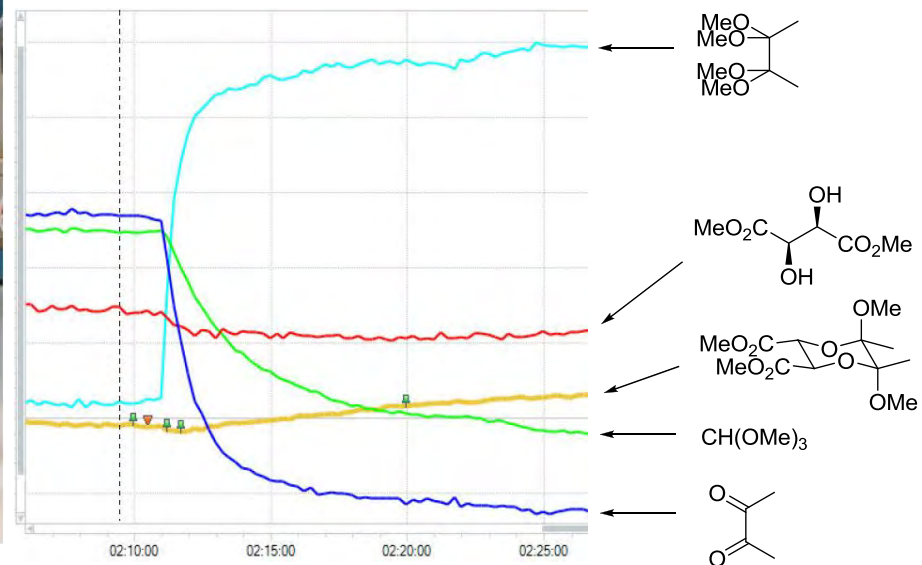


# BDA tartrates – monitoring concentrations

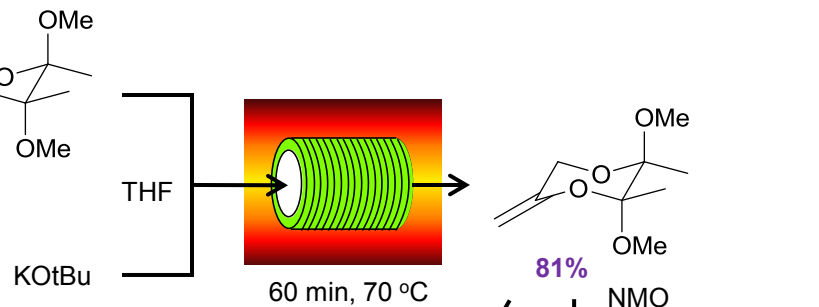
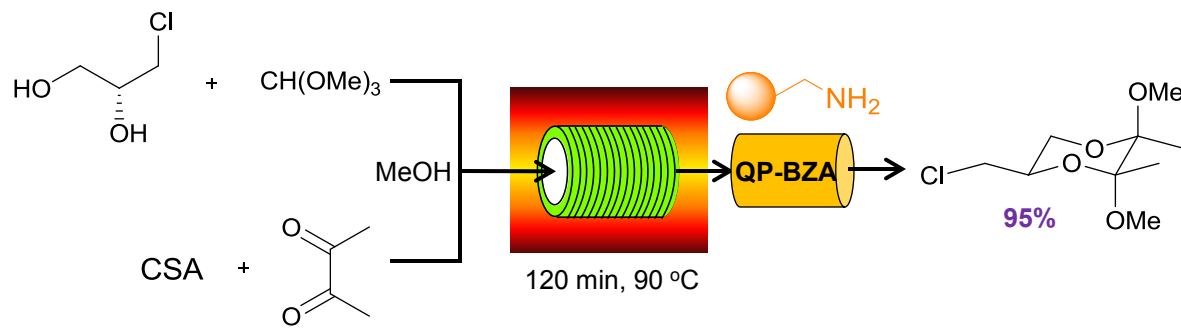
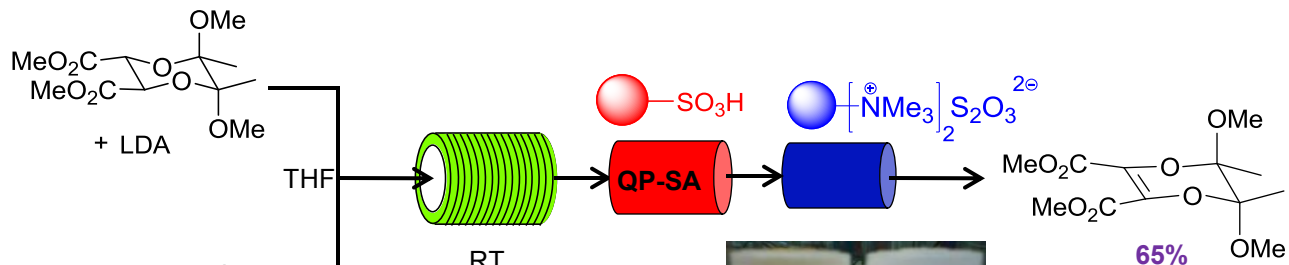


UniQsis FlowSyn

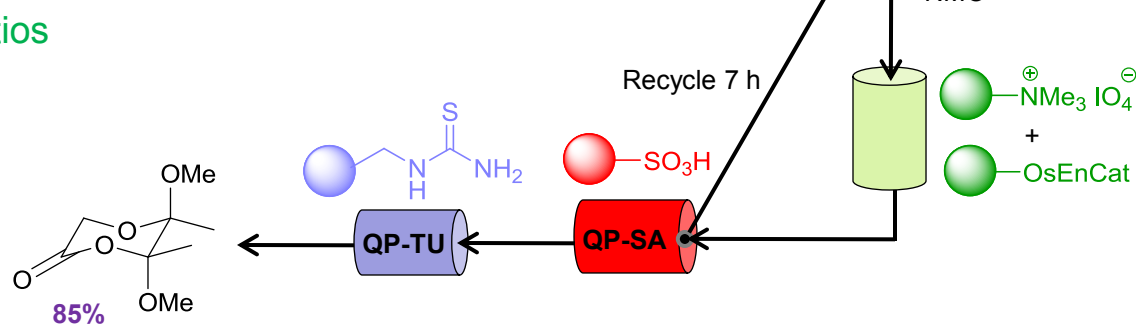
**Batch: 14 h reflux, bicarbonate work-up,  
 Et<sub>2</sub>O extraction - aqueous washing,  
 vac down, 2 x recryst. 50-70%**



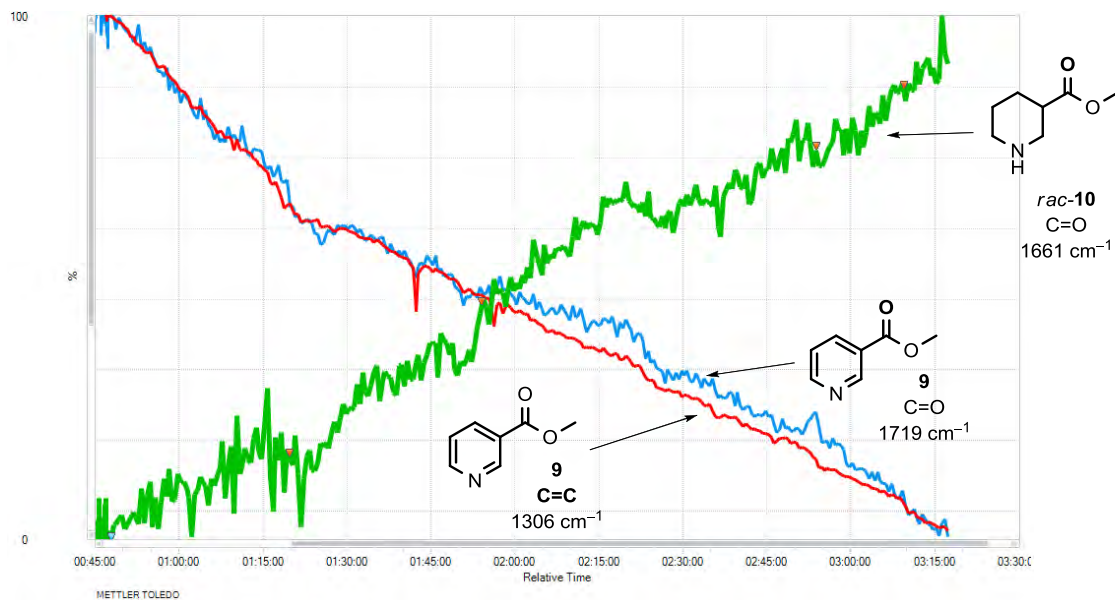
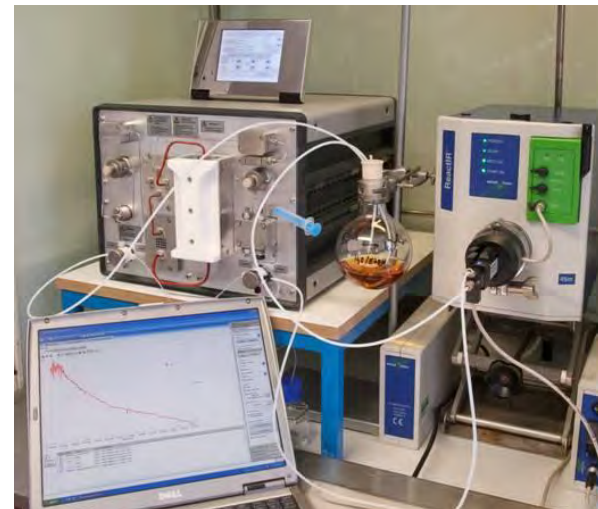
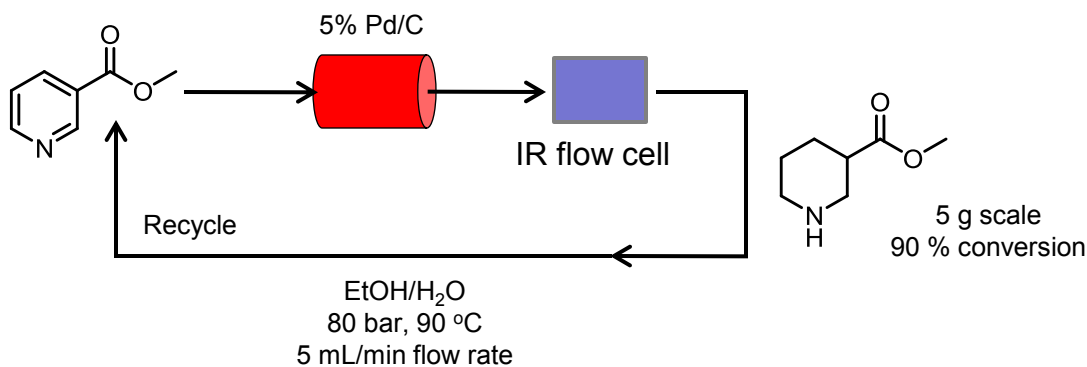
# BDA Modified Building Blocks



ratios



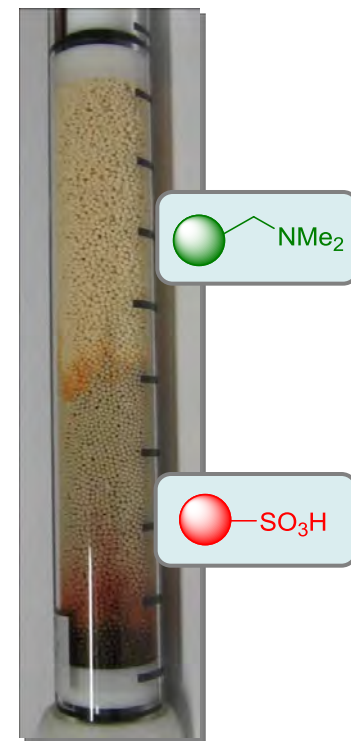
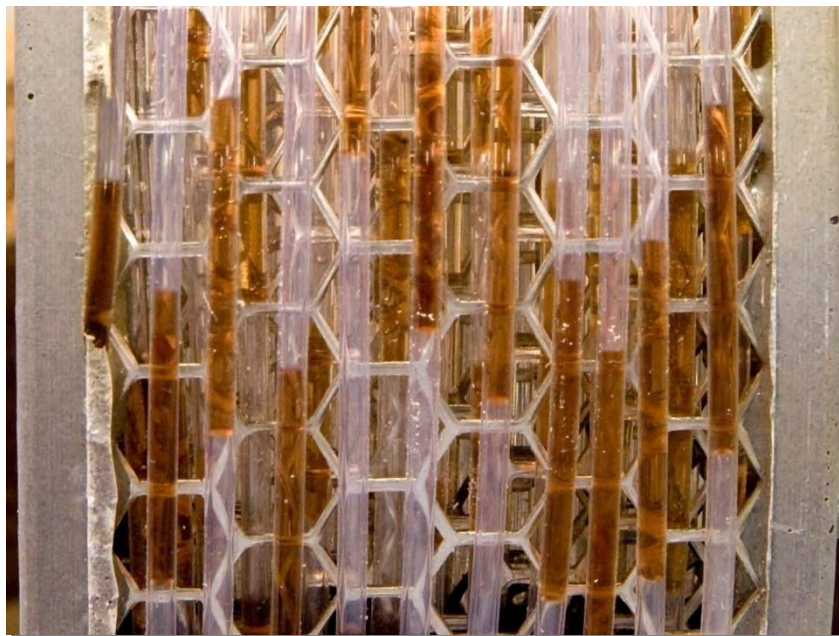
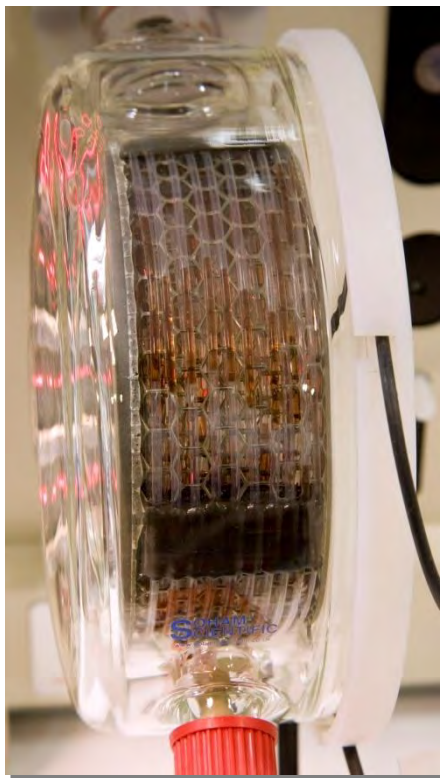
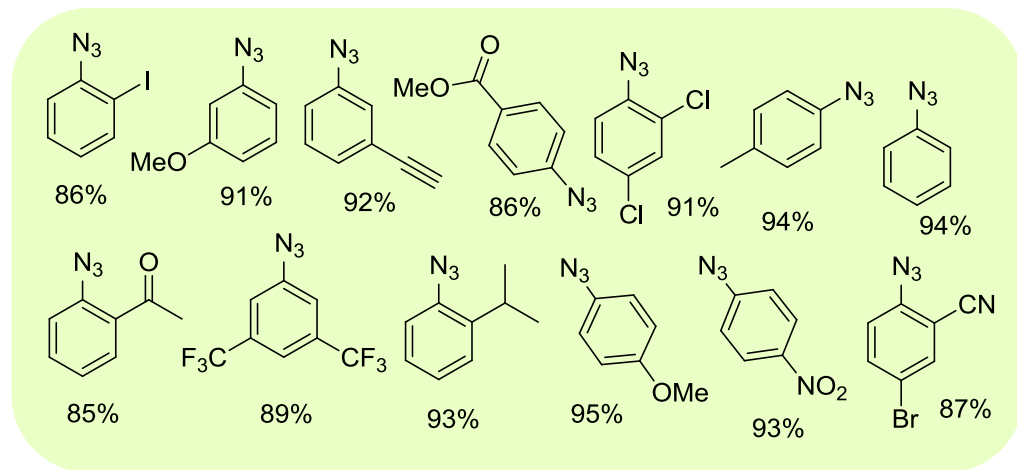
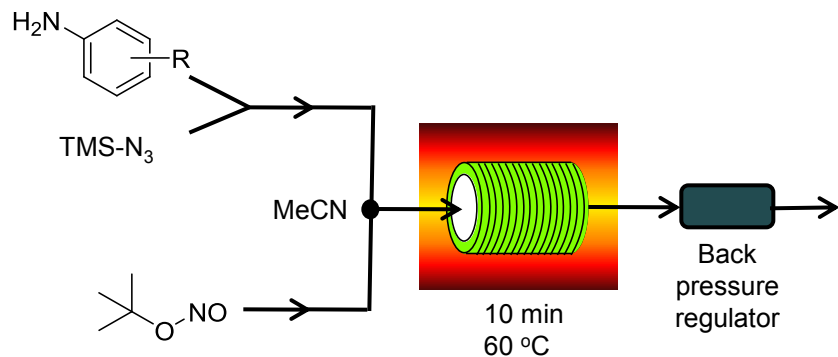
# MT React IR™ 45m flow cell



- Body: ReactIR™ 45m, fitted with a Mercury Cadmium Telluride (MCT) detector. Flow cell: Attenuated Total Reflectance (ATR) diamond sensor
- Full infrared spectral region from 650 to 1950 cm<sup>-1</sup> and from 2250 to 4000 cm<sup>-1</sup>
- Head can be heated and can stand pressures up to 30 bar
- HPLC connections to flow chemistry equipment
- iC IR 4.0 software for system operation and data analysis

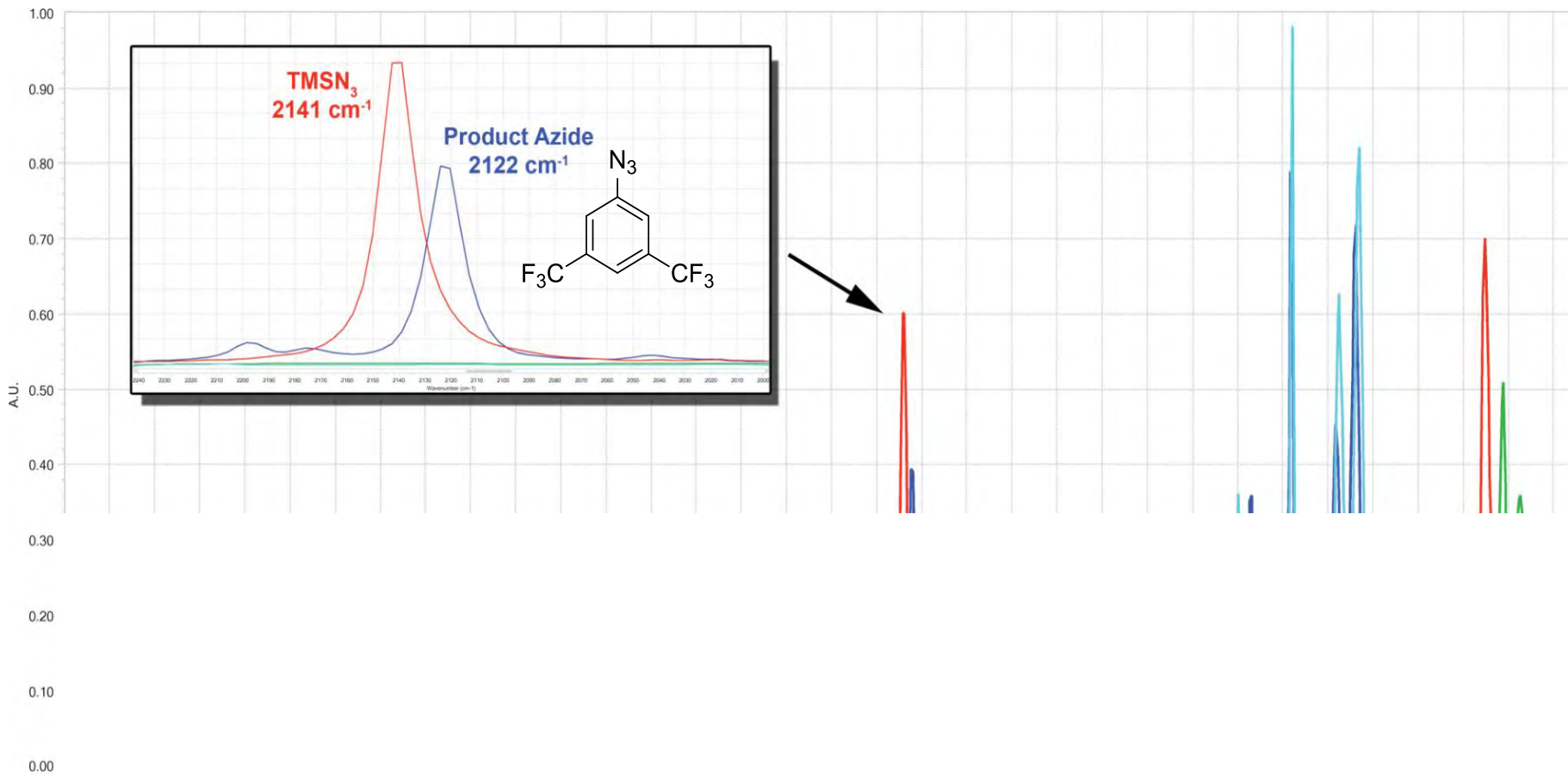


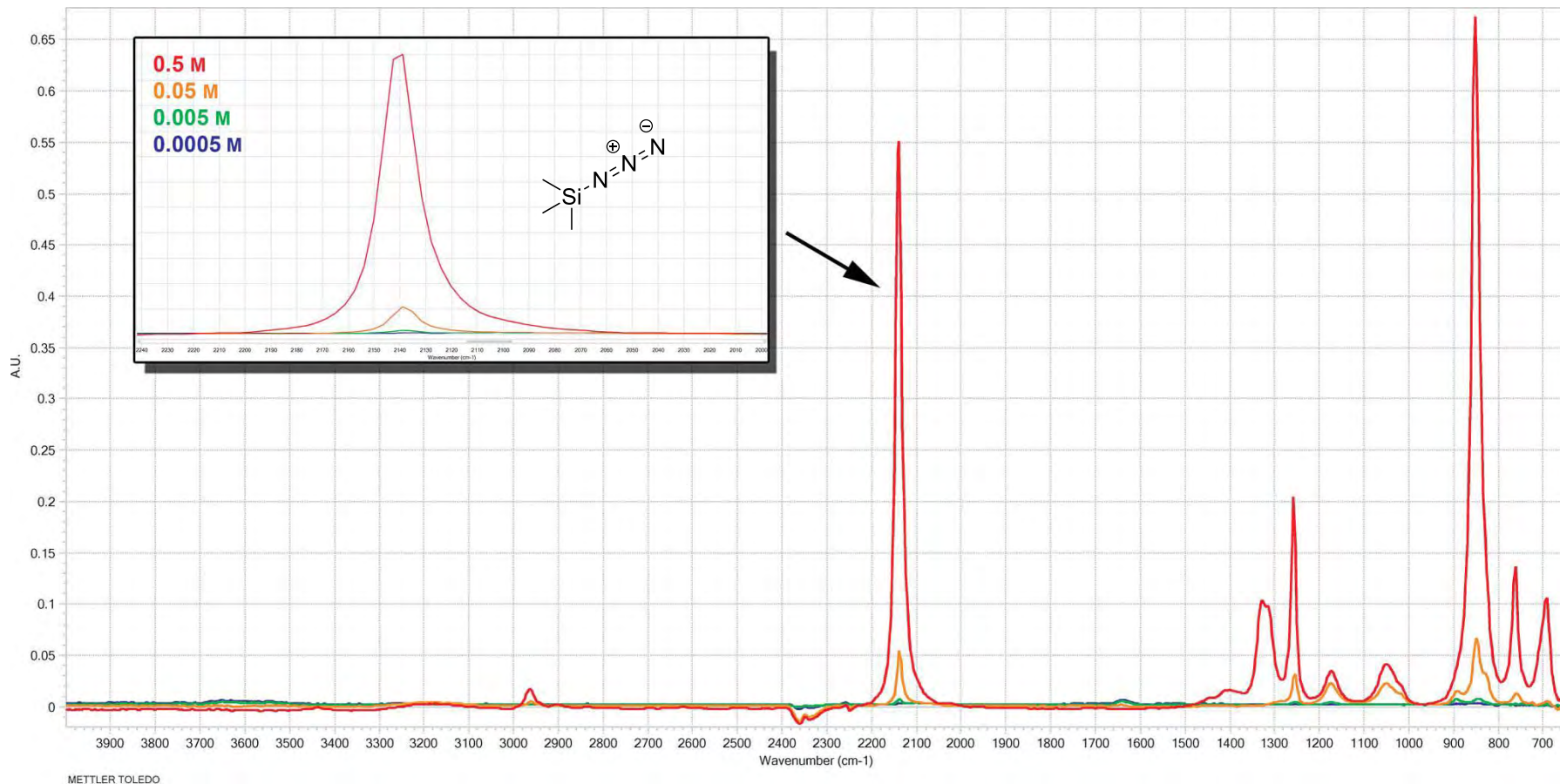
# Azides: Preparation in Flow



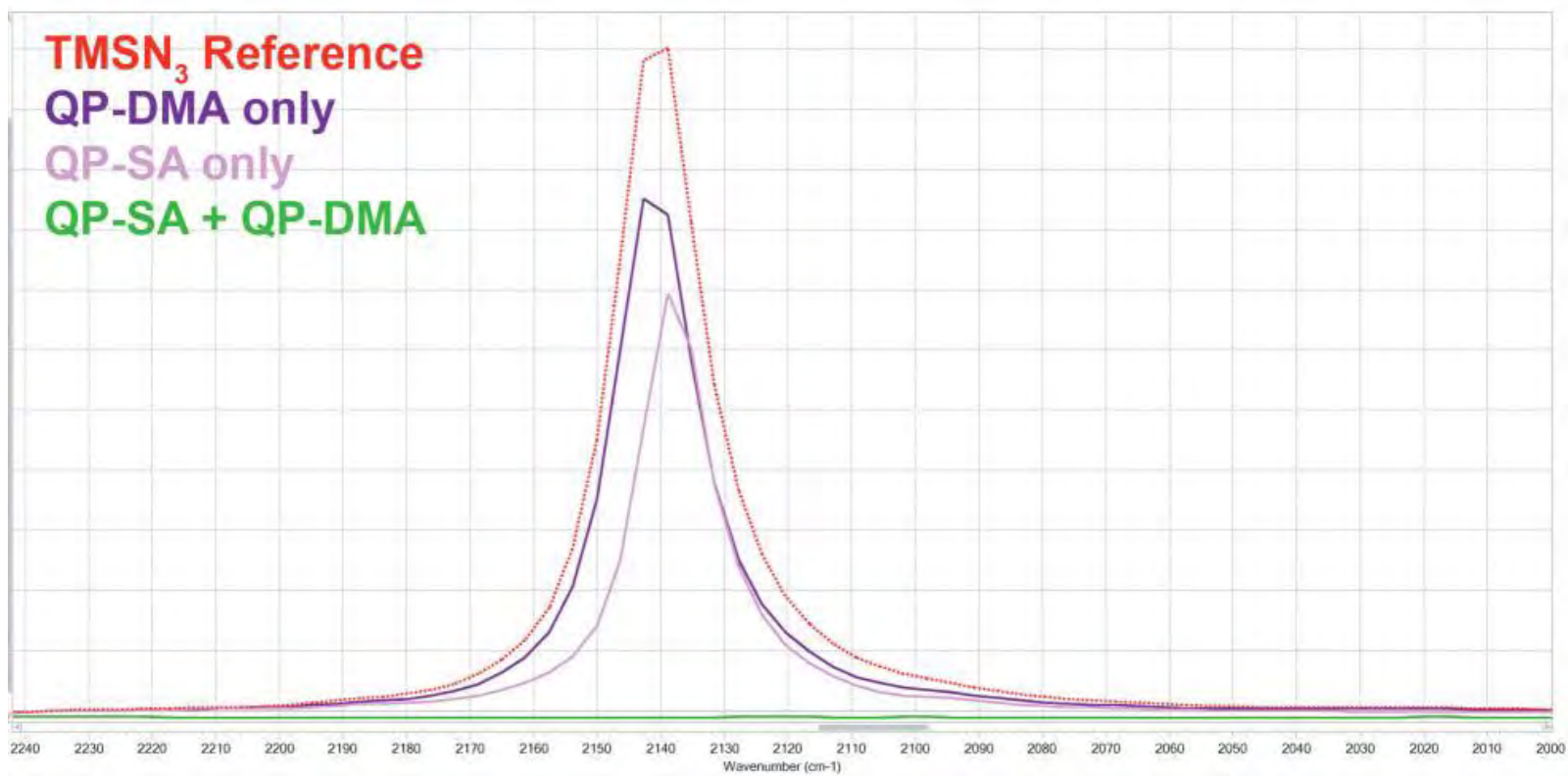
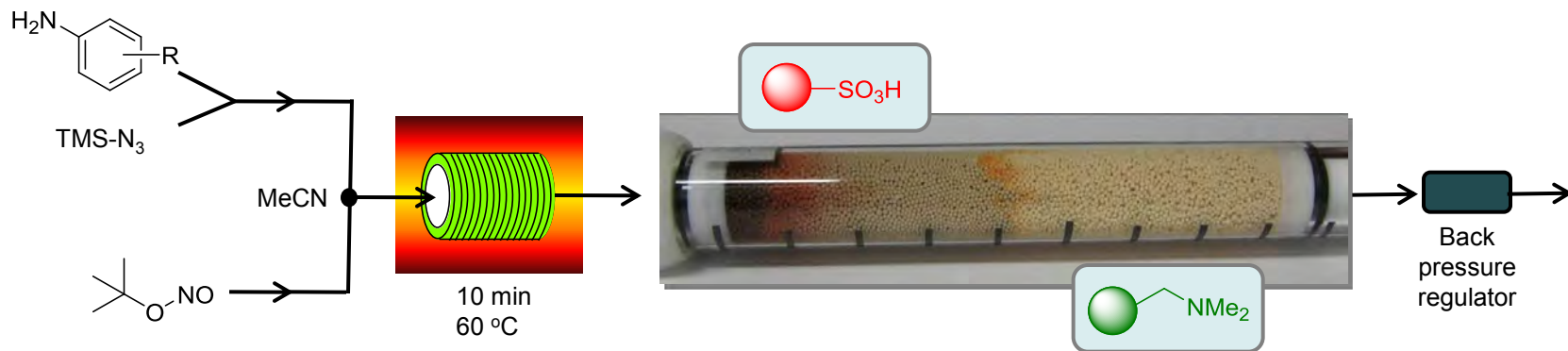
# In-line monitoring for Azides

Mettler-Toledo ReactIR flow cell

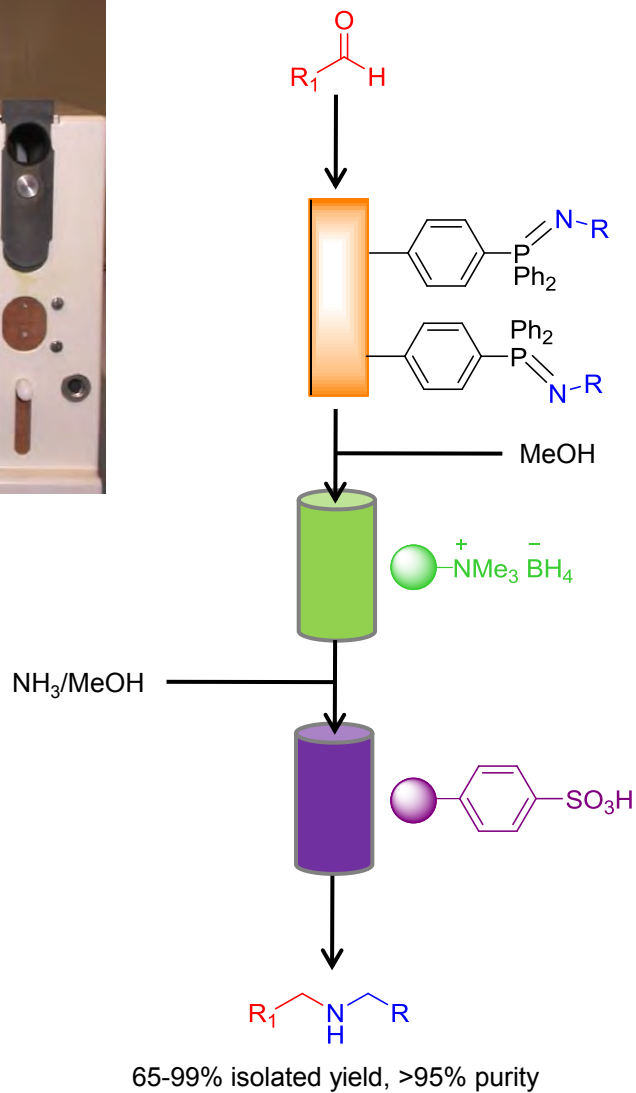
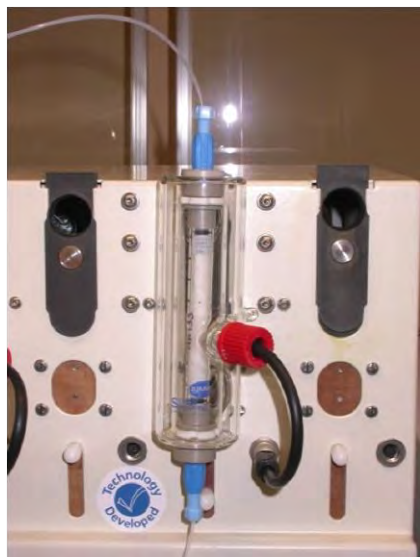




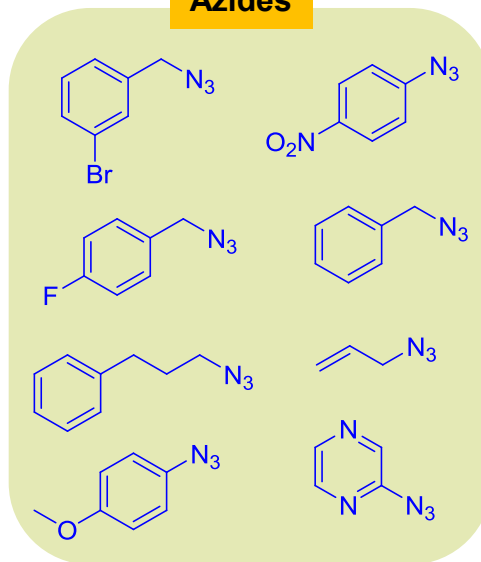
**Ferric chloride colourimetric test**



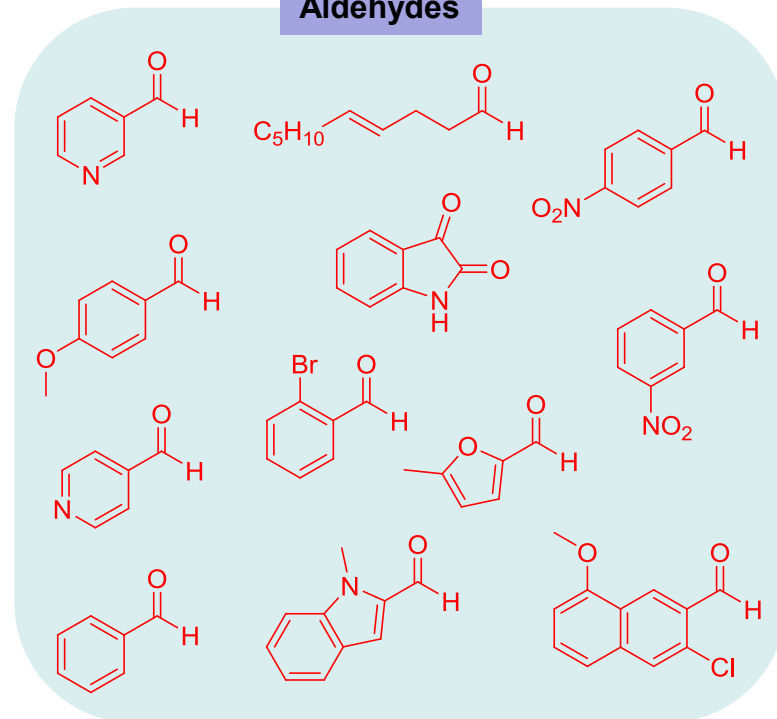
# Stauginger Aza Wittig Reaction



## Azides



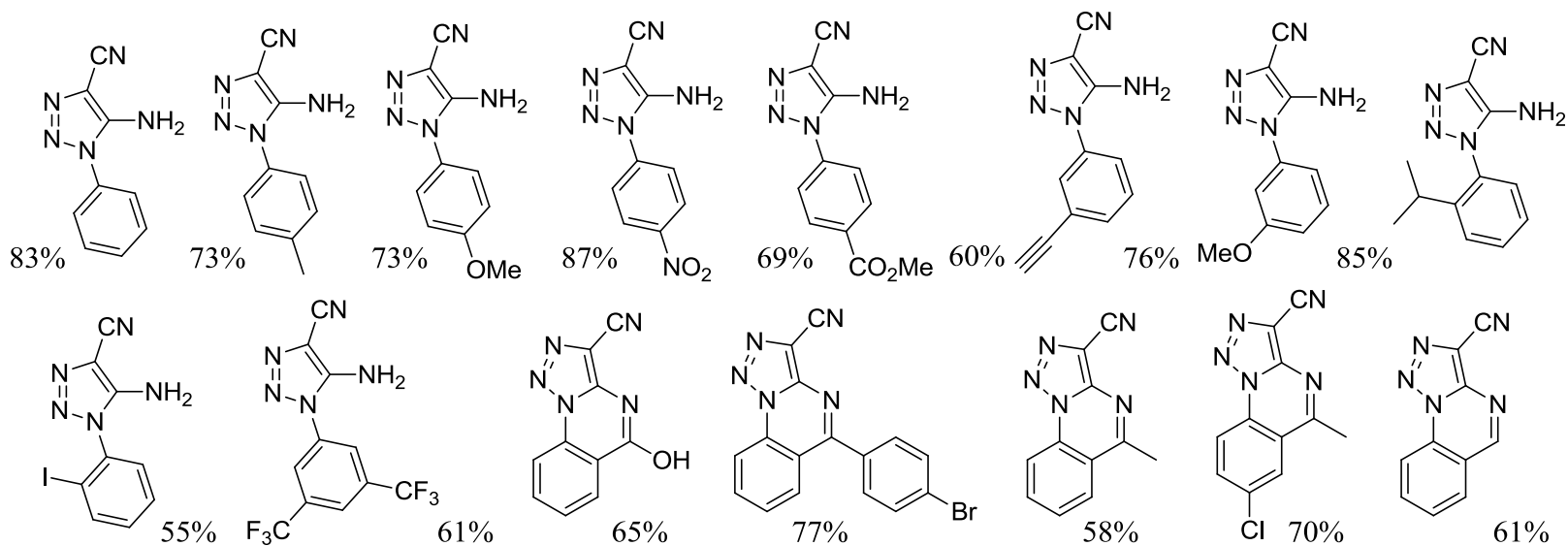
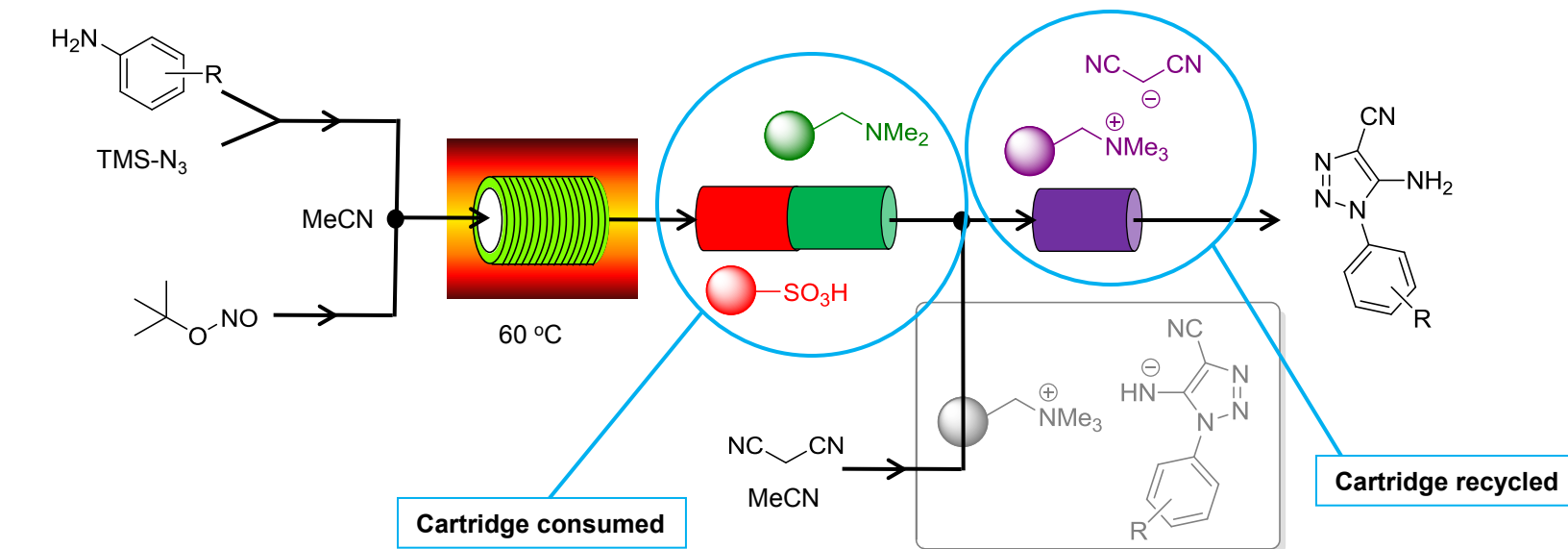
## Aldehydes



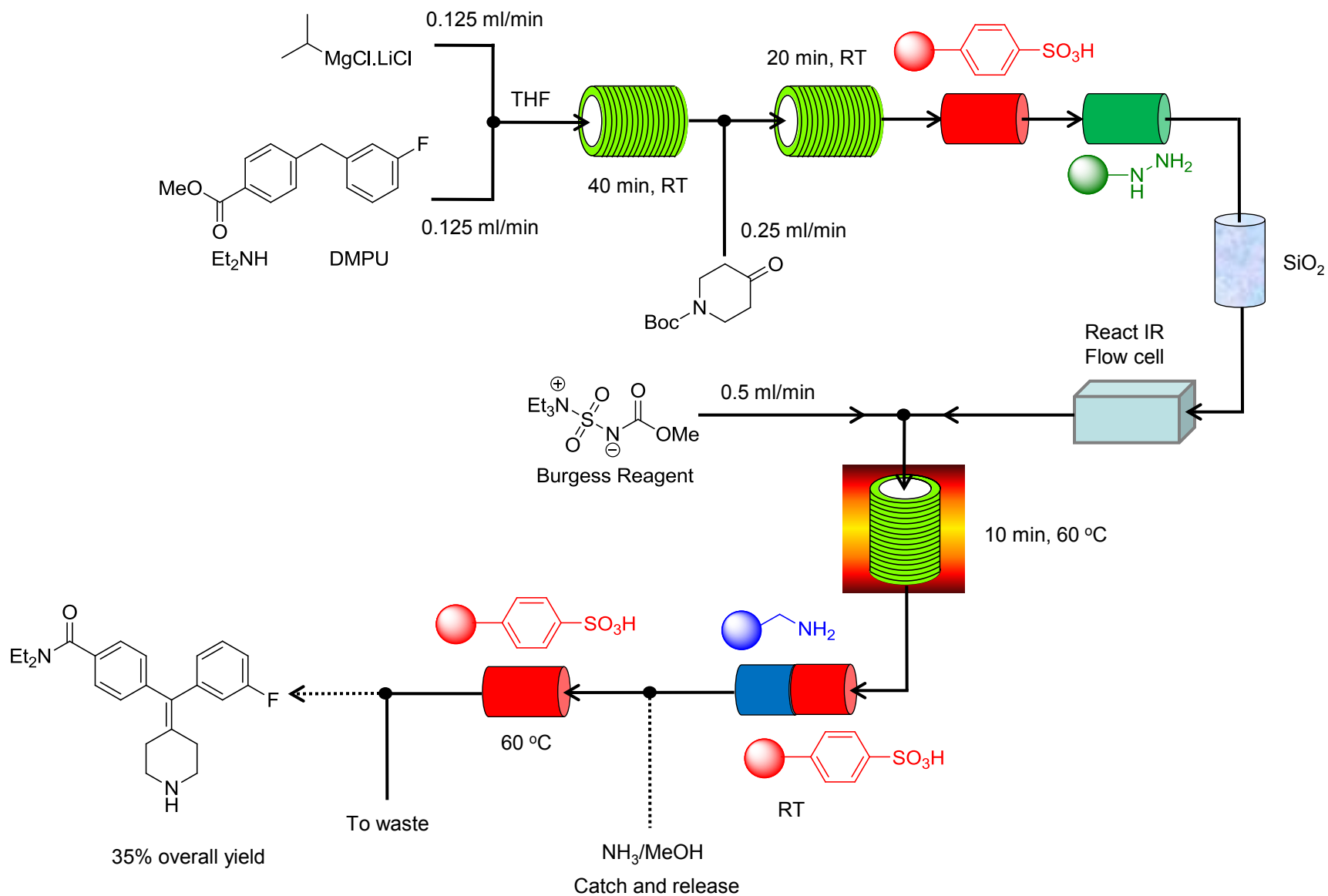
# Triazole Synthesis in Flow: Automation



# Triazole Synthesis in Flow

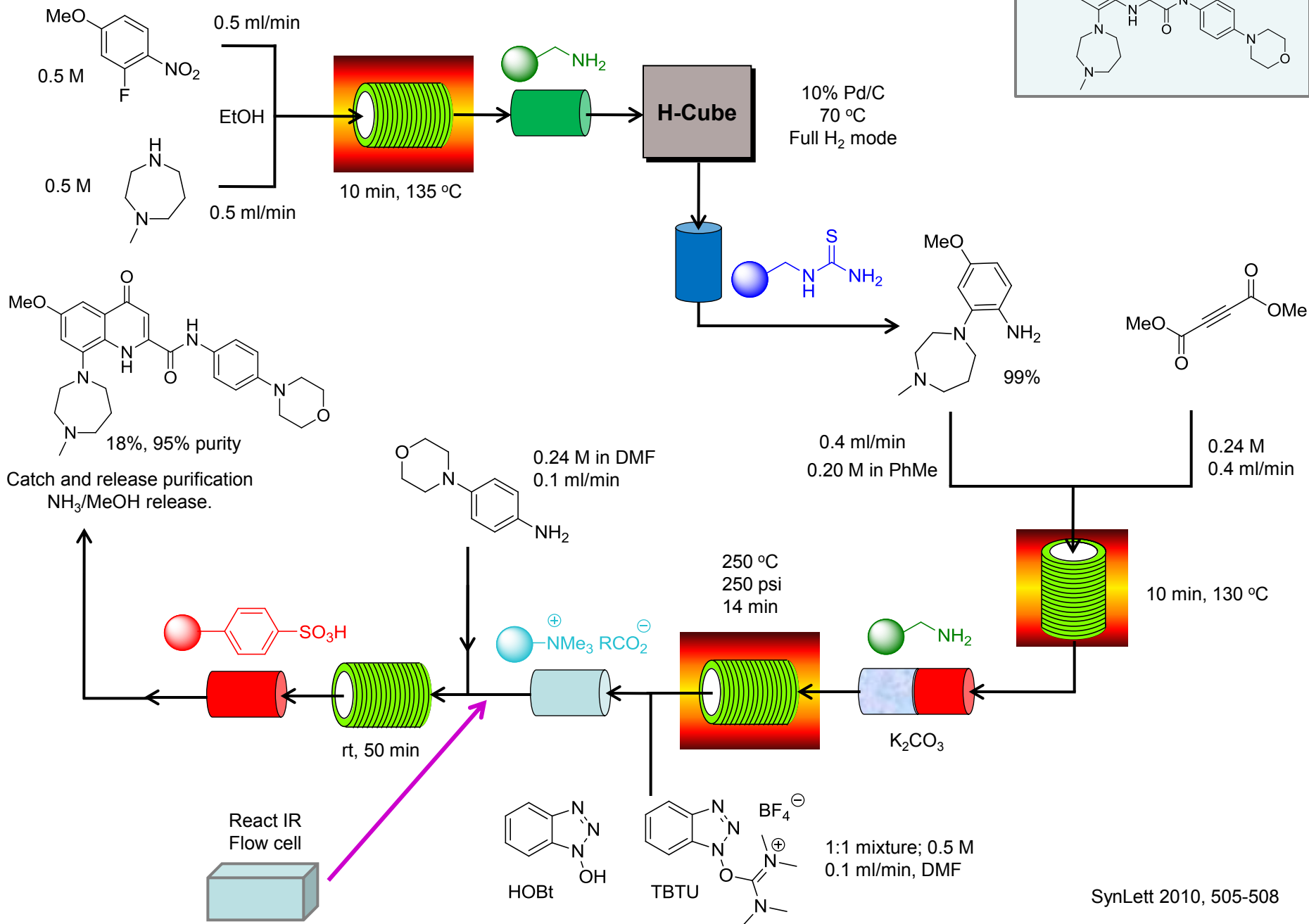
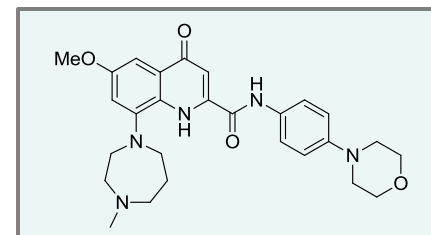


# $\delta$ -Opioid Receptor Agonist

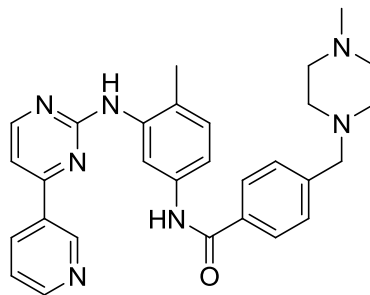




# Potent 5HT<sub>1B</sub> Antagonist



# Synthesis of Gleevec

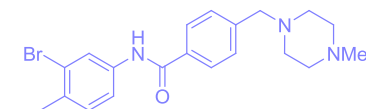


Gleevec

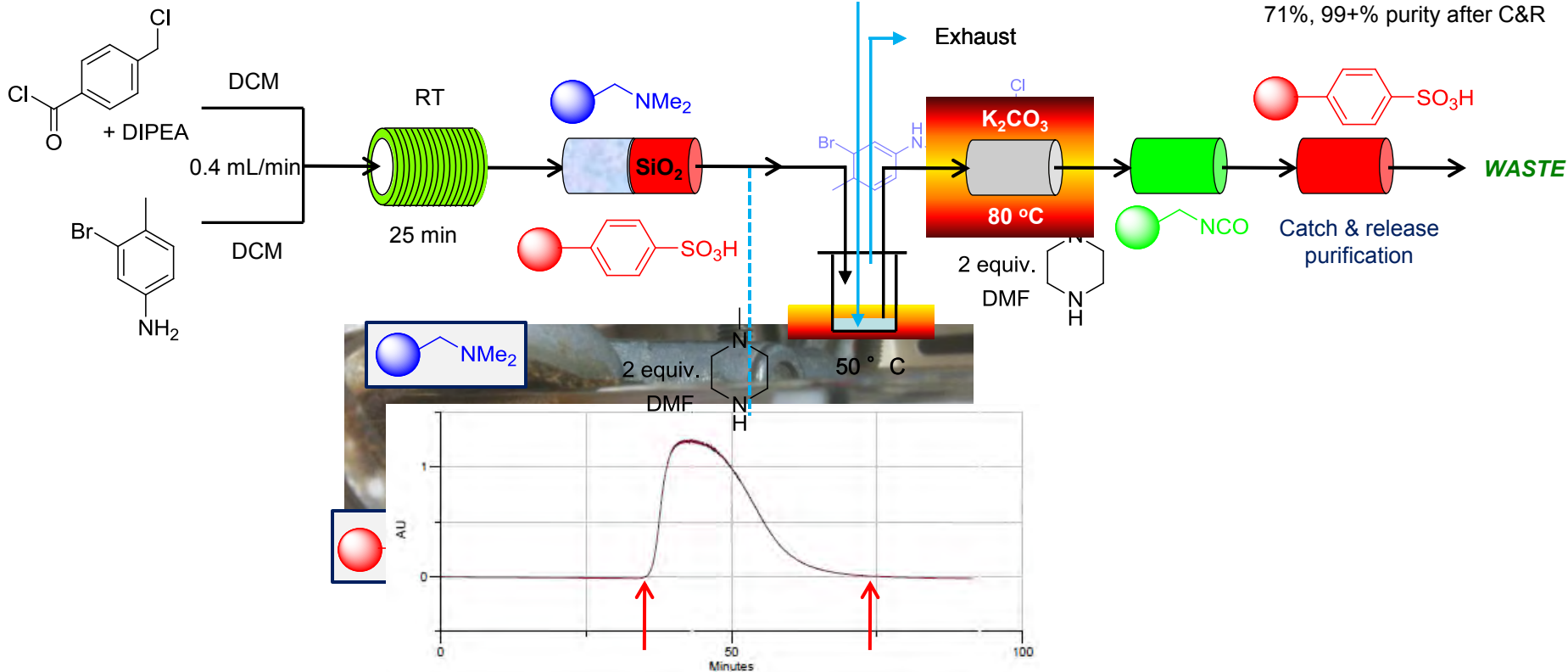
## Aim:

- Devise a flow-based synthesis of Gleevec that reduces the need for manual work-up/purification.
- Use the generic reactor to demonstrate library production from commercially available building blocks.
- Create a route that allowed for increased points of diversity in analogues construction.
- Demonstrate production and in-line screening of drug candidates using a known pharmaceutical.

# Synthesis of Gleevec

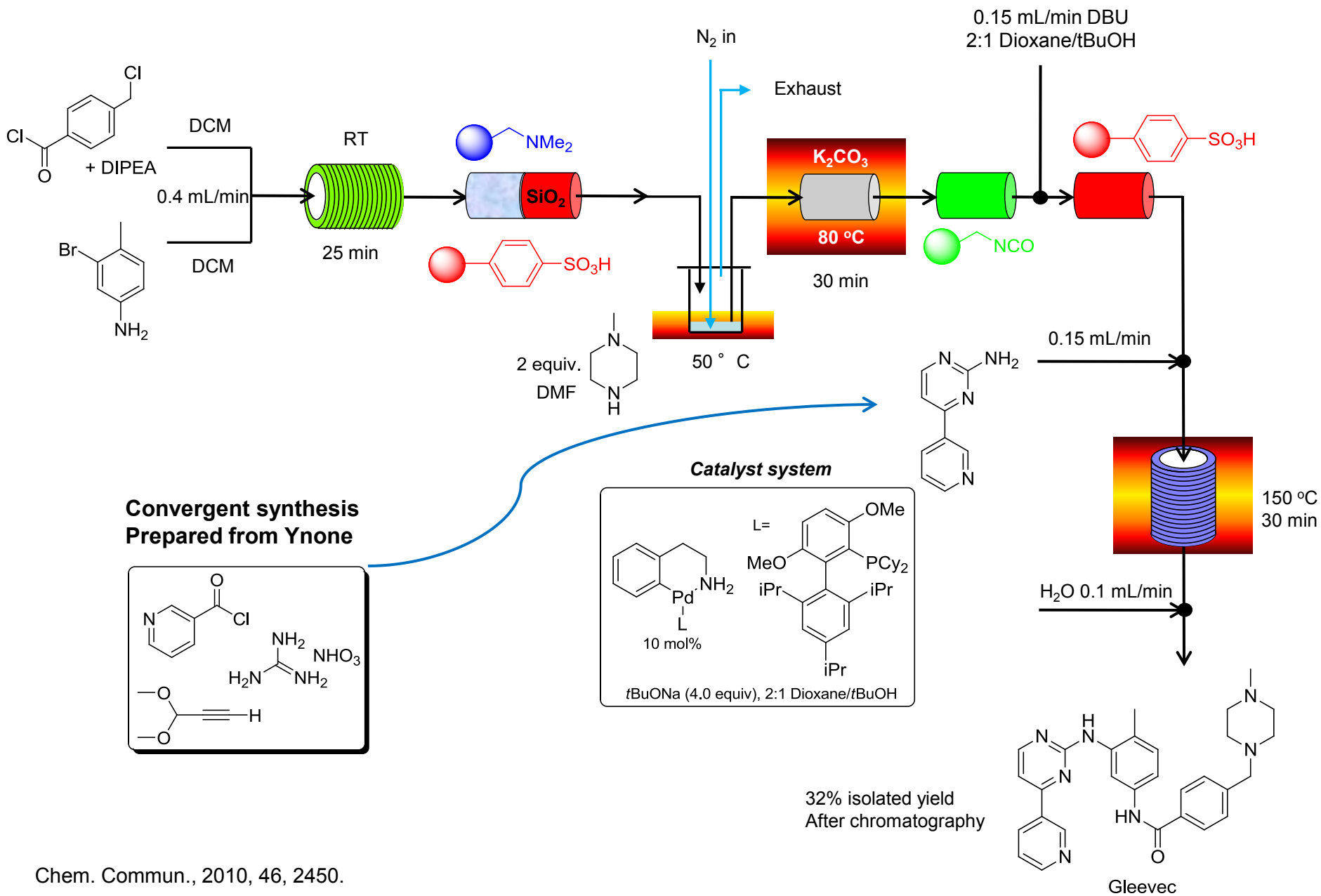


71%, 99+% purity after C&R



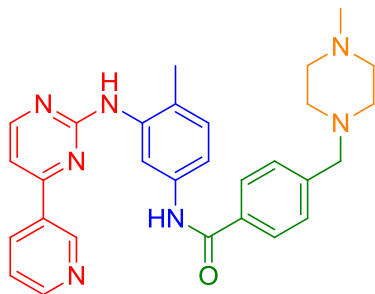
- Use UV triggered fraction collector to collect product into heated vial
- N<sub>2</sub> gas bubbled through the solution removes the DCM
- All product can be collected from the previous step – increased overall yield
- 80% isolated yield

# Synthesis of Gleevec

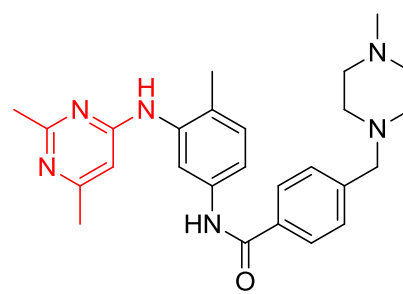


# Analogues of Gleevec

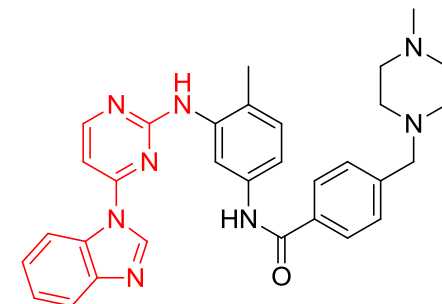
Route provides access to analogues not achievable via process route



Gleevec 32%

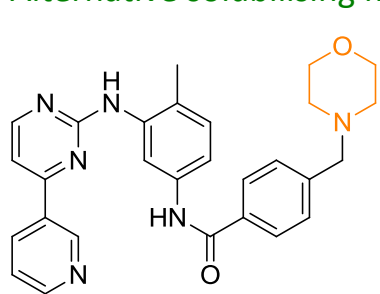


33%

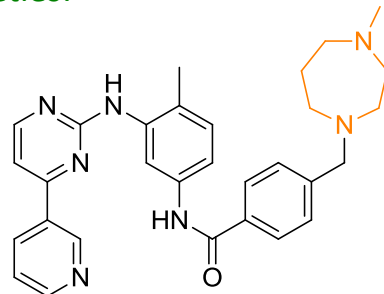


29%

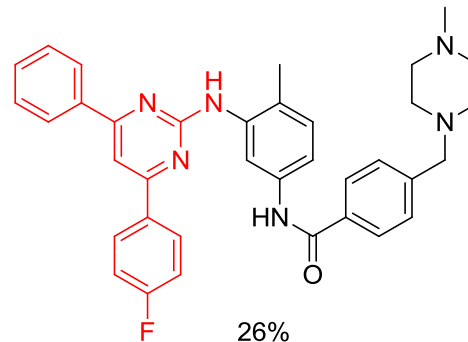
Alternative solubilising moieties:



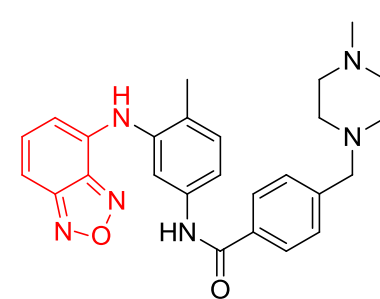
24%



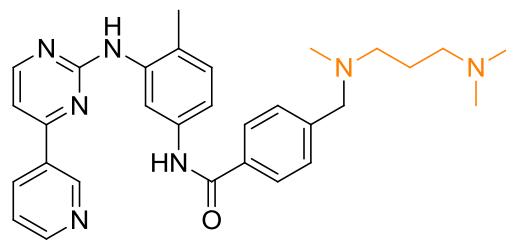
25%



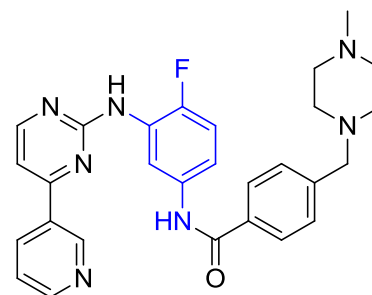
26%



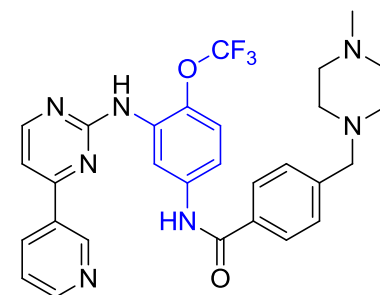
31%



24%

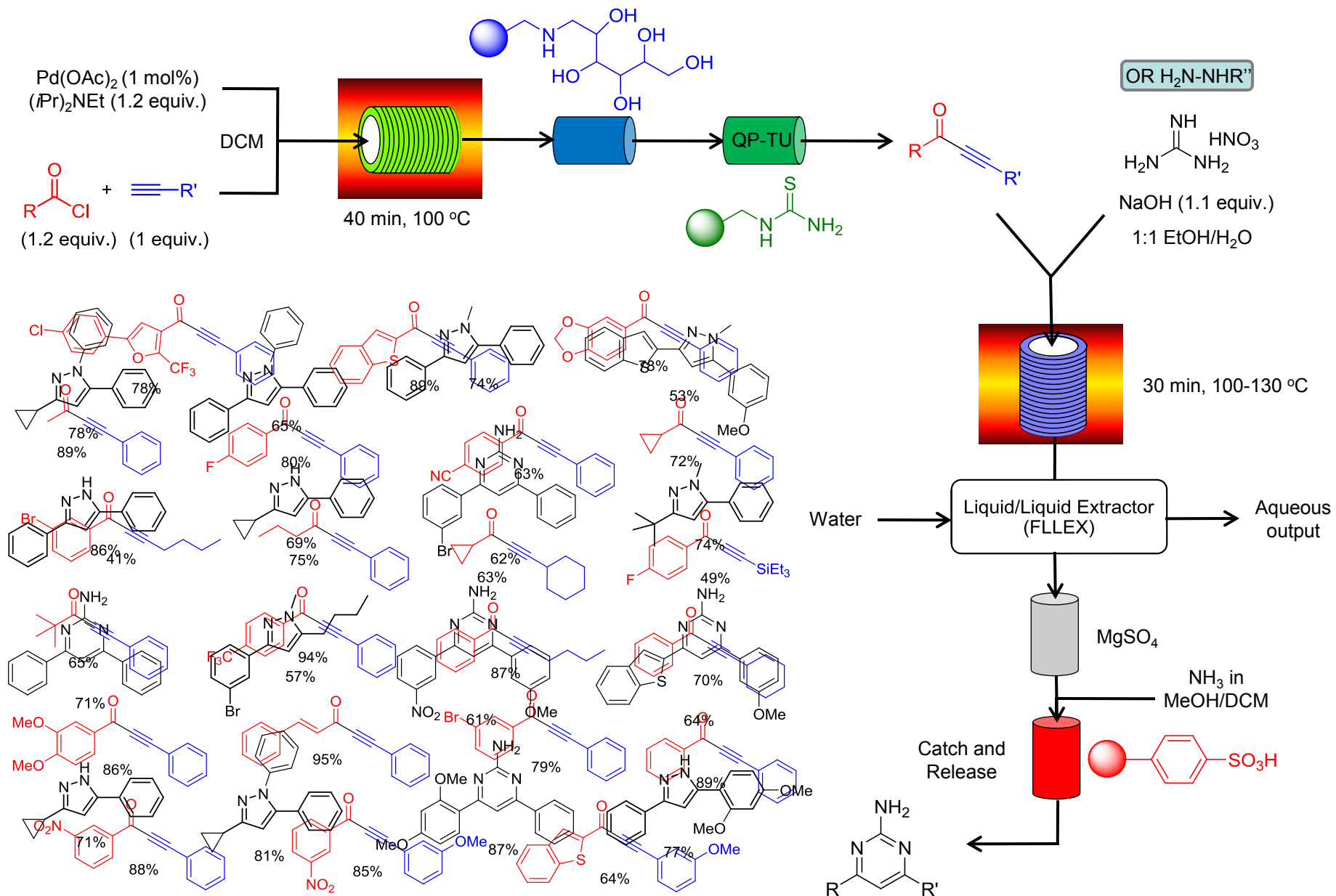


35%

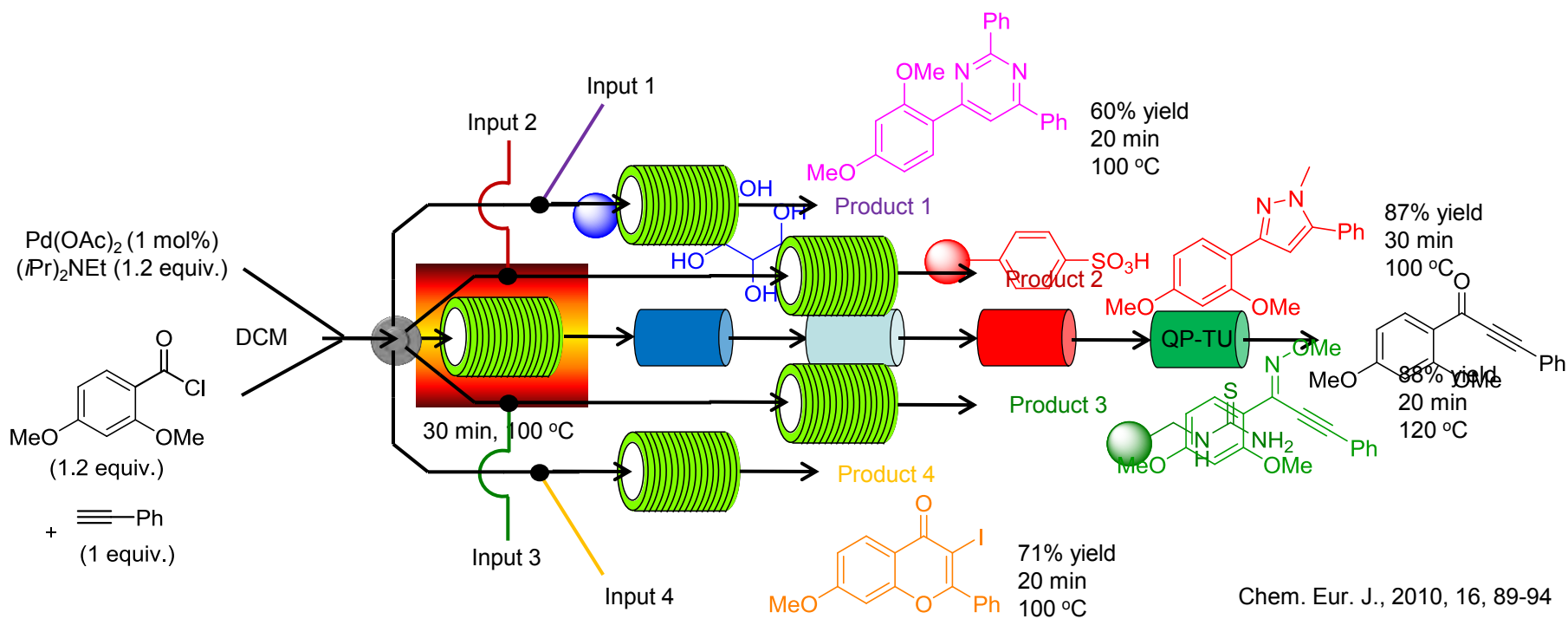
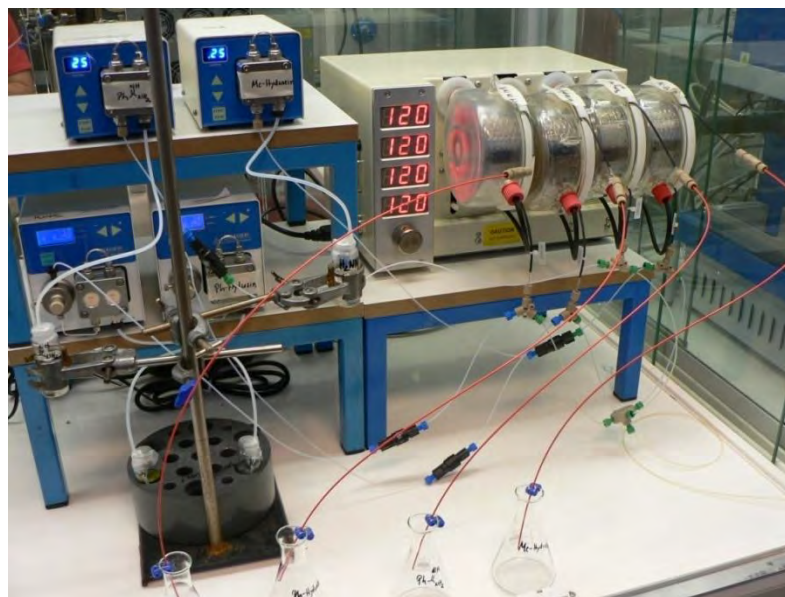


28%

# Ynone Synthesis – numbering out



# Stream Splitting in Flow



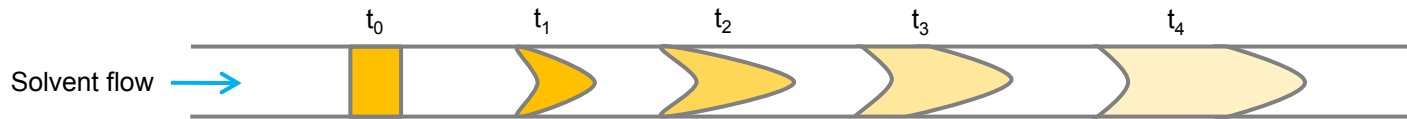
# Mixing and Dispersion

Dispersion Model accounts for diffusion

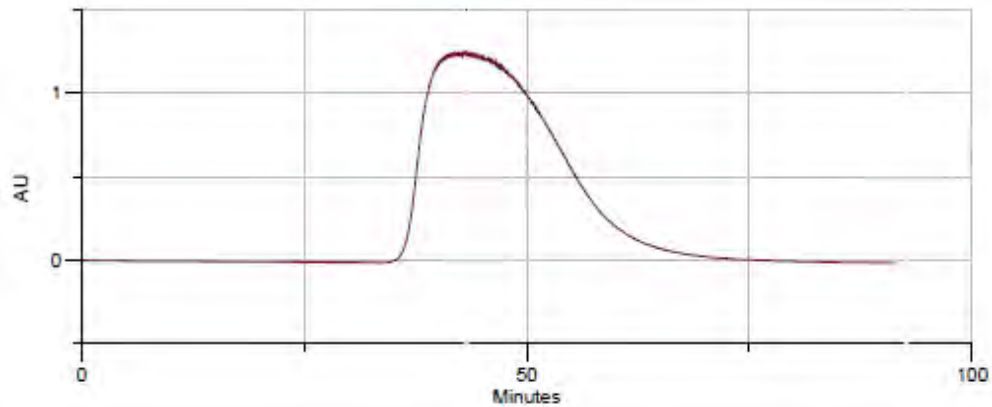
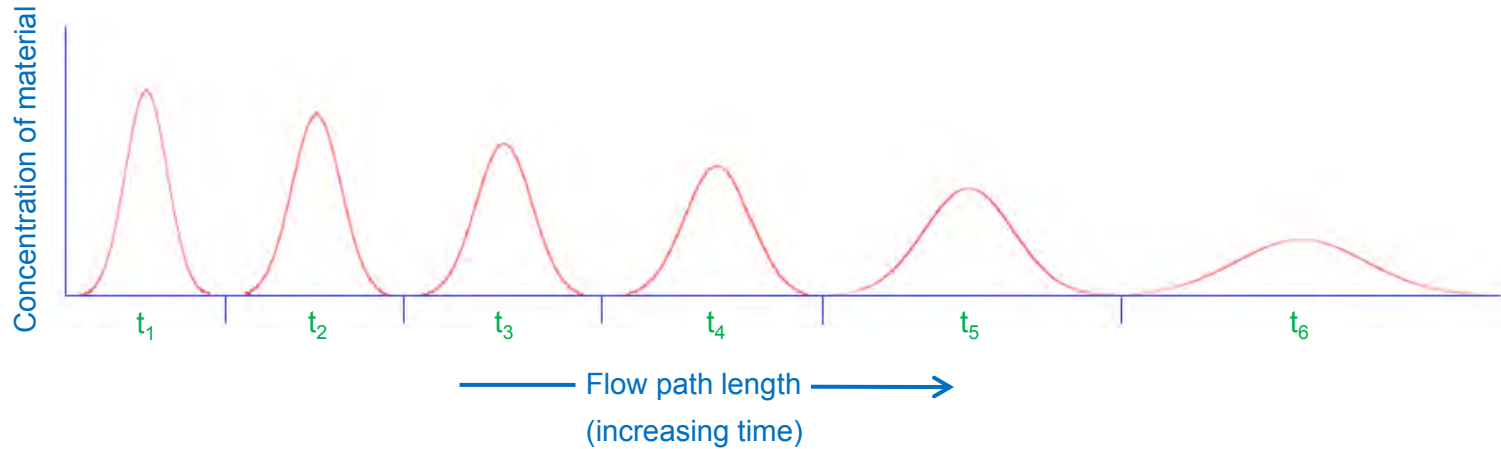
diffusion molecular

diffusion convective

Aris-Taylor dispersion in laminar flow or turbulent dispersion from eddies

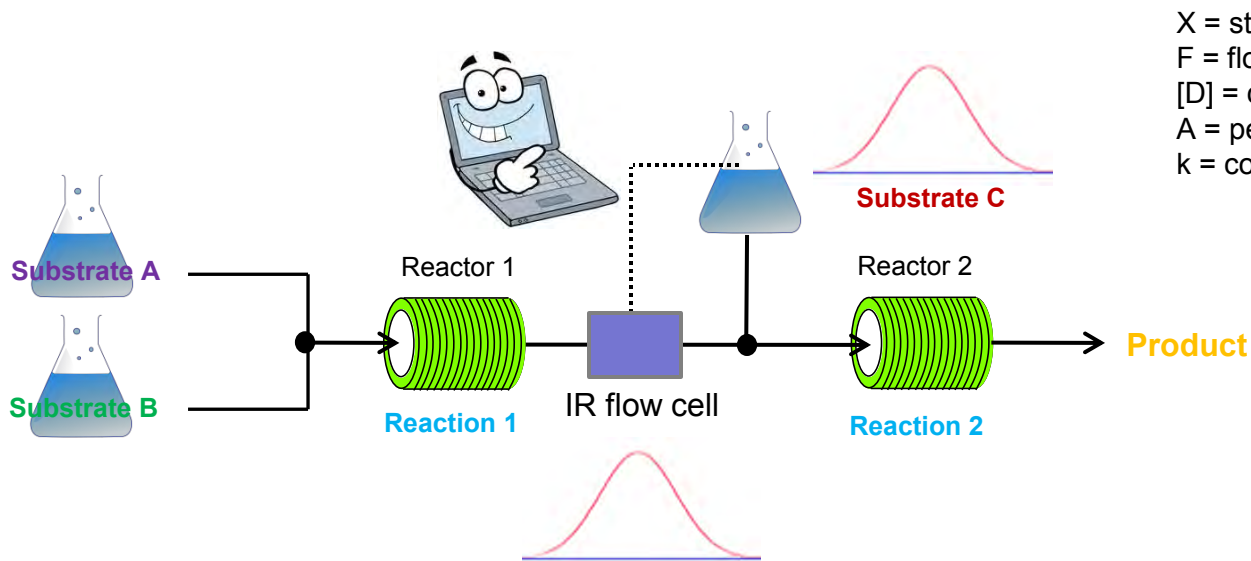
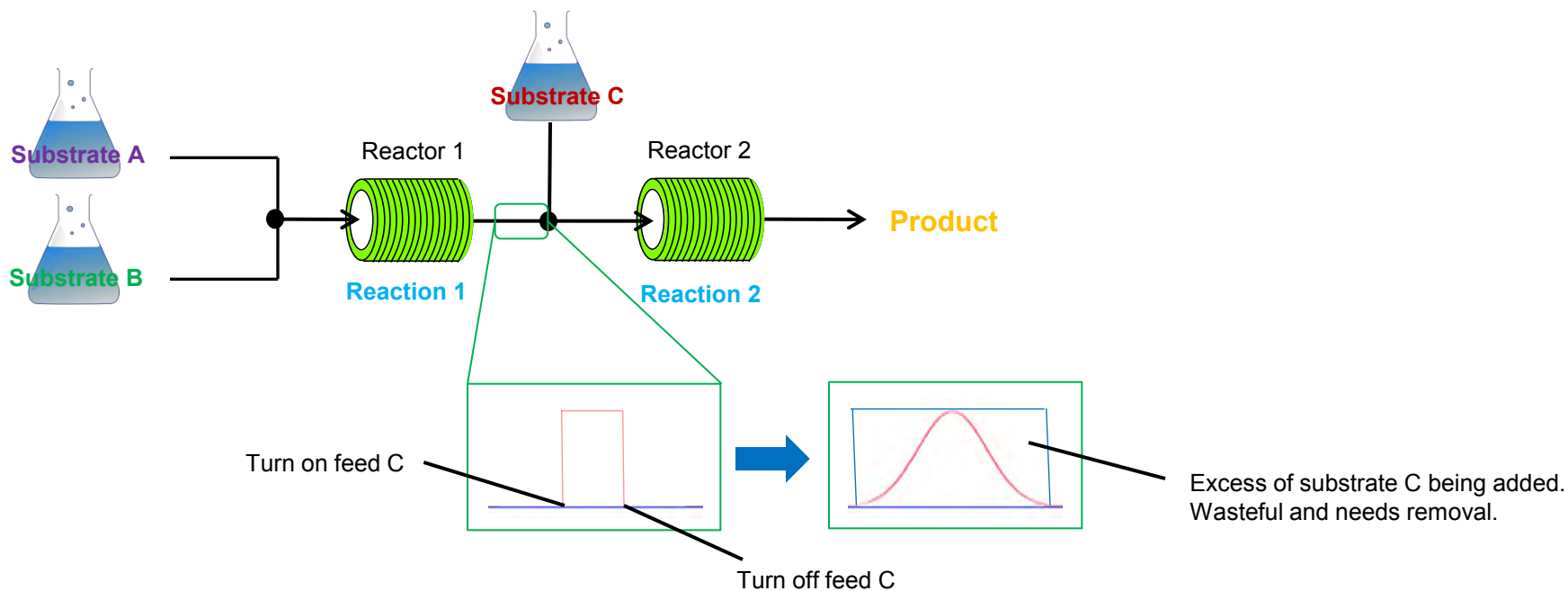


Addition into  
flow stream





# The third stream issue

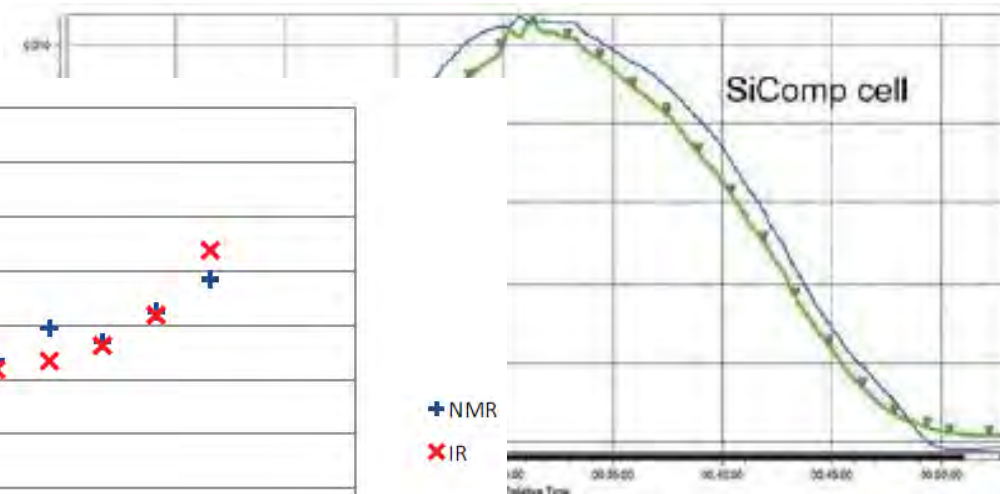
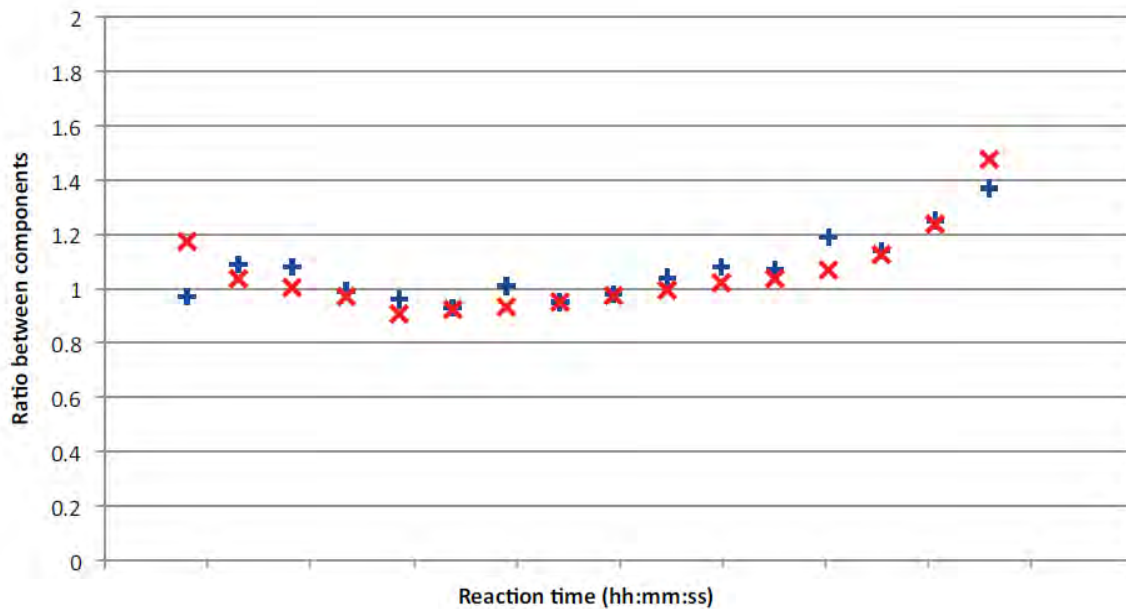
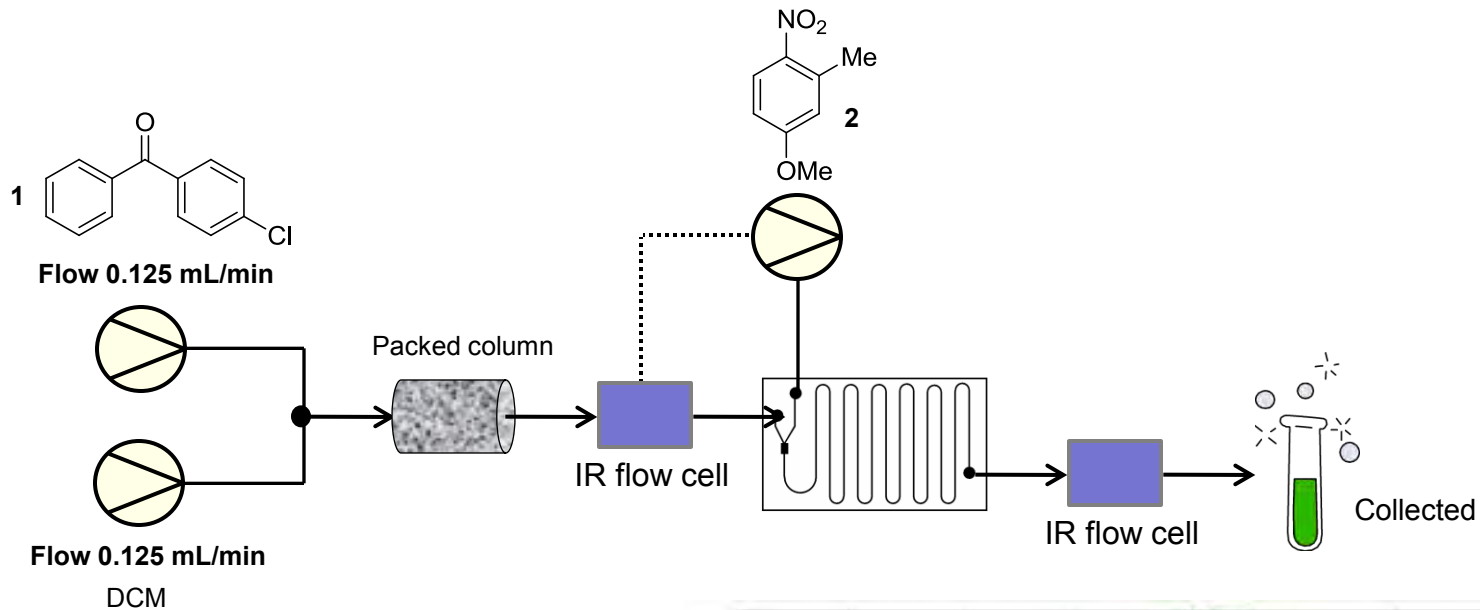


X = stoichiometry between the two components  
 F = flow rate of output process  
 [D] = conc. of third stream component  
 A = peak height value measured by IR  
 k = conversion factor

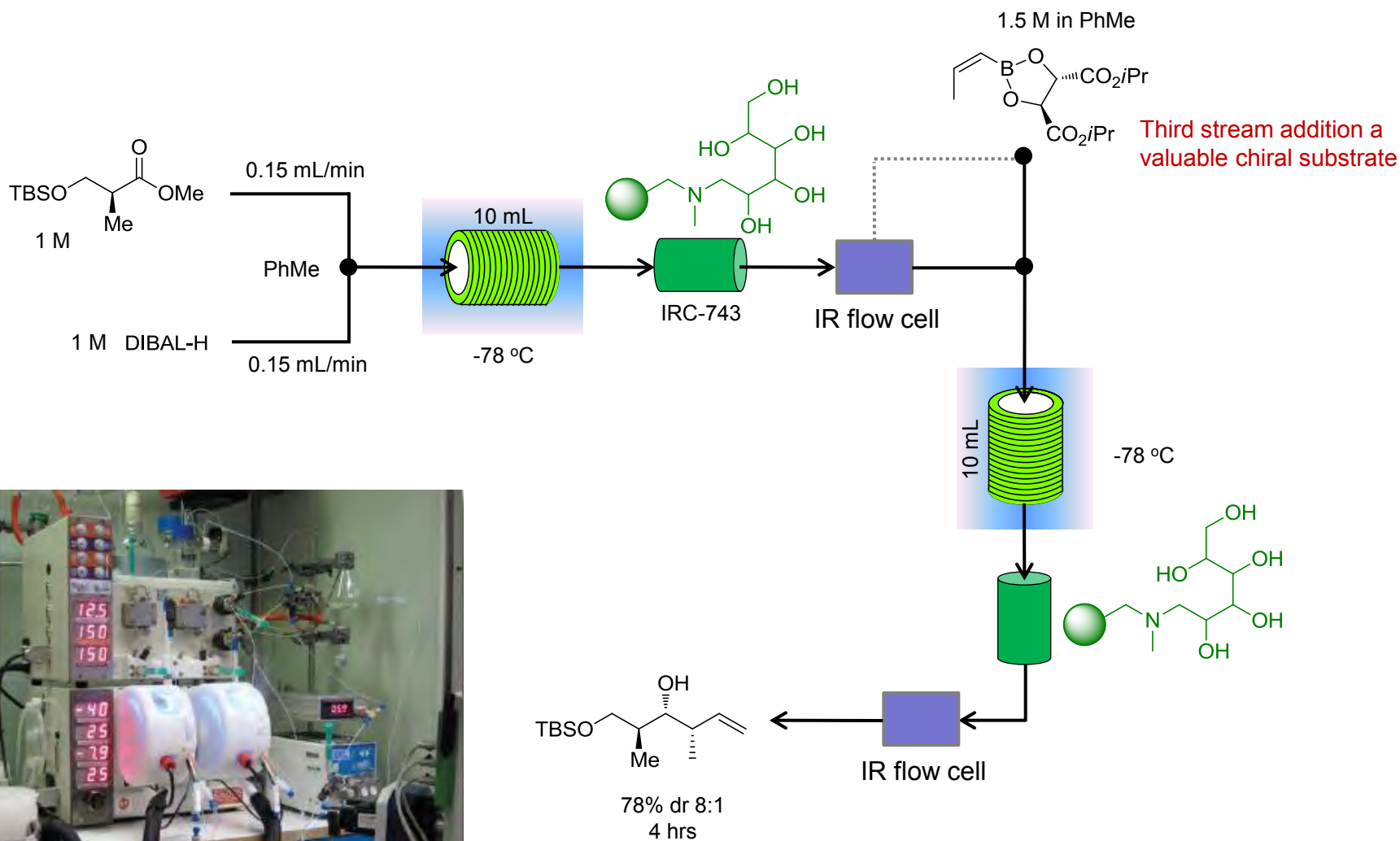
$$\text{Flow rate} = \frac{X \cdot F \cdot k}{[D]}$$



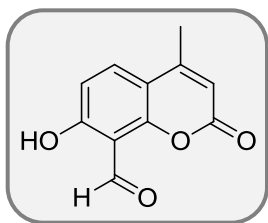
# The third stream issue



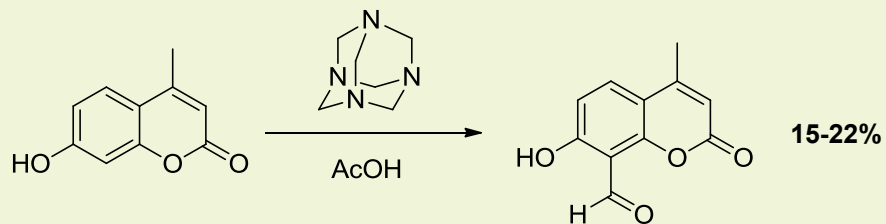
# The third stream issue



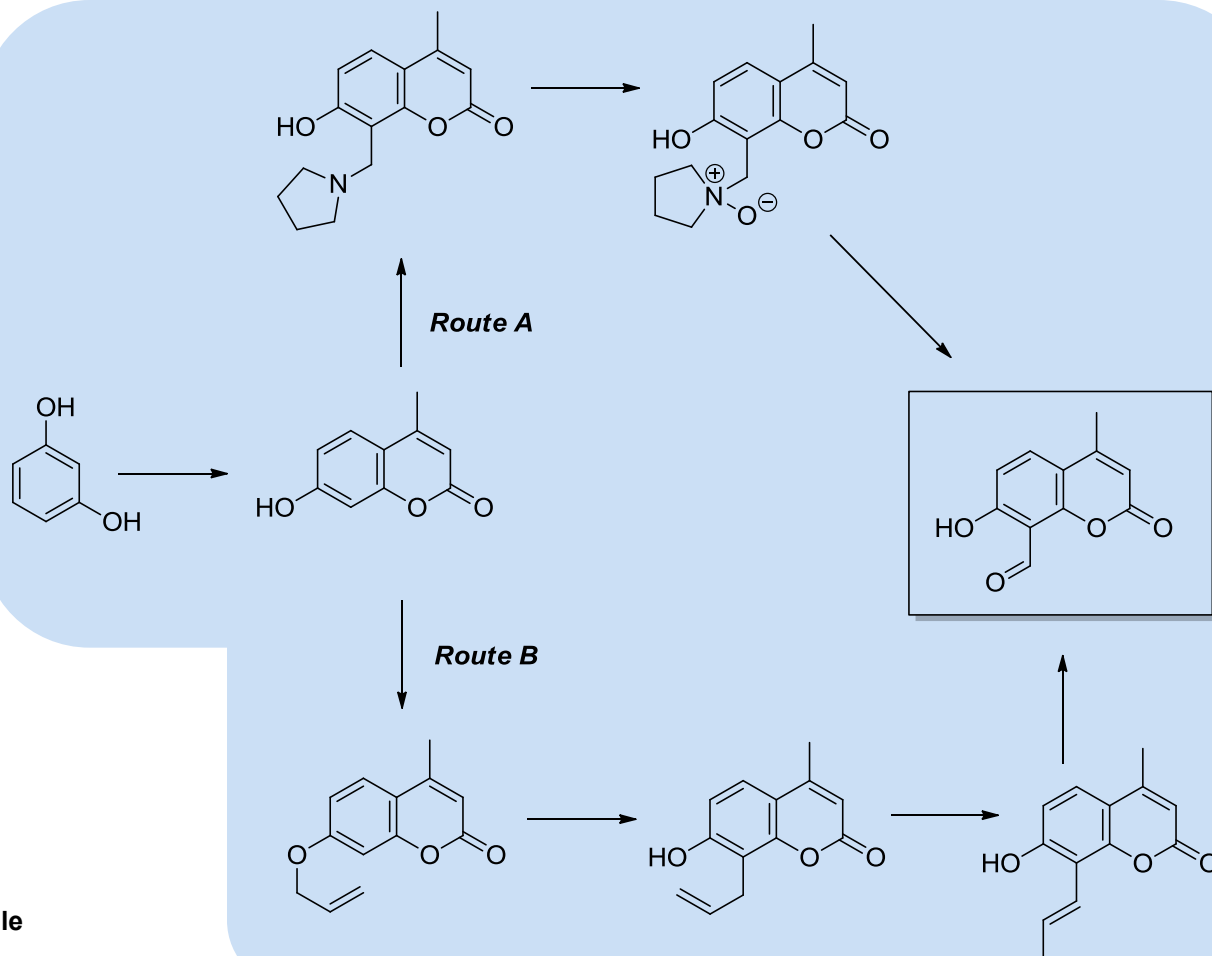
# Synthesis of an IRE-1 binding probe



## Duff Reaction

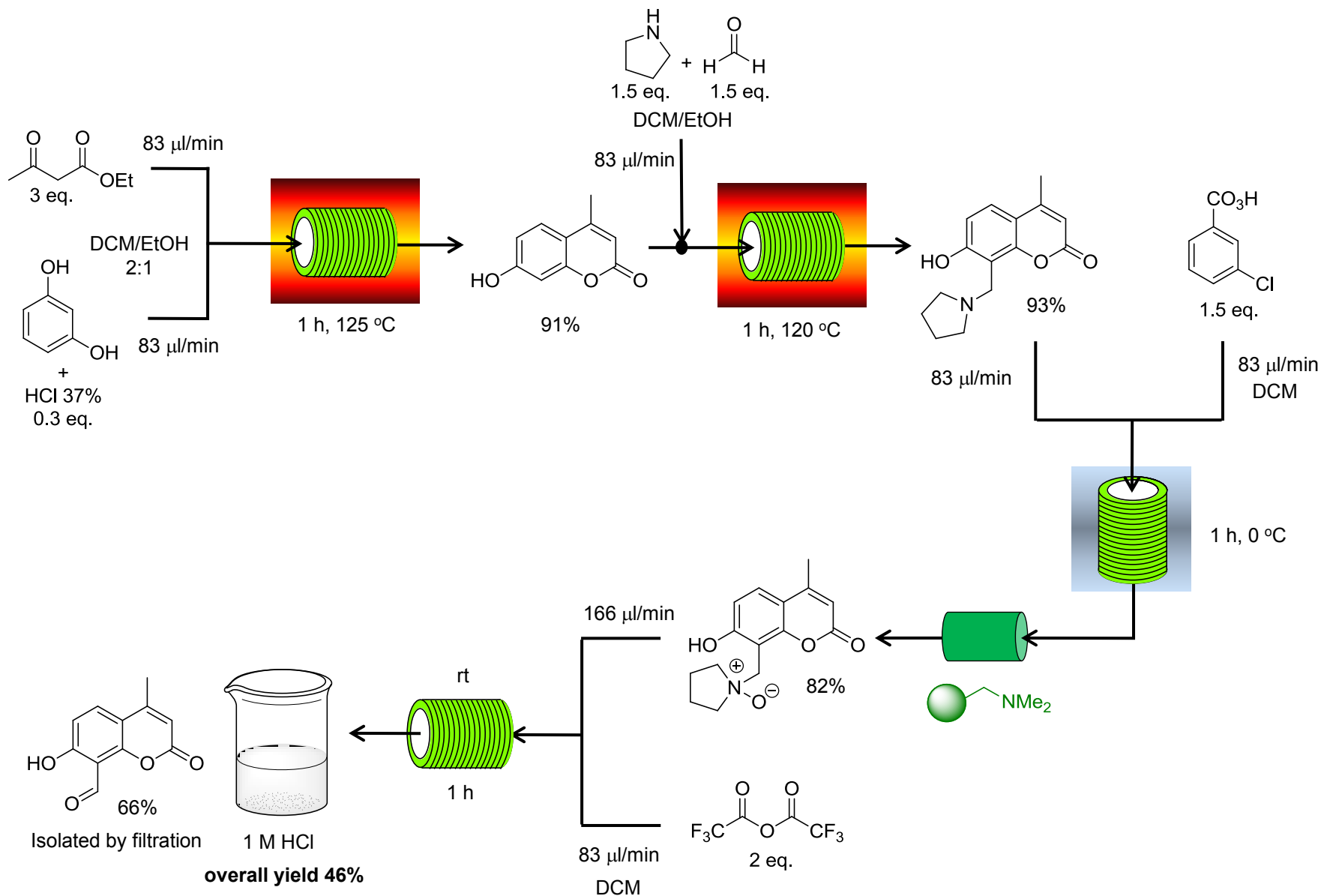


- Cheap starting materials/reagents
- Scalable via the same route
- Highly reproducible
- Automated synthesis
- Avoid work-up/purification

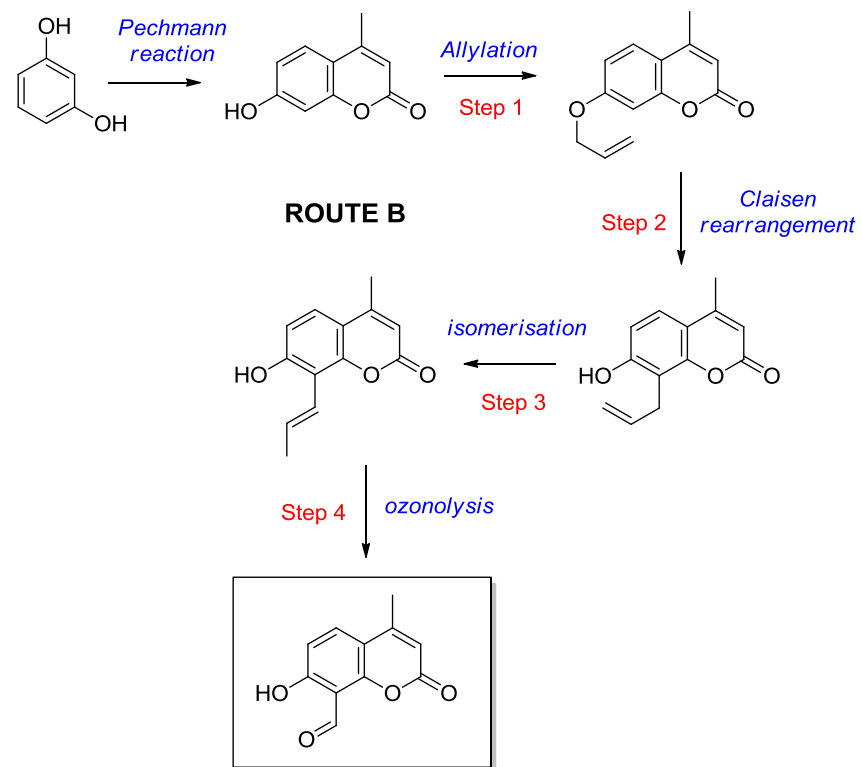


Selective inhibition of unconventional mRNA splicing by an IRE1-binding small molecule

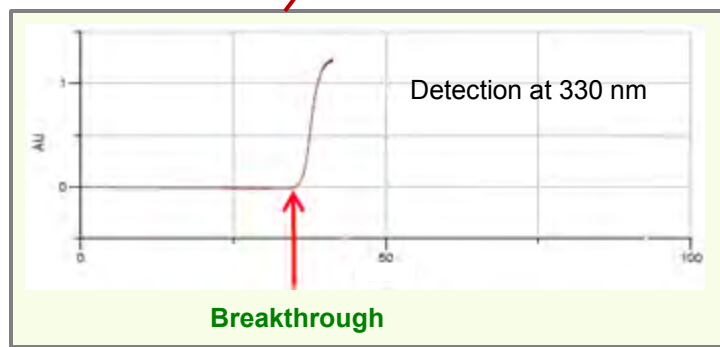
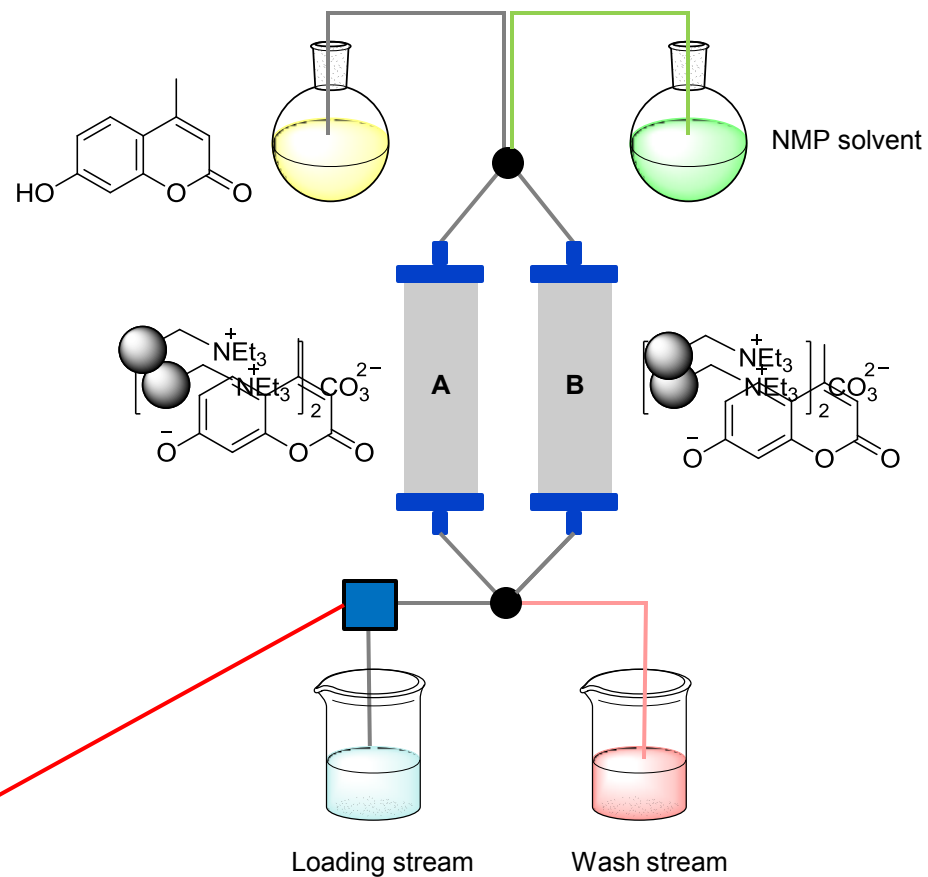
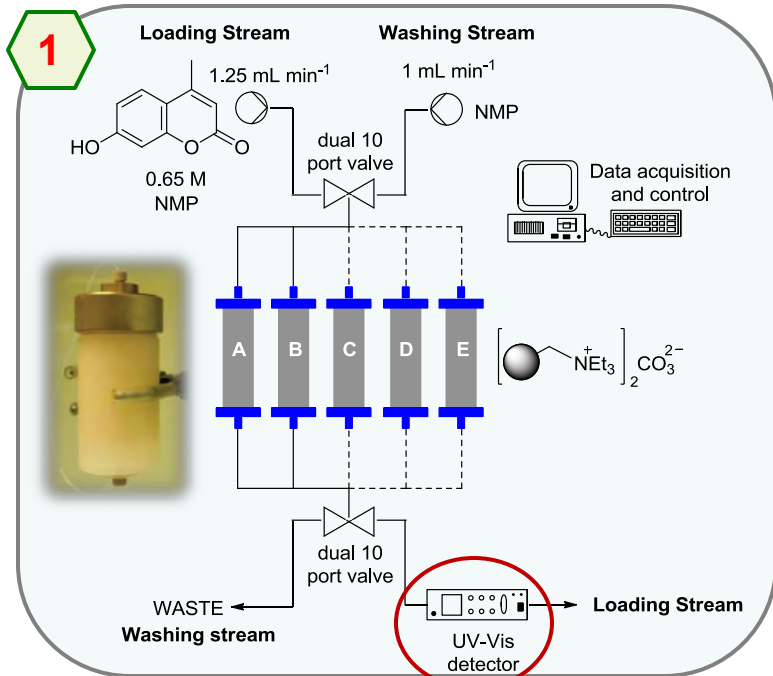
# Route A: *N*-oxide Derived Synthesis



# Route B: Claisen Rearrangement



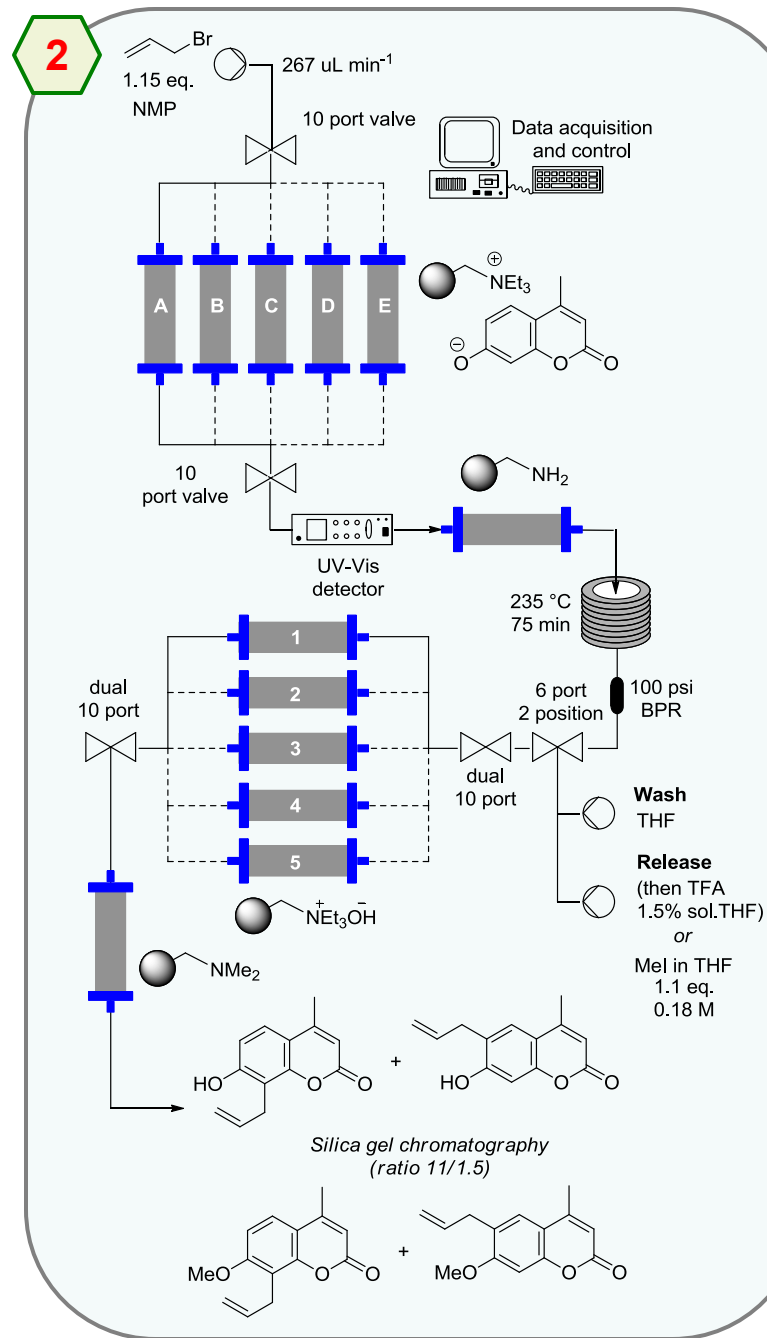
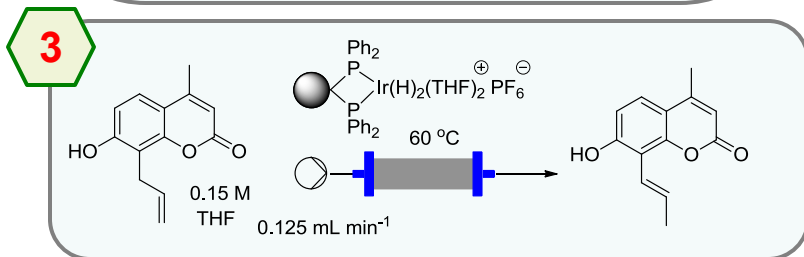
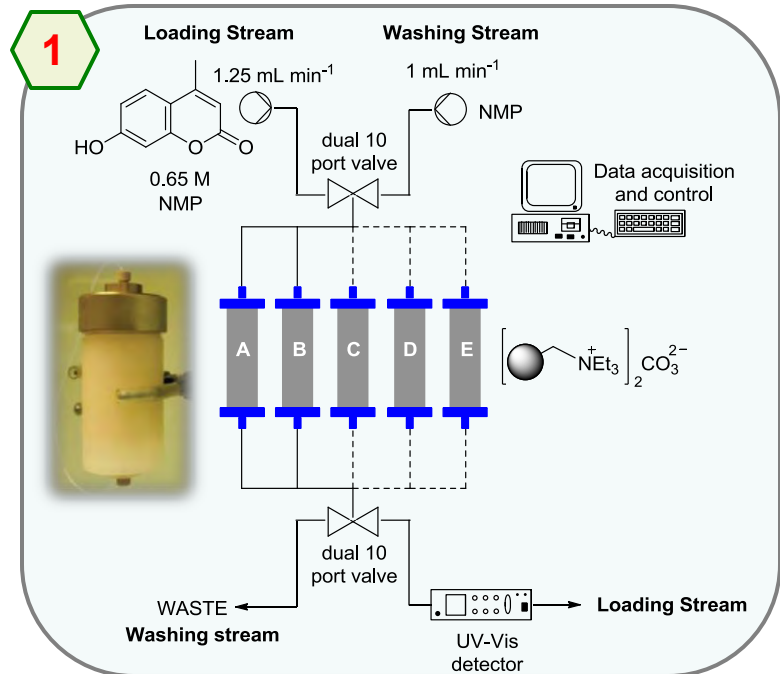
# Route B: Claisen Rearrangement



**10 cartridges loaded sequentially  
in a fully automated procedure**

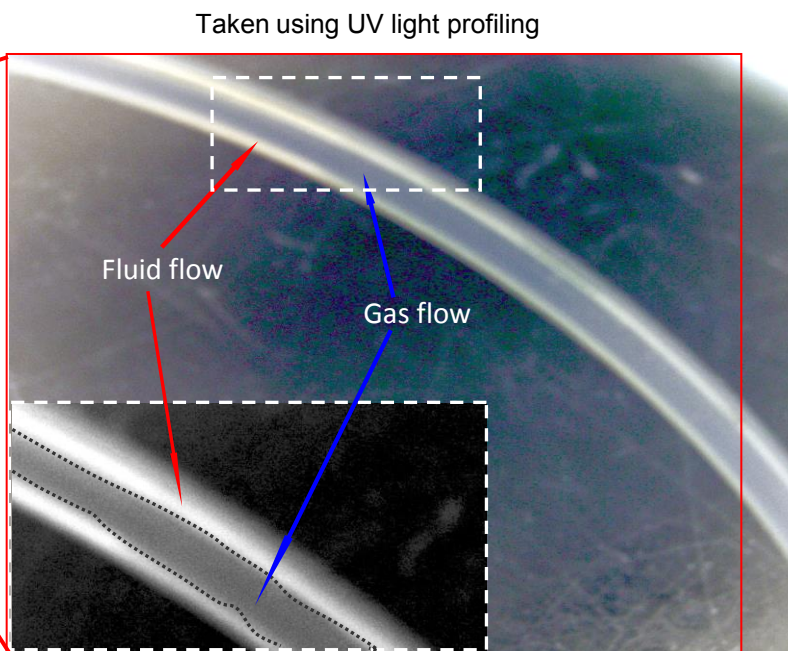
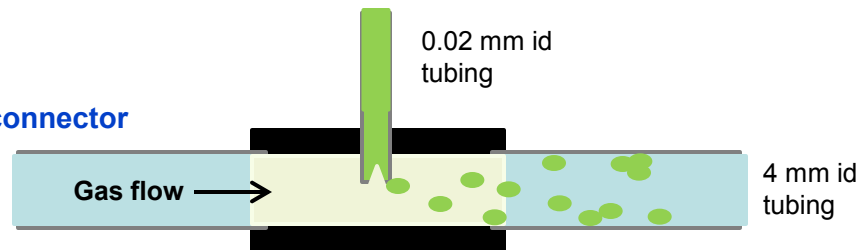
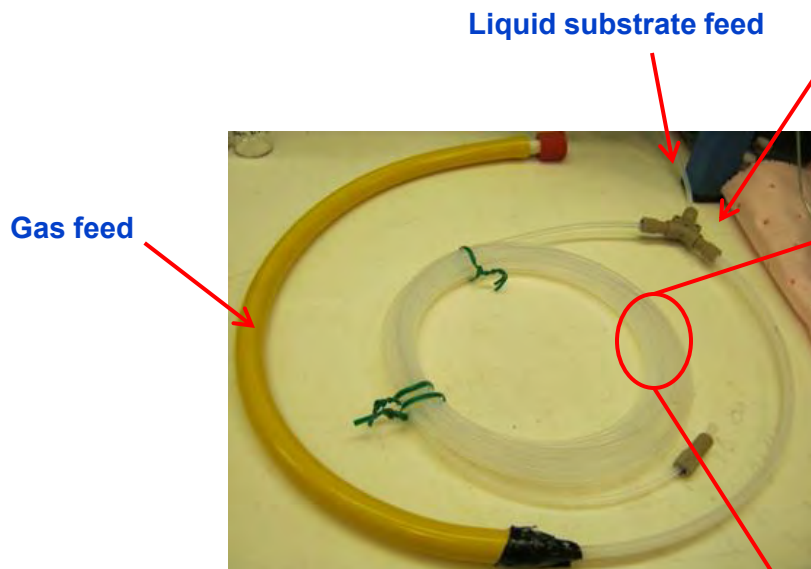
**~ 2 M of substrate**

# Route B: Claisen Rearrangement

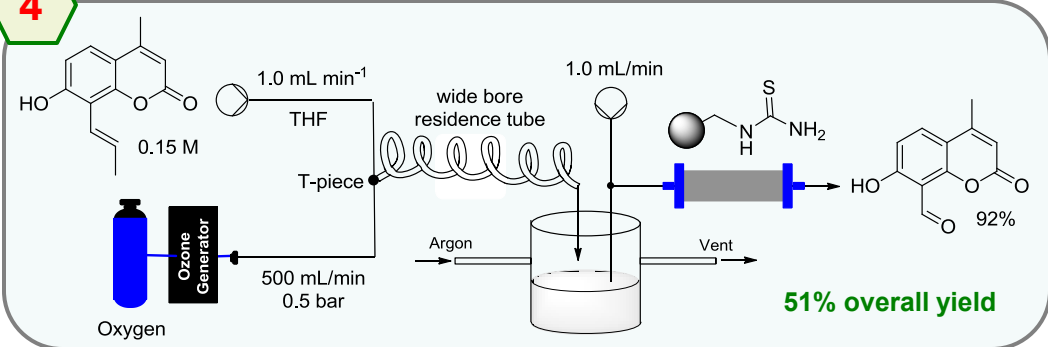




# Route B: Claisen Rearrangement



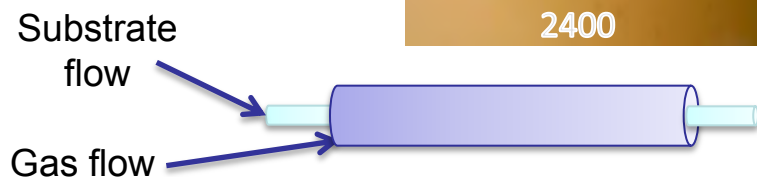
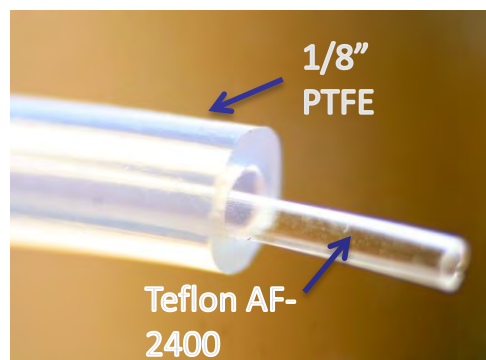
4



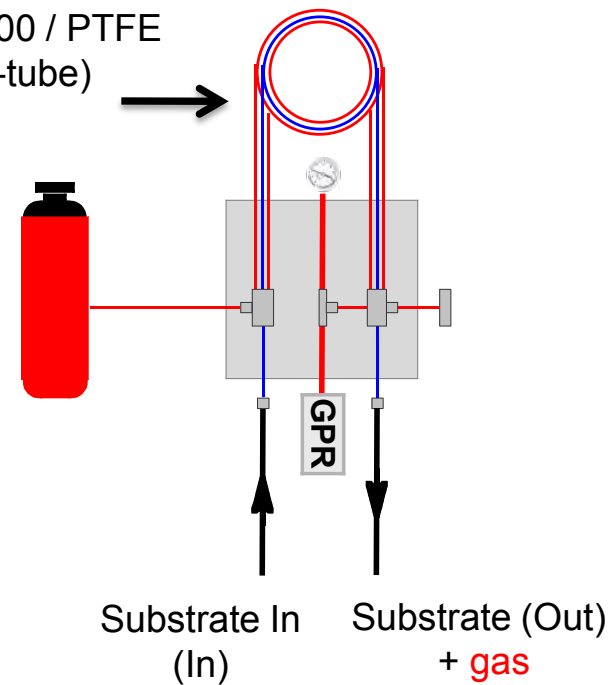
# Tube-In-Tube Gas-Liquid Flow Reactor



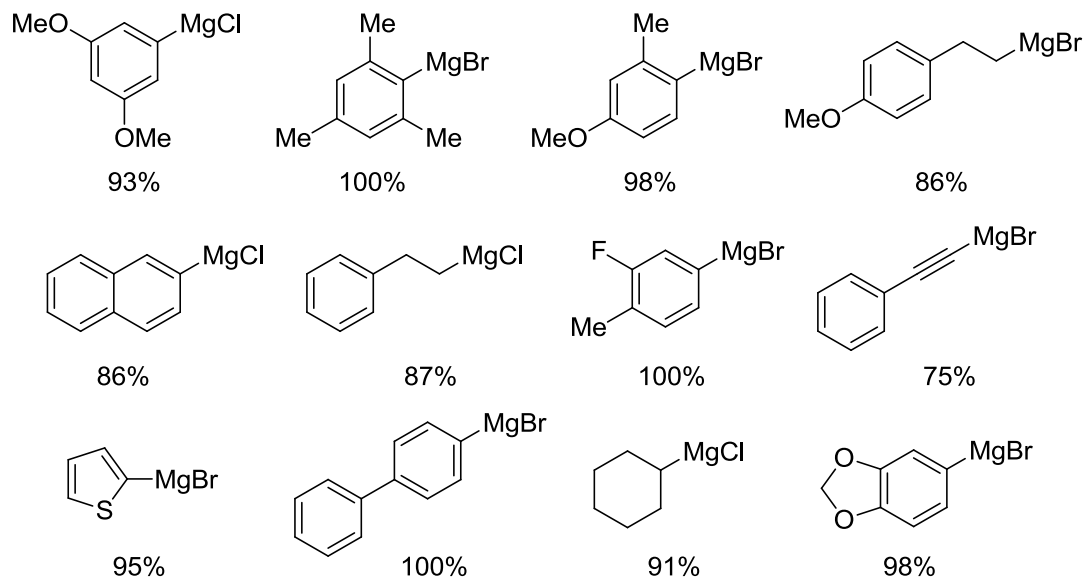
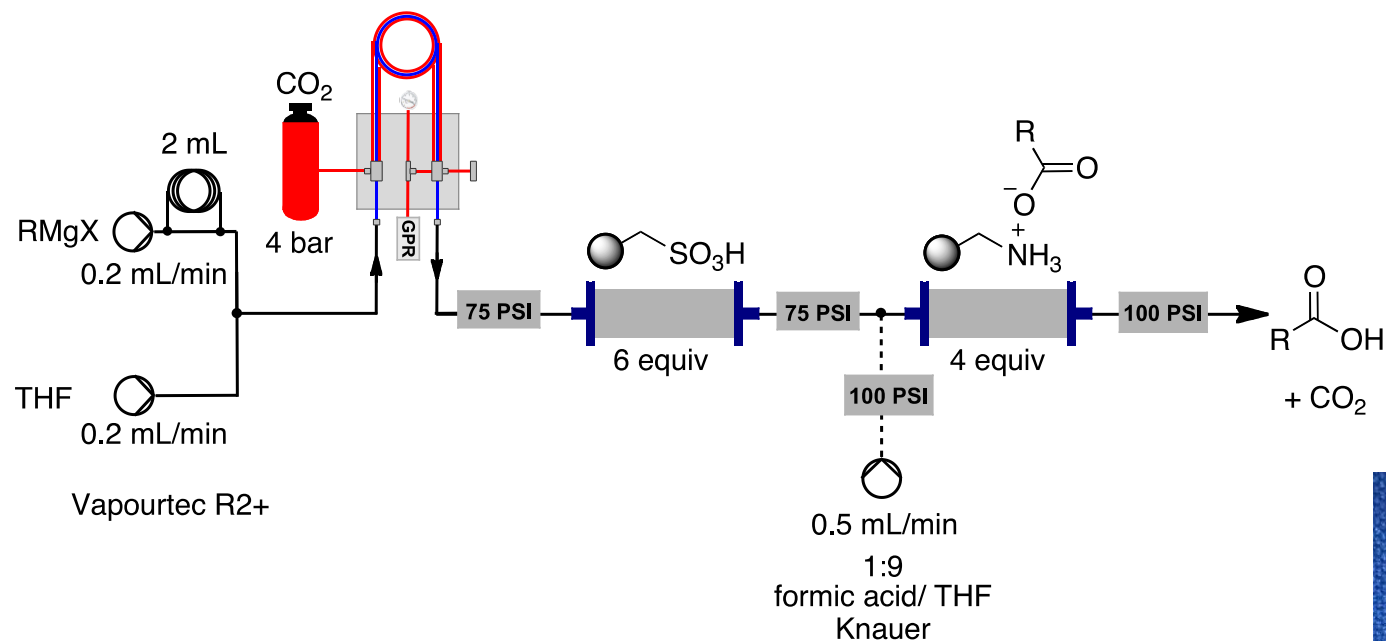
- reactor volume 0.28-0.56 mL (1-2 m Teflon AF-2400)
- gas pressure 10-35 bar
- flow rates 0.1-10 mL/min



Teflon AF-2400 / PTFE  
(Tube-in-tube)



# Carbonylations of Grignard Reagents

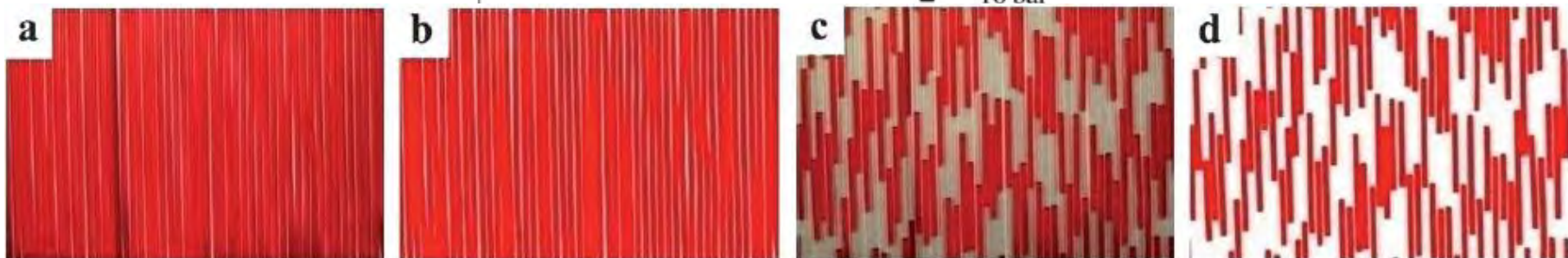
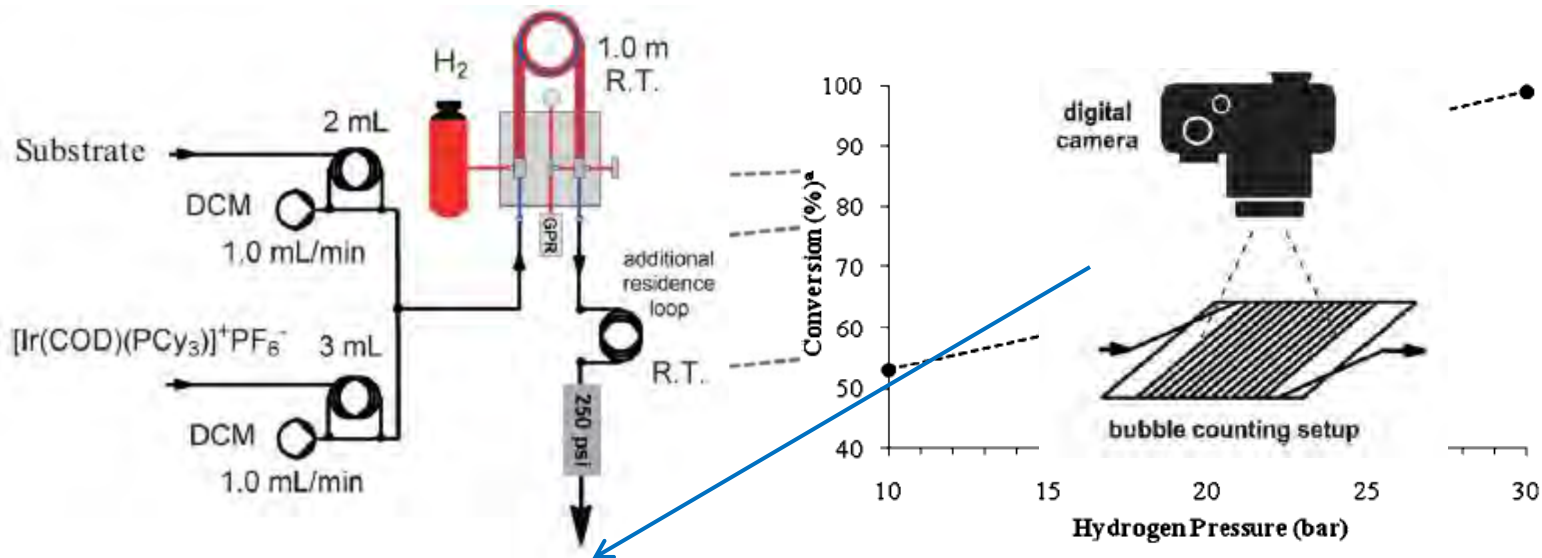


5-8 g resin

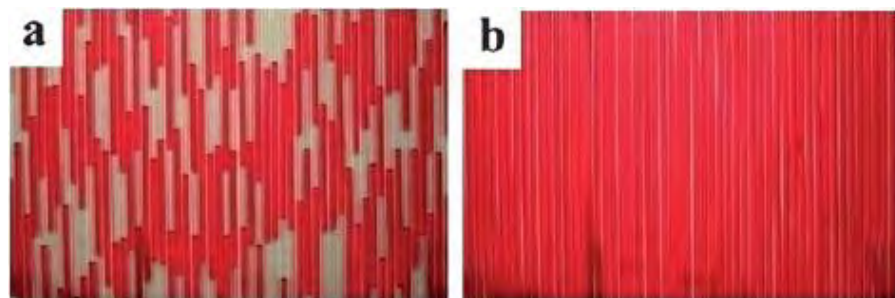
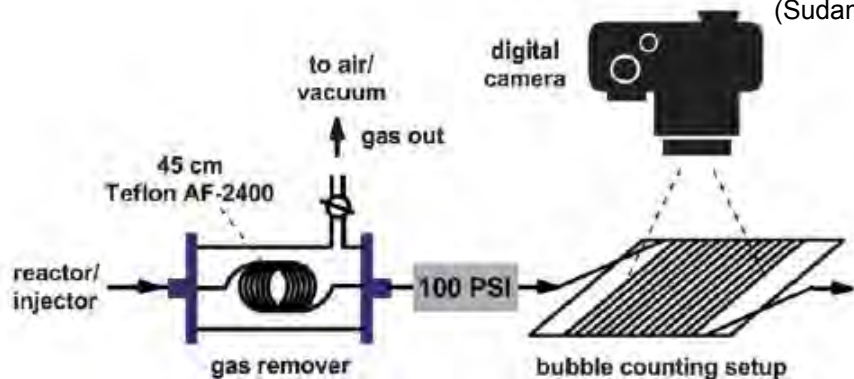


55-65 g of resin

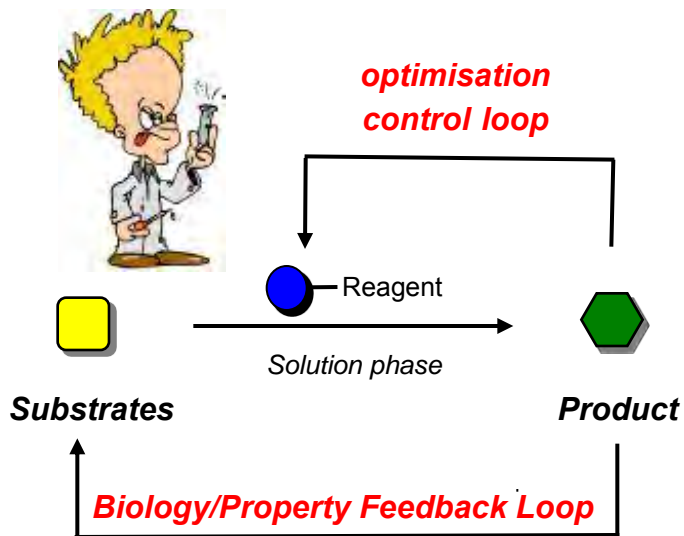
# Hydrogenations using a Tube-in-Tube reactor



(Sudan red 7B in DCM)

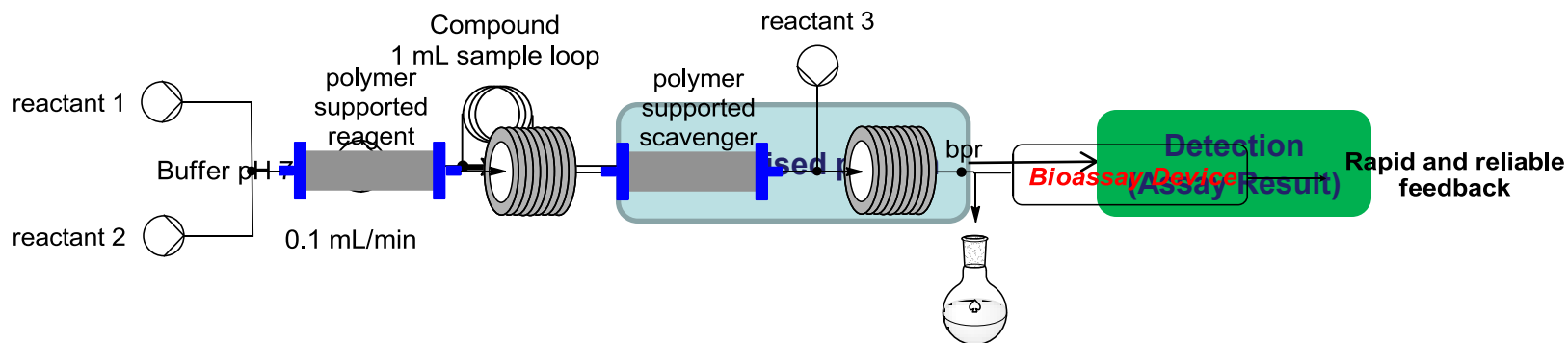


# Proof of Concept Design



## What to make

- SAR
- ADME/Tox
- Chemotype profiles
- Validation



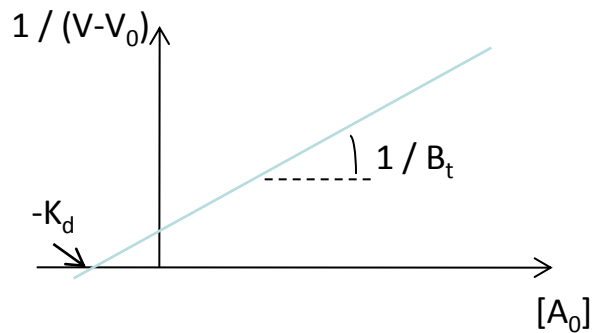
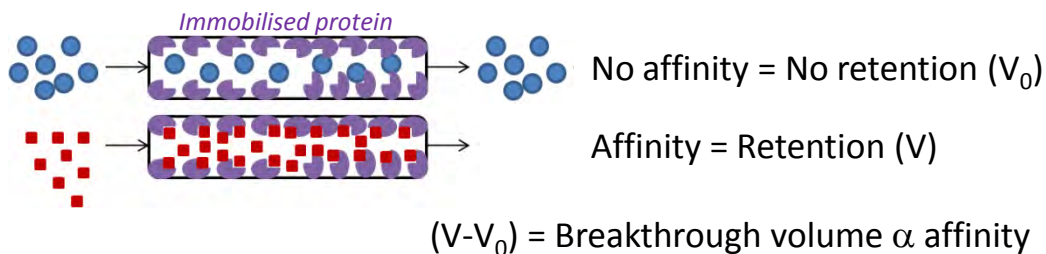
# Frontal Affinity Chromatography

Continuous infusion of analyte over immobilised target

Injection of several concentrations gives access to  $K_d$

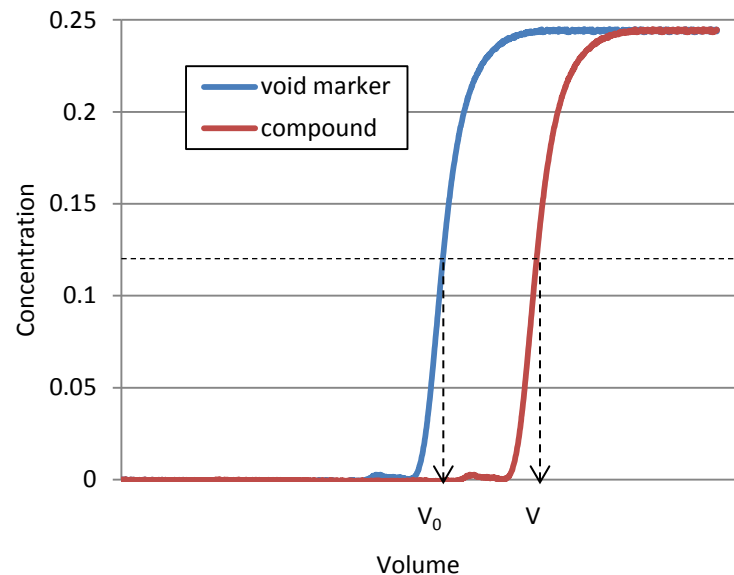
Compatible with existing Flow Chemistry platforms

Method to calculate  $B_t$  directly: biocatalyst application



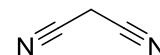
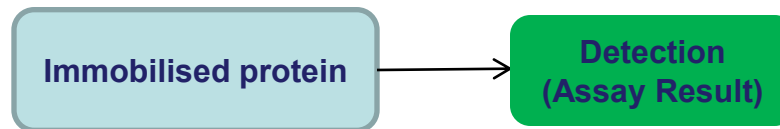
$$1 / (V-V_0) = (1 / B_t) [A_0] + K_d / B_t$$

$B_t$  = amount of immobilised protein

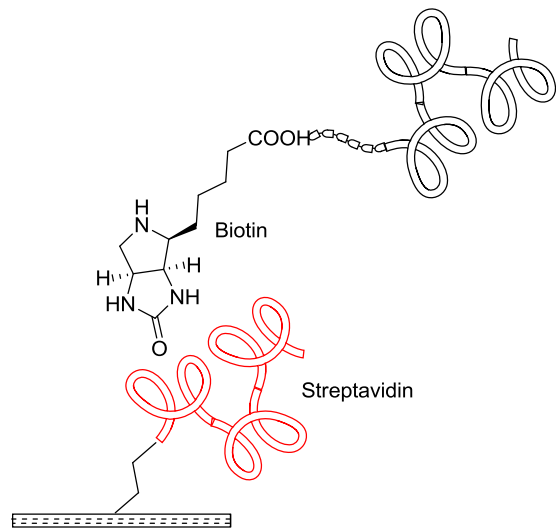


Amount bound give access to  $K_d$  using:

$$[A_0] (V-V_0) = \frac{B_t [A_0]}{[A_0] + K_d}$$

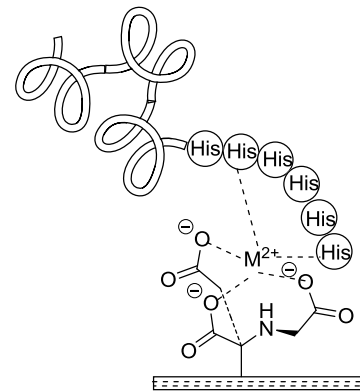
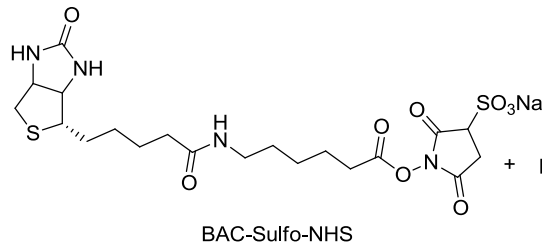


Void marker



Biotin-streptavidin  $k_d=10^{-15}$

- MALDI-TOF was used for characterisation of biotinylated HSA



Hexahistidine tagged protein  
Weaker interaction, Cu strongest

- His-tag not strong enough, protein is washed out

## Downsizing the column:



2.5-23  $\mu\text{L}$



15  $\mu\text{L}$



31  $\mu\text{L}$



175-353  $\mu\text{L}$

## Objective:

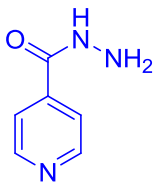
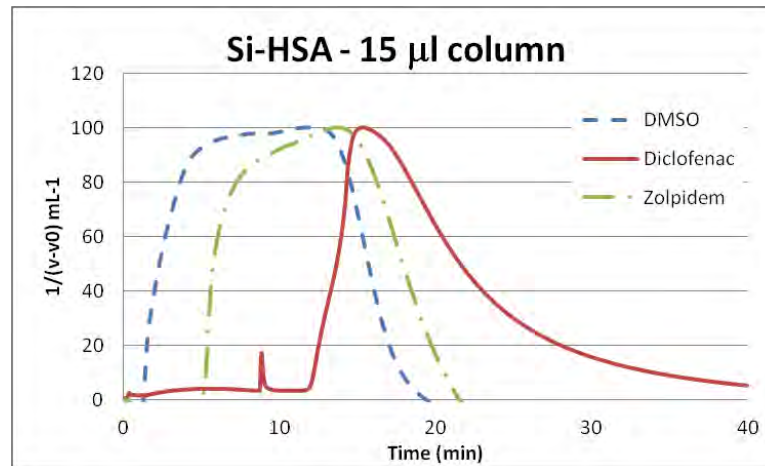
To assess the system using Human Serum Albumin (HSA)

HSA column

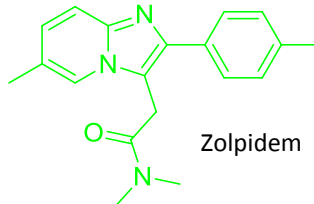


(1 mm x 2 cm)  
volume of 15  $\mu$ l

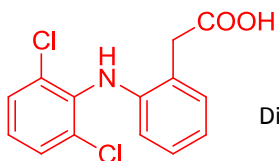
10 mM sodium phosphate  
2.7 mM KCl  
137 mM NaCl , pH = 7.4



Isoniazid



Zolpidem



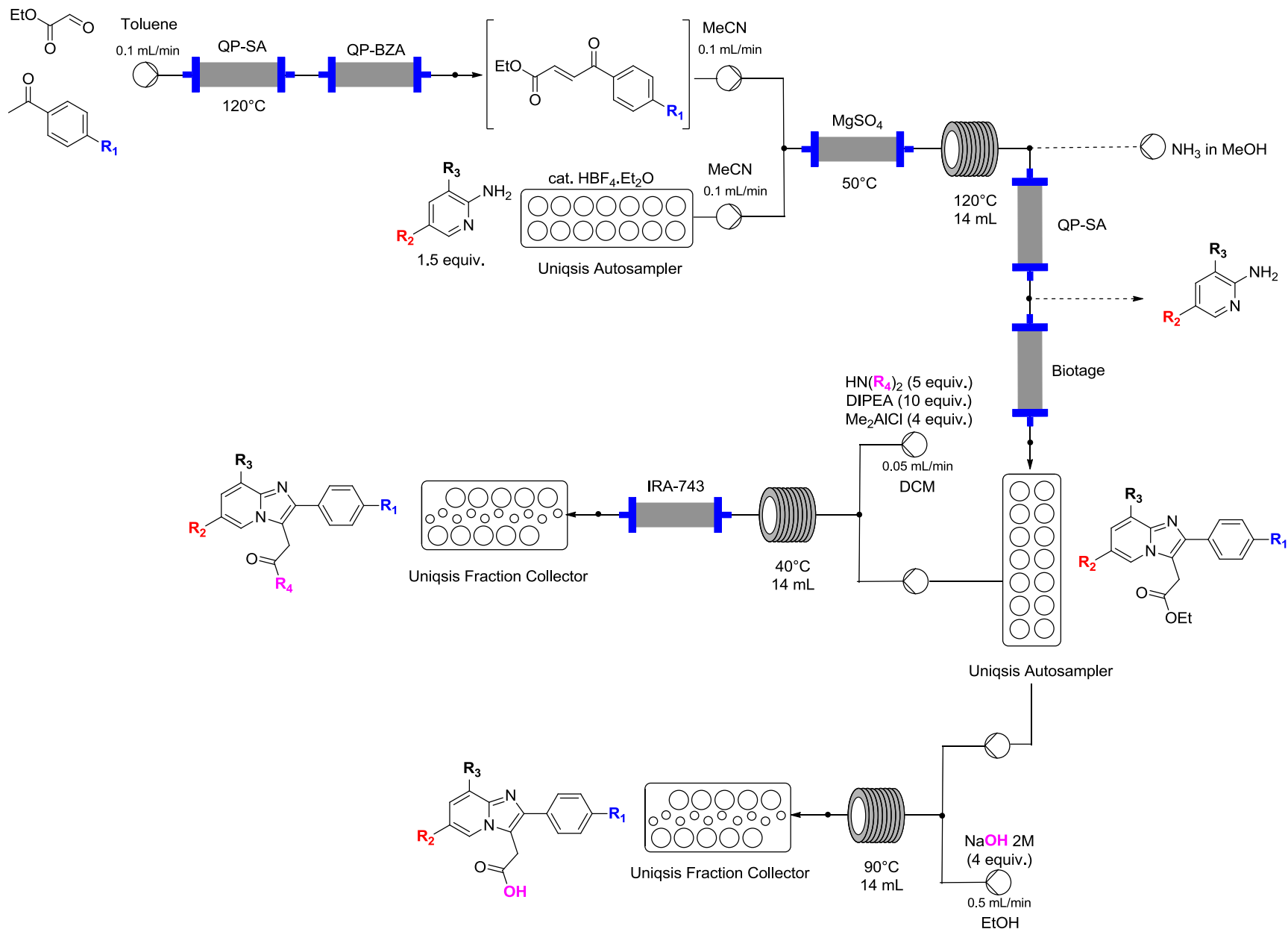
Diclofenac

Molecule	Bound in plasma (%)	Rt Volume	Estimated Kd (microM)
DMSO	-	127 $\mu$ L	- $V_o$
Isoniazid	0	130 $\mu$ L	-
Zolpidem	92	414 $\mu$ l	52
Diclofenac	99.8	838 $\mu$ l	1.2

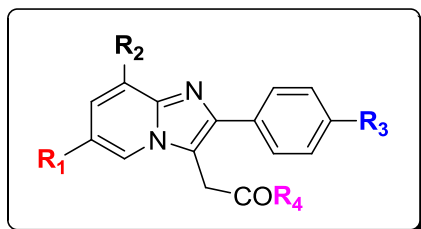
- Diclofenac, zolpidem and DMSO were retained with the correct order and reproducibly
- The assay was used to evaluate the binding of a series of GABA<sub>A</sub> agonists to HSA



# Automated Flow Synthesis of GABA<sub>A</sub> Ligands

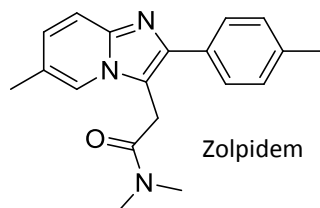


## Synthesised GABA<sub>A</sub> Ligands



	R <sub>1</sub>	R <sub>2</sub>	R <sub>3</sub>	R <sub>4</sub>	V (μL) @ 8 μM	K <sub>d</sub> (μM)	B <sub>t</sub> (nmoles)
DMSO	-	-	-	-	115.9	-	-
1	CH <sub>3</sub>	H	CH <sub>3</sub>	NMe <sub>2</sub>	430.1	60	20.5
2	CH <sub>3</sub>	H	CH <sub>3</sub>	OH	680.5	25	21.5
3	CH <sub>3</sub>	H	CH <sub>3</sub>	NPr <sub>2</sub>	520.2	42	32.8
4	Cl	H	Cl	NMe <sub>2</sub>	456.0	64	24.9
5	Cl	H	Cl	OH	822.5	37	31.2
6	H	H	CH <sub>3</sub>	NMe <sub>2</sub>	267.5	152	23.5
7	H	H	CH <sub>3</sub>	OH	428.9	49	18.0
8	CH <sub>3</sub>	H	Cl	NPr <sub>2</sub>	552.2	79	36.6
9	CH <sub>3</sub>	H	Cl	NMe <sub>2</sub>	425.1	78	26.2
10	CH <sub>3</sub>	H	Cl	OH	486.4	57	22.9
11	Cl	H	CH <sub>3</sub>	NMe <sub>2</sub>	332.4	88	20.2
12	Cl	H	CH <sub>3</sub>	OH	494.3	40	17.5
13	CH <sub>3</sub>	Br	CH <sub>3</sub>	OH	203.7	33	14.4
14	CH <sub>3</sub>	Br	CH <sub>3</sub>	NMe <sub>2</sub>	378.4	84	24.1

K<sub>d</sub> (μM) 52





**Department of Chemistry**  
**E-mail: [i.r.baxendale@durham.ac.uk](mailto:i.r.baxendale@durham.ac.uk)**

**Members of the ITC**

Dr Francesco Tozzi	Dr Steve Lanners	Dr Jason Tierney
Dr Lucia Tamborini	Dr Tash Polyzos	Dr Peter Koos
Dr Heiko Lange	Dr Celeste Iannuzzi Maria	Dr Victoria Rojo
Dr Laetitia Martin	Dr Malte Brasholz	Dr Catherine Carter
Dr Matt Kitching	Dr Francesco Venturoni	Dr Elena Riva
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Dr Tobias Brodmann	Dr Ulrike Gross	

**Members of BCL**

Carl Millia  
Laurens Brocken  
Dr Marcus Baumann  
Francesco Calogero  
Dr Francesco Venturoni  
Antonio M. Rodríguez  
Ben Thompson

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# Understanding and Optimising Chemical Processes through Statistical Methodologies

Durham University, 8th-10th July 2013

**Do you want to:**

- significantly expand process understanding?
- establish and develop capability?
- ensure robust and in-control processes?
- improve quality?
- reduce operational and environmental costs?



**For more details please contact**  
**matthew.linsley@newcastle.ac.uk**  
**or**  
**p.g.steel@durham.ac.uk**